

Welcome to

Pump

Installation & Maintenance

by Fayek Shakran

Course Objective

identify pump classifications

describe the purpose of pump parts.

define various pump terms.

explain pump operation.

describe the components of a pump curve.

Describe a simple pumping system.

describe typical pump failures and their causes



Introduction



Introduction

Pump Definition

Pump is defined as a mechanical device that rotates or reciprocates to move fluid from one place to another

Purpose of a pump:

A pump is designed to:
transfer fluid from one point
to another.

~from low pressure areas to
higher pressure Areas.

~from lower elevations to
higher Elevations.

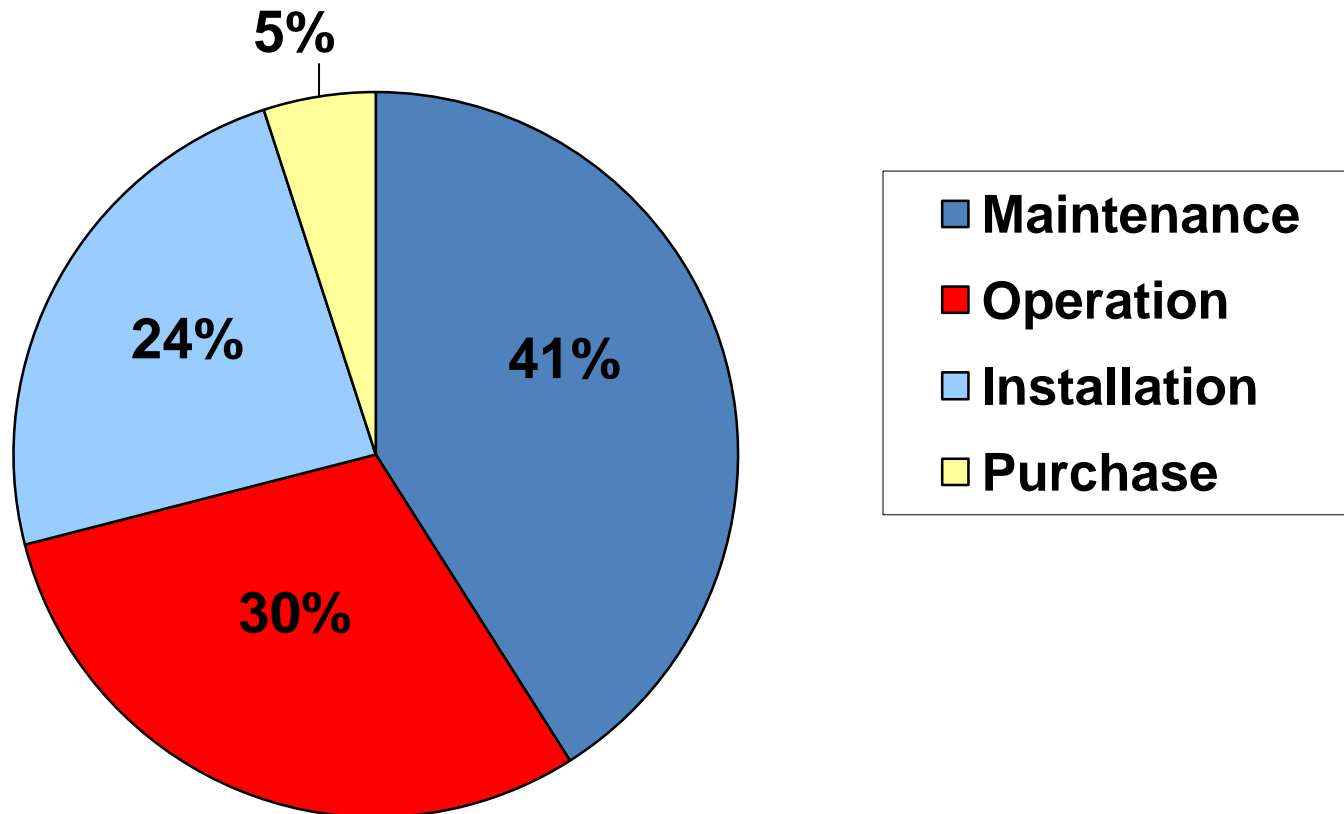
~From local locations to
distant locations.



Life Cycle Cost

Energy and maintenance costs during the life of a pump system are usually more than 10 times its purchase price

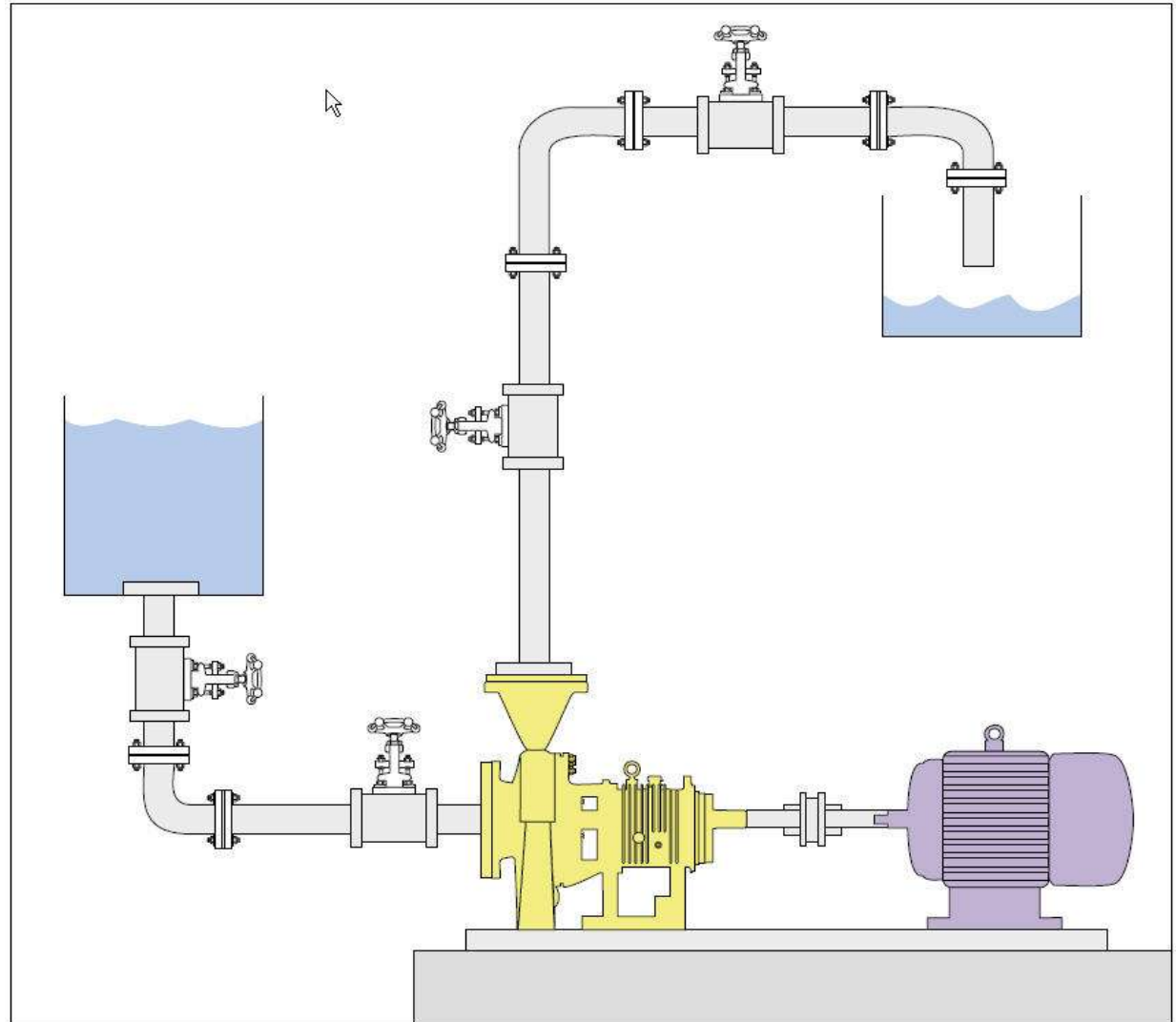
20 Year Life Cycle Cost Chemical Process Pump



Pumping System Basics

Typical pumping systems contain five basic components:

Pumps.
prime movers.
Piping.
Valves.
end-use equipment.

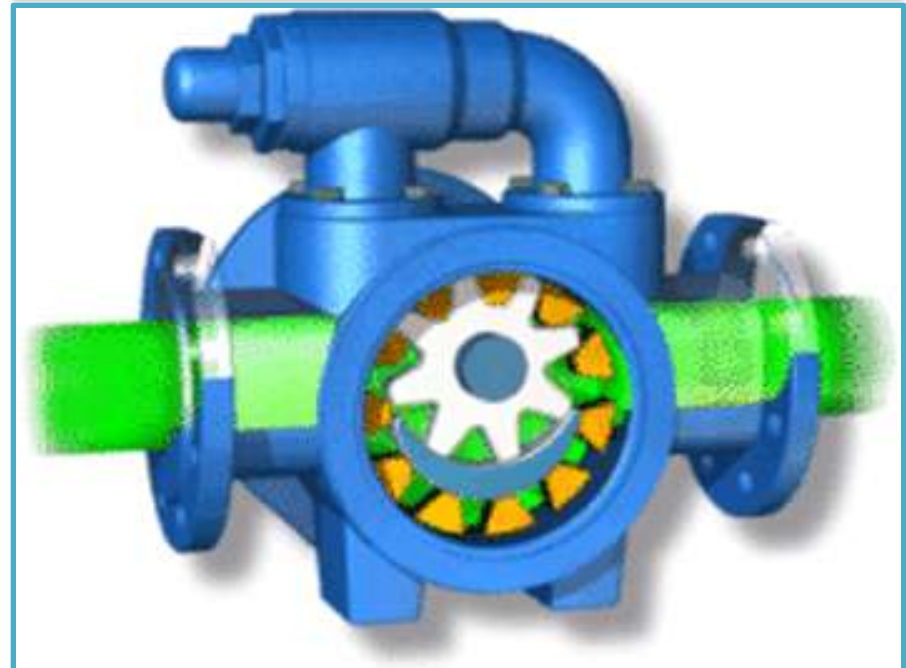


Pumps Types

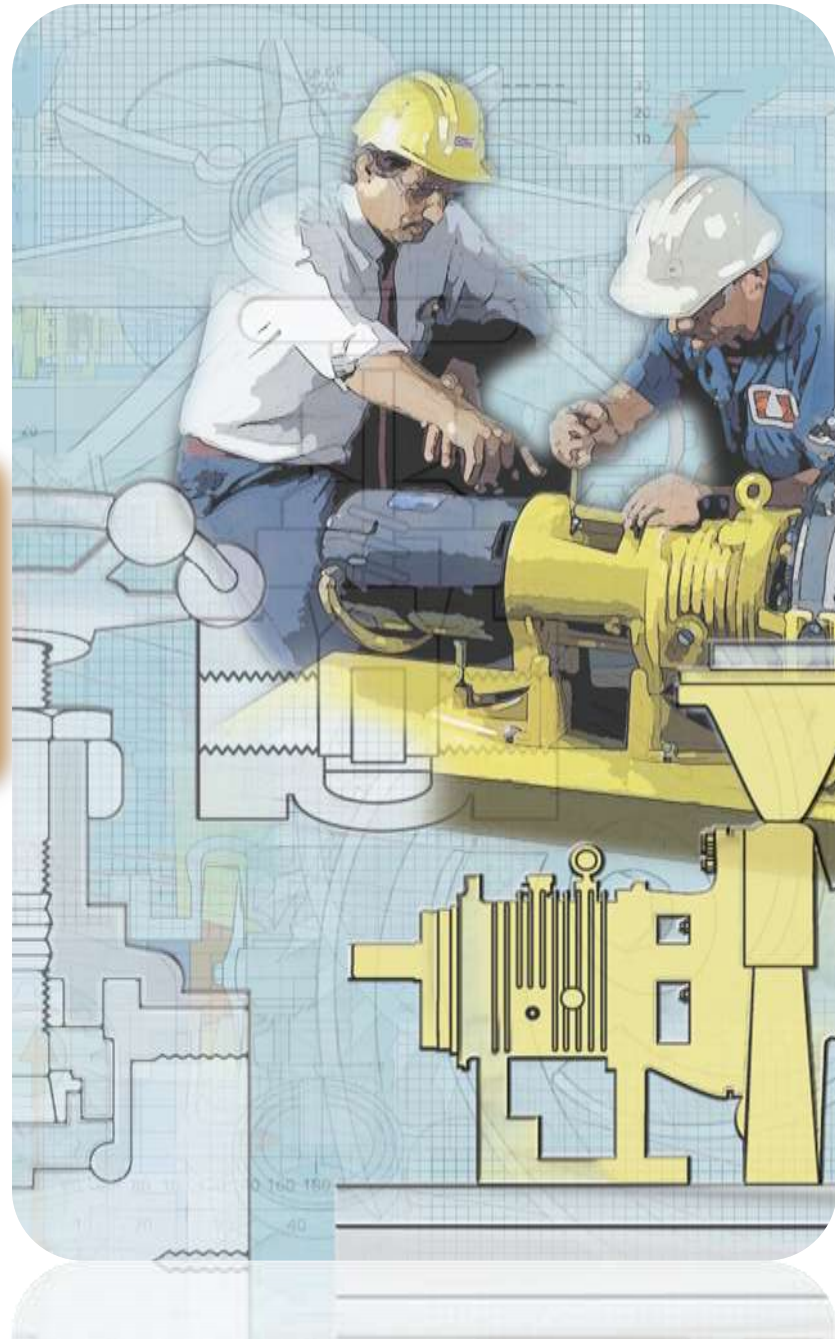
Pumps are available in a wide range of types, sizes, and materials, two categories described—positive displacement and centrifugal.

Centrifugal pumps have a variable flow/pressure relationship.

positive displacement pumps have a fixed displacement volume. Consequently, the flow rates they generate are directly proportional to their speed.



Positive displacement pump



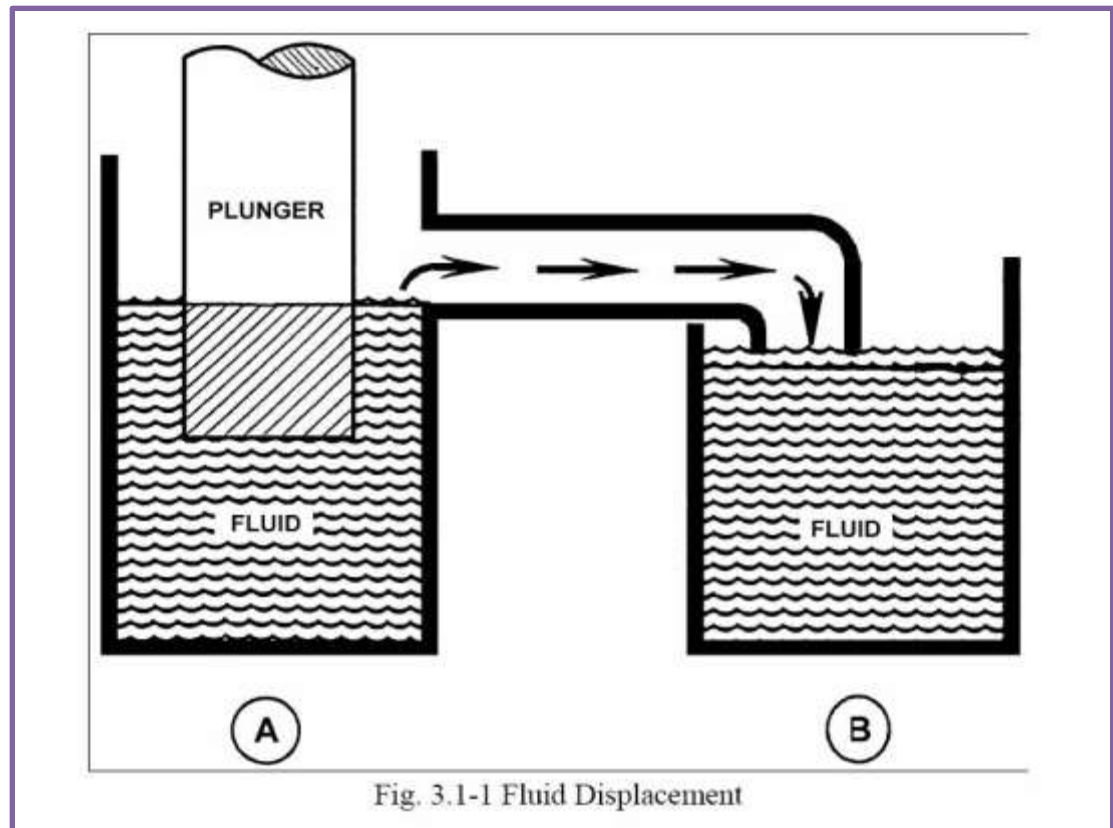
Positive Displacement Pumps

Positive displacement pumps work on the principle that – No two objects can occupy the same space at the same time

A solid will displace a volume of fluid equal to its own volume

Reciprocating element
(piston – plunger)

Rotating element
(Vans , Screws or
Gears)



Positive Displacement Pumps

Discharge flow / rate can be controlled by:

- ~ Change the speed of the prime mover.
- ~ Use of bypass lin.
- ~ Change of the piston stroke length.

Types of Positive Displacement Pumps

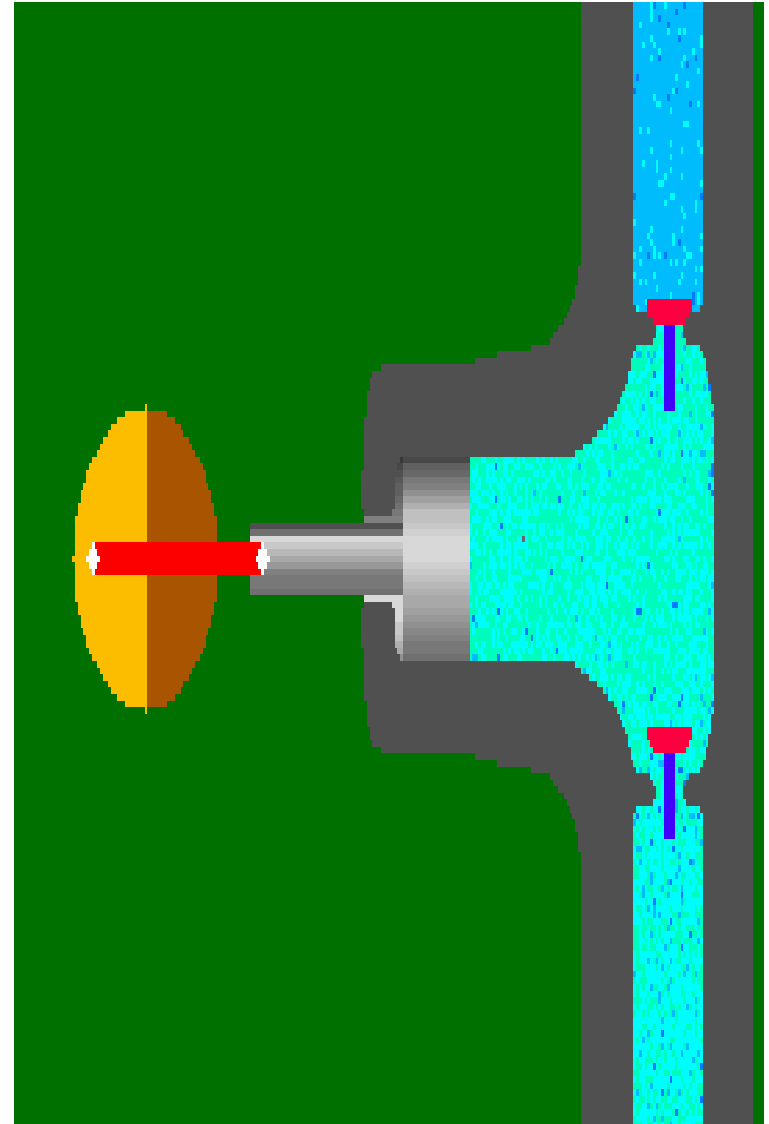
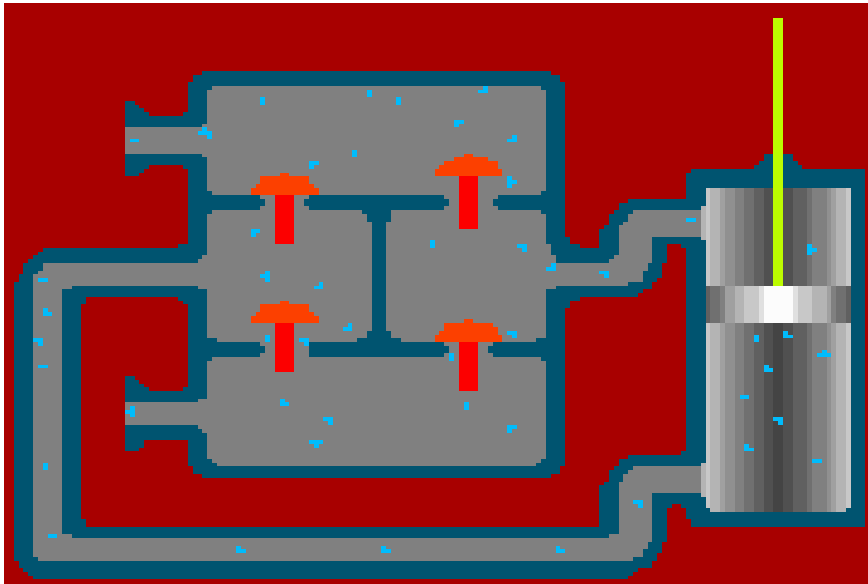
Reciprocating Pumps

Rotary Pumps

Reciprocating Pumps

Three main types:

- Piston Type.
- Plunger Type.
- Diaphragm Type.



Piston Type Reciprocating Pump

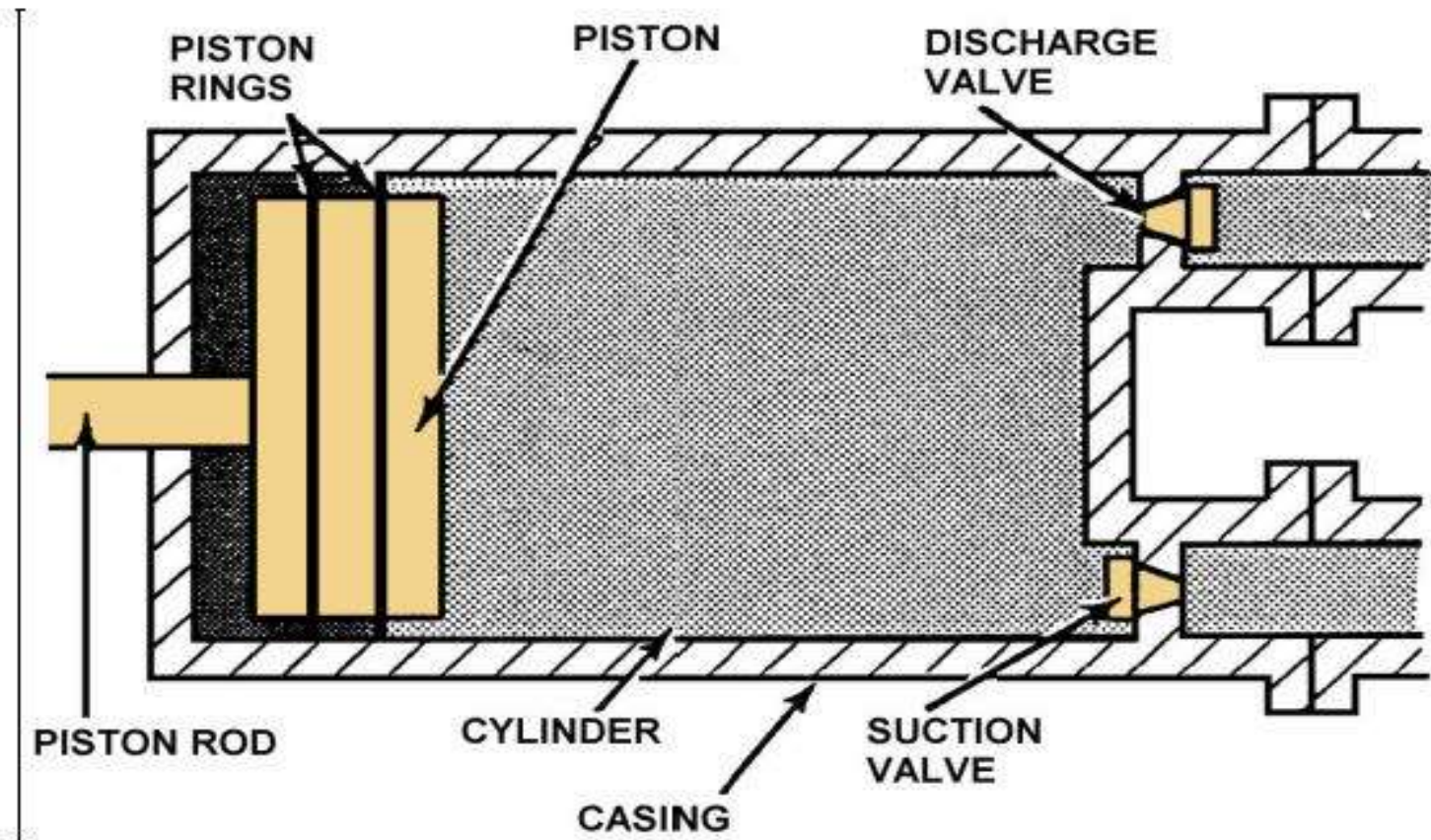
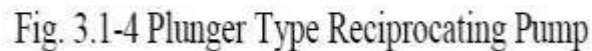


Fig. 3.1-3 Piston Type Reciprocating Pump

Each complete movement of the piston along the length of the cylinder is called A STROKE

Used as portable backup pumps for the removal of surplus process fluids

Very similar to piston type pumps and either vertical or horizontal acting



Diaphragm Pump

Get their name from the flexible diaphragm

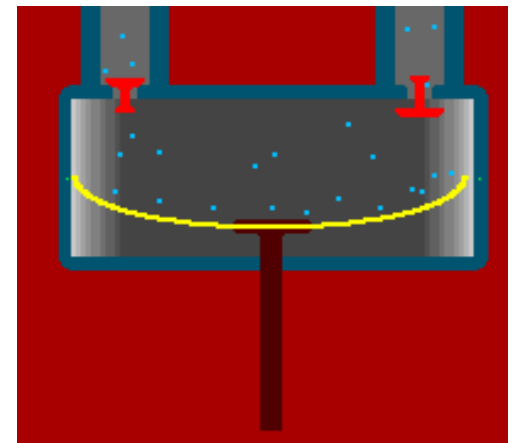
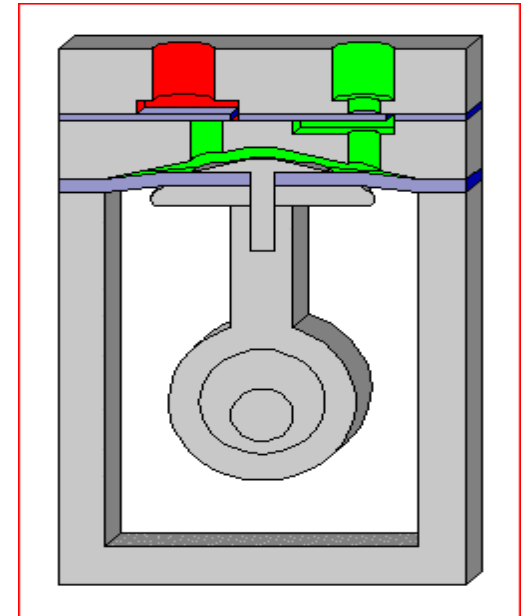
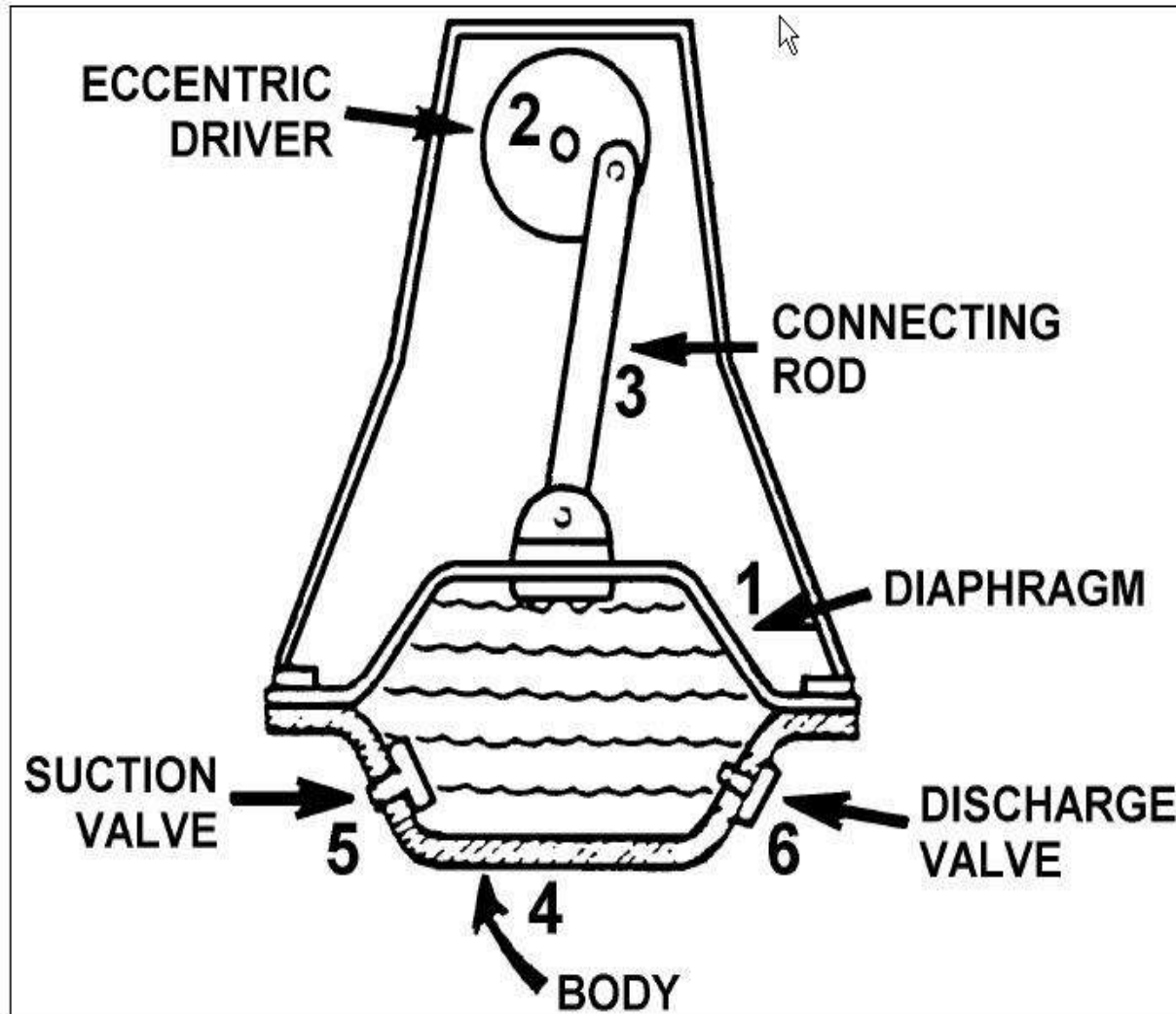
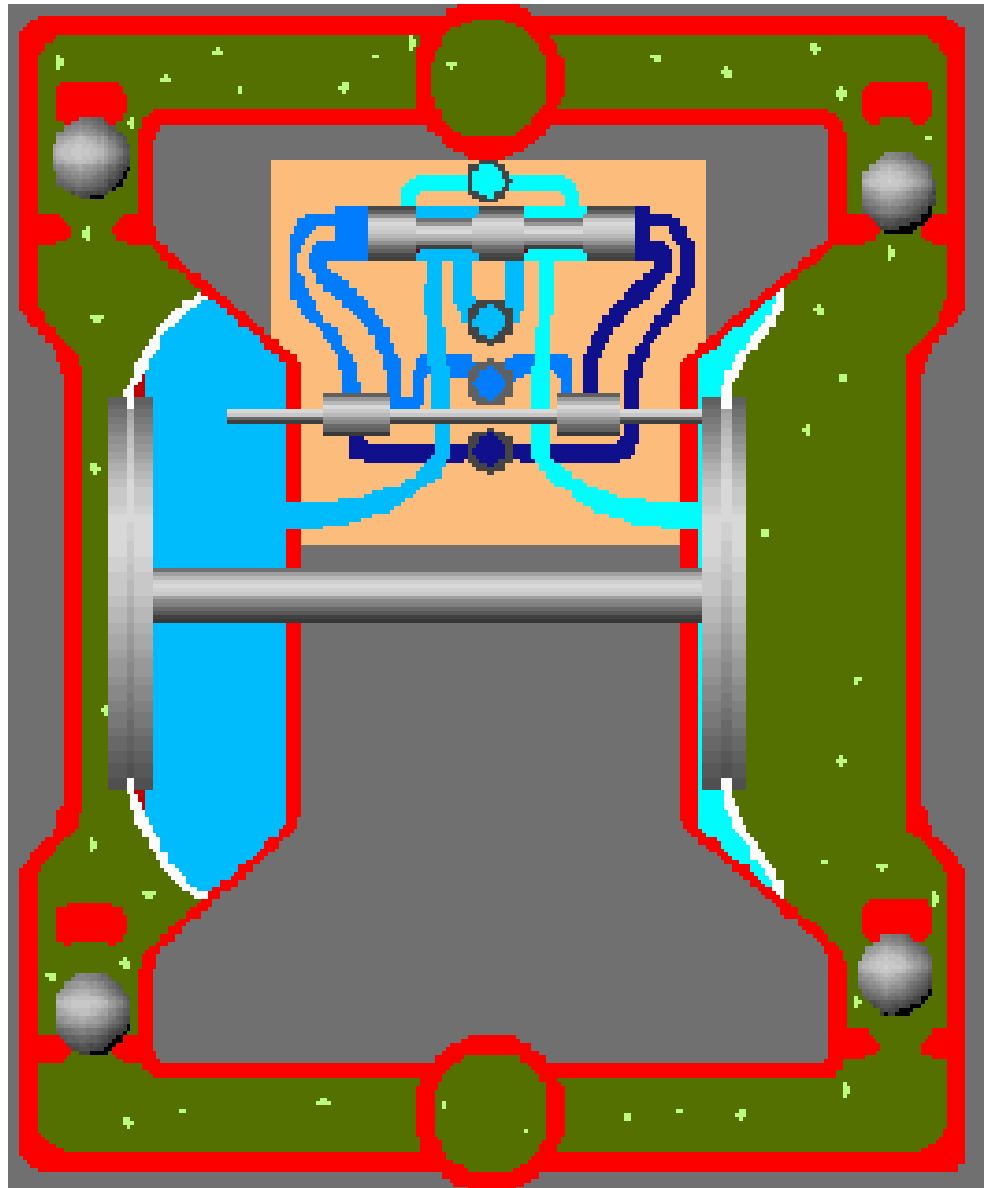


Fig. 3.1-5 Diaphragm Pump

Diaphragm Pump

Double-Diaphragm Pump



Diaphragm Pump

A perfect seal, it makes **Diaphragm Pump** ideal for:

- 1~ pumping chemicals.
- 2~ Controlled metering.

A diaphragm is usually made of a flexible rubber materials often covered with a thin metal disc where the connecting rod is attached.

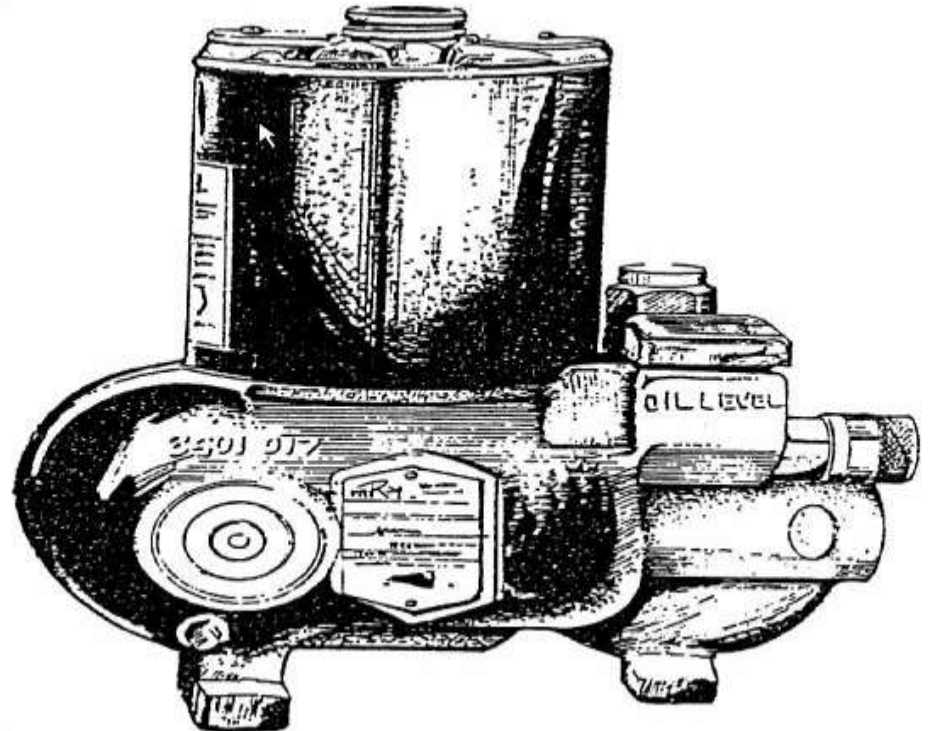
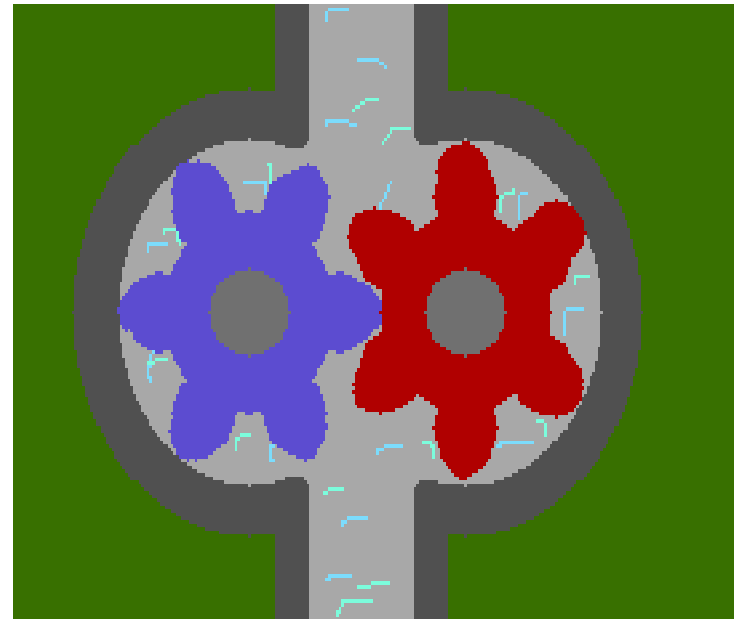


Fig. 3.1-6 Positive Displacement Diaphragm Pump

Rotary Pumps

Types of Rotary Pumps

- ~Gear Pump.
- ~Sliding Vane Pump.
- ~Rotary Lobe Pump.
- ~Rotary Screw Pump.



Gear Pump / External

consists of two intermeshing gears, one driven and one idling, in a close-fitting casing

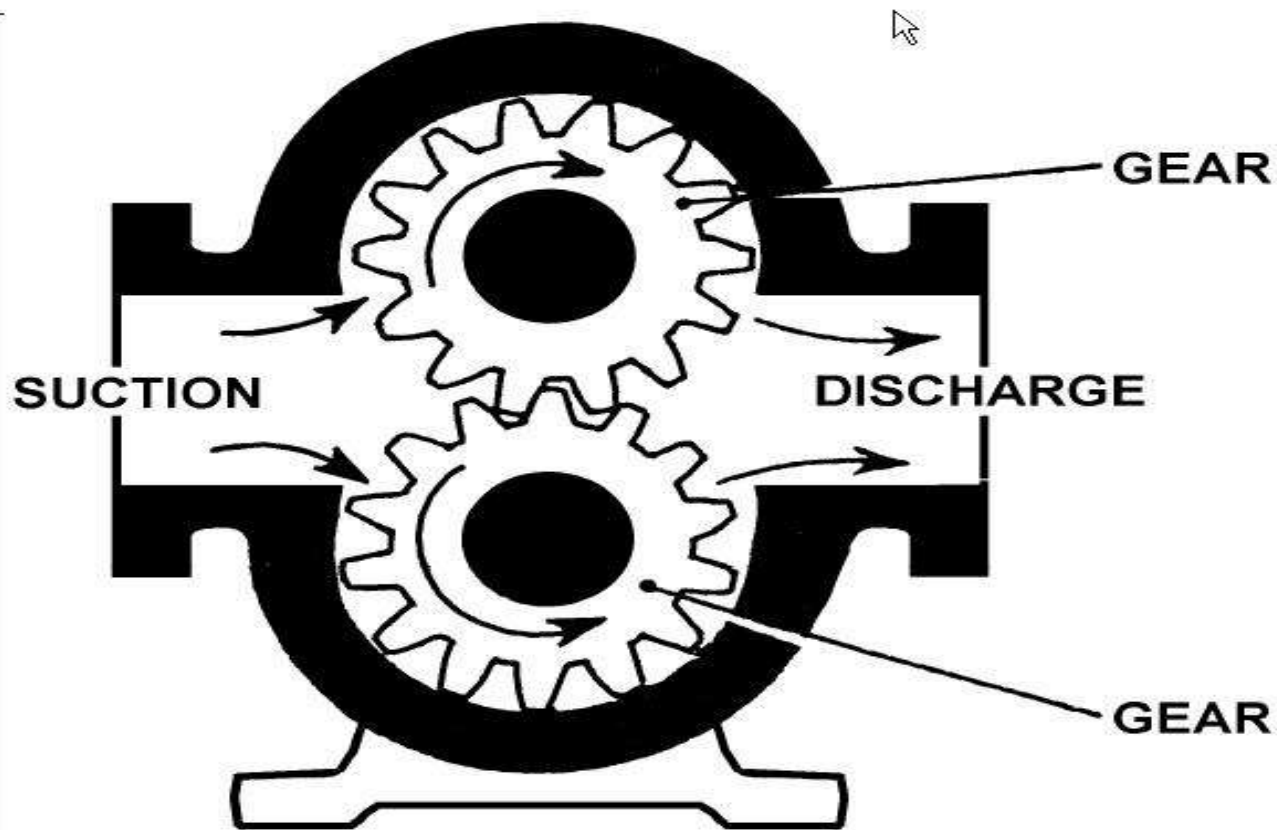
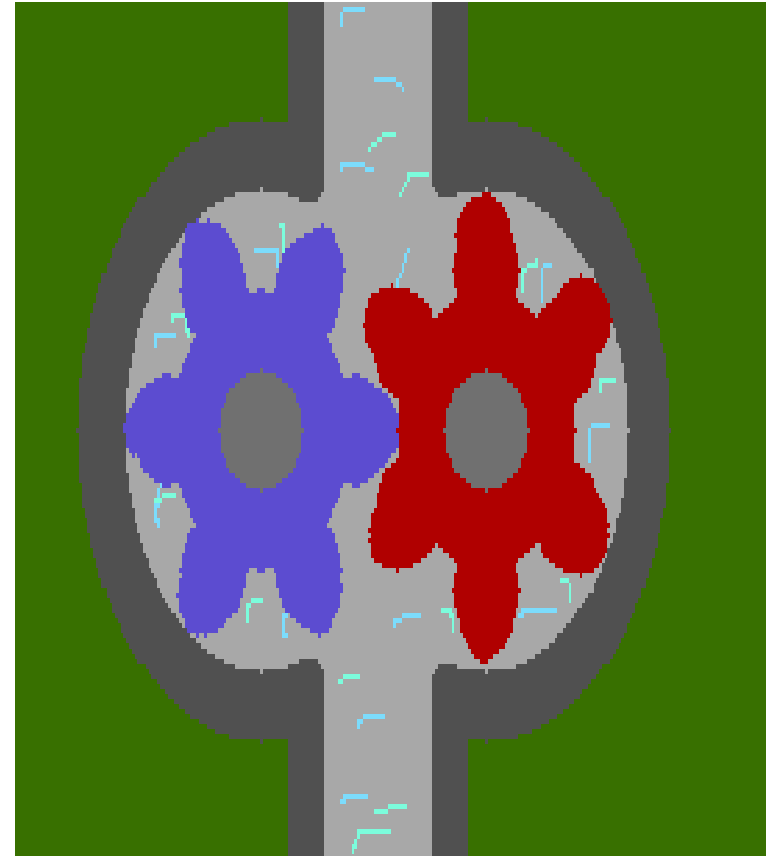


Fig. 3.2-1 External Gear Pump

Gear Pump / External



Gear Pump / Internal

Internal gear pump has a small (driven) gear mounted eccentrically inside a larger idler gear that rotates inside a circular casing.

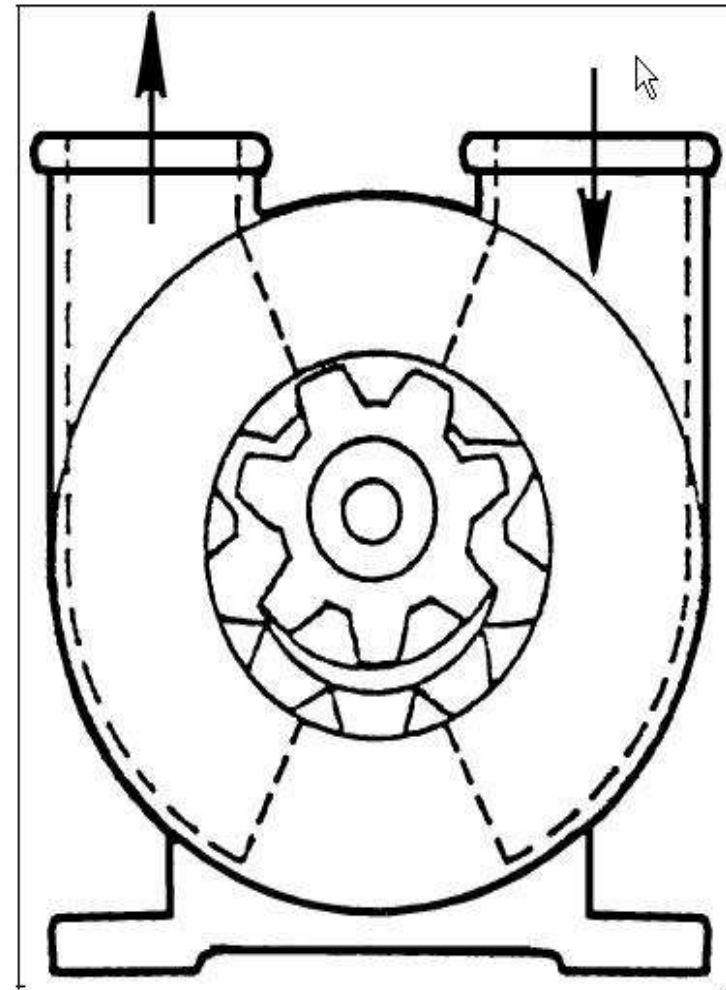
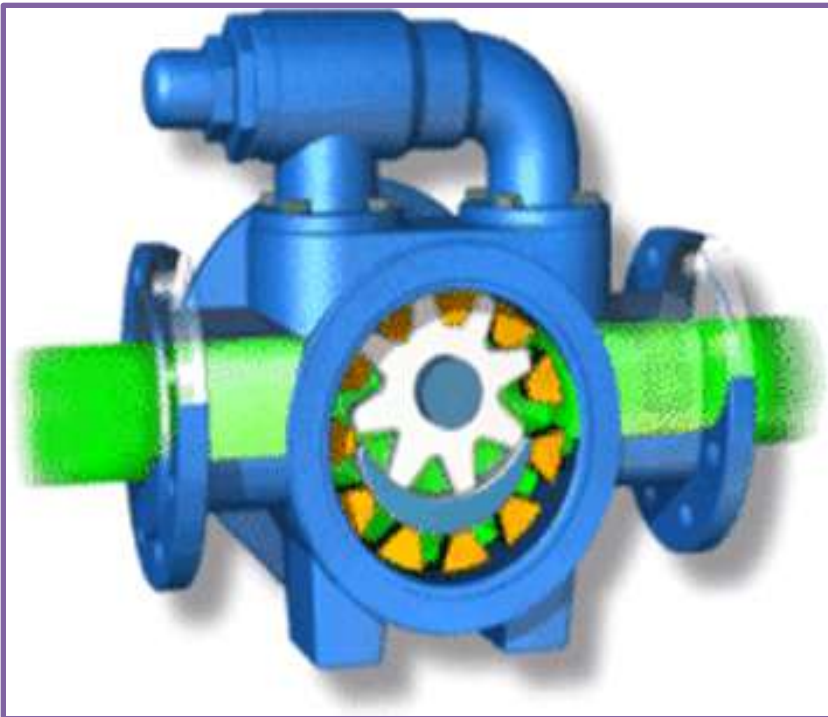
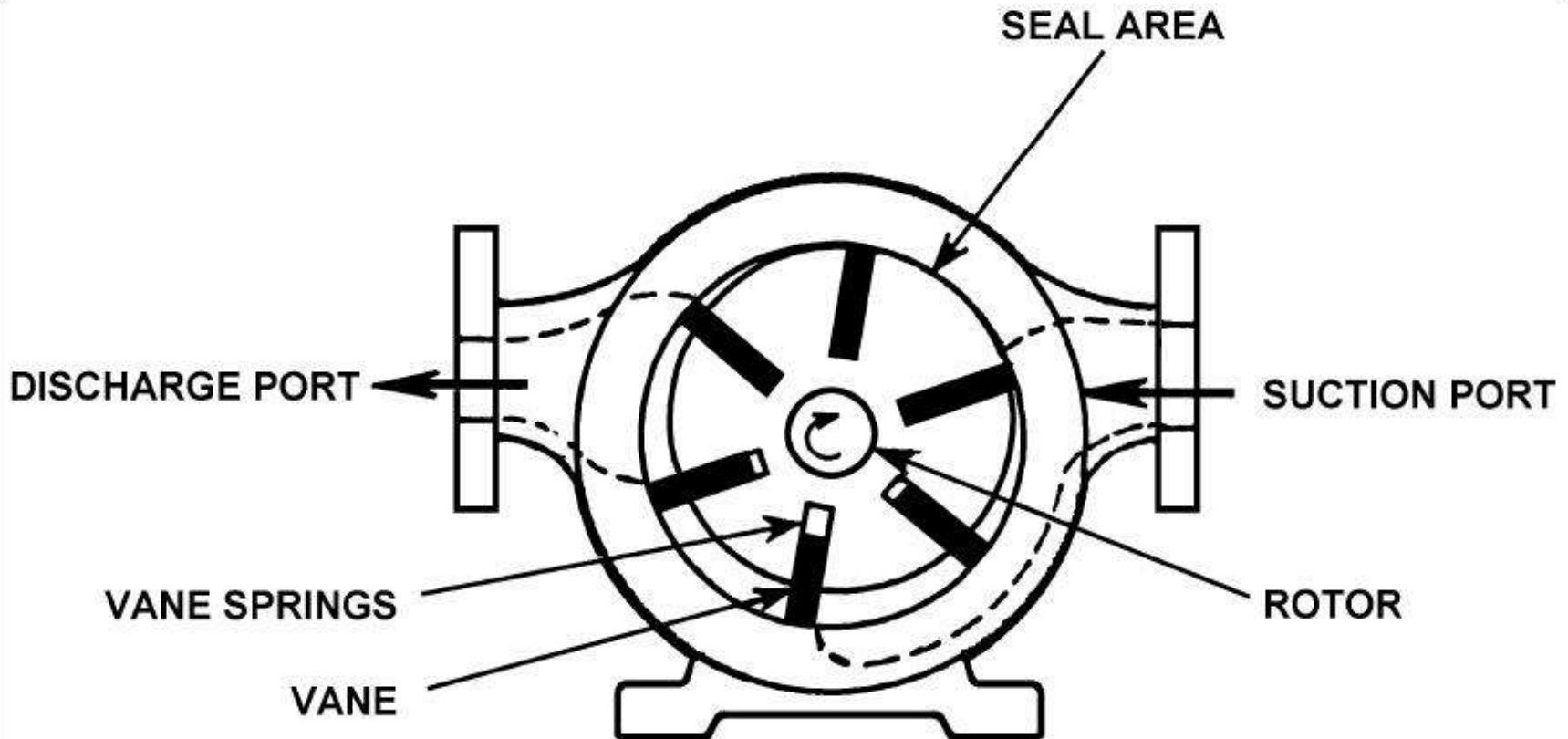


Fig. 3.2-3 Internal Gear Pump

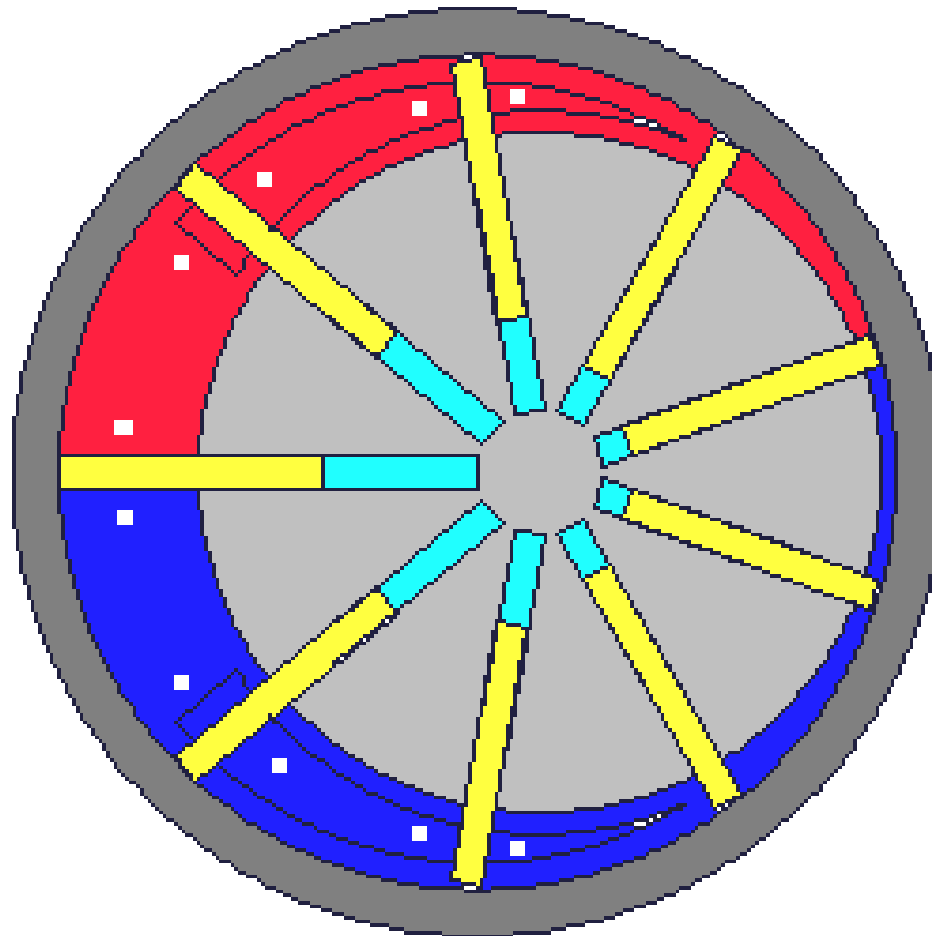
Vane Pump

The common vane type pump consists of a rotor with a radial slots machined into it. The rotor is mounted off-center and rotates inside a circular casing.

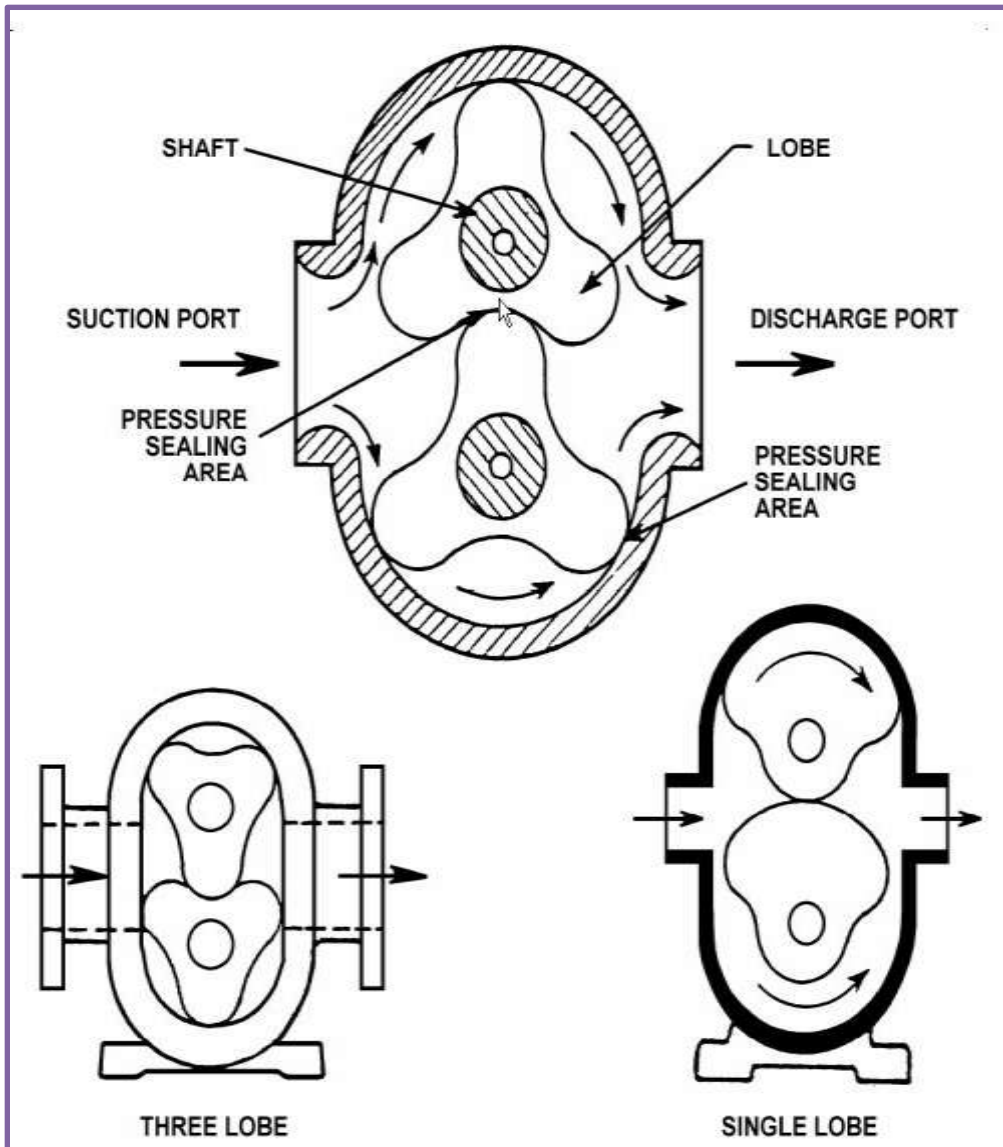


Vane Pump

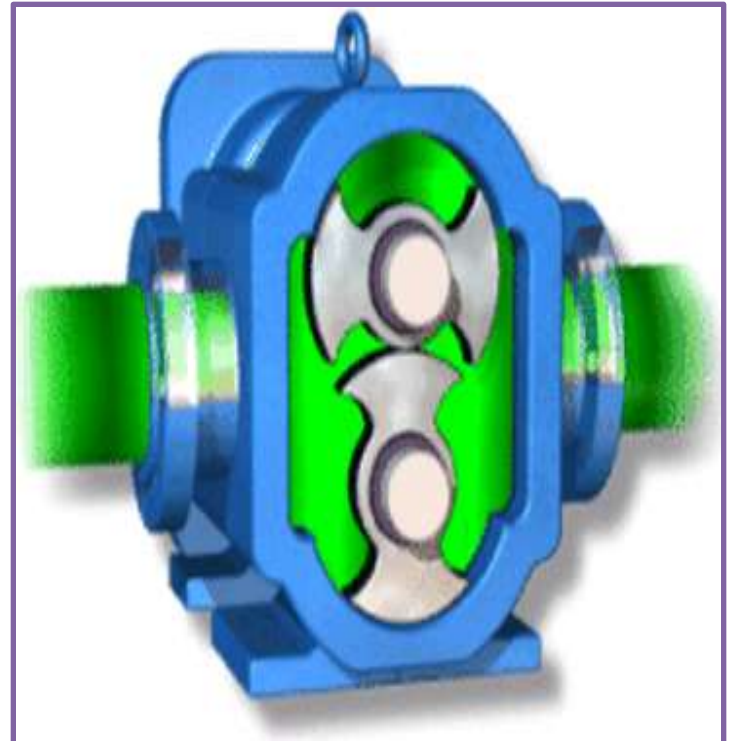
Liquid is drawn in through the suction side and squeezed out under pressure through the discharge side.



Rotary Lobe Pump



The rotary lobe pump works on a similar principle to the gear pump



Rotary Screw Pump

Rotary screw pumps are special types of rotary positive displacement pumps in which the flow through the pumping elements is truly axial.

Screw pumps are also called **axial flow pumps**

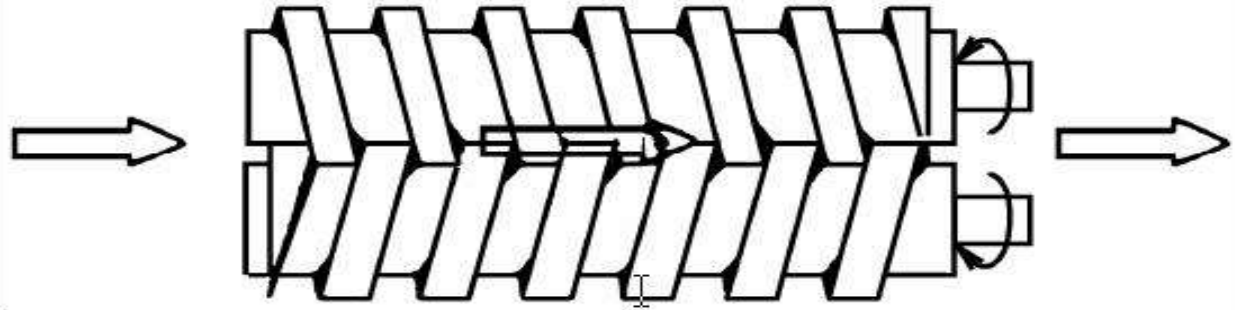


Fig. 3.2-7A Screw Pump — Axial Flow

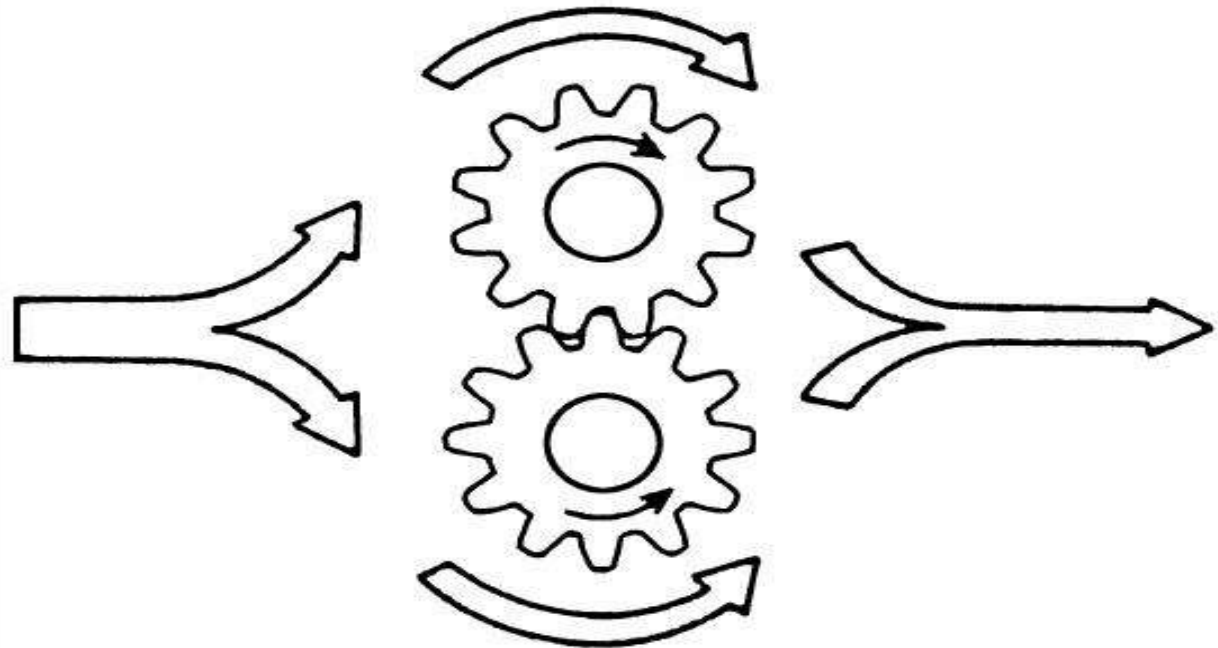


Fig. 3.2-7B Gear Pump — Circumferential Flow

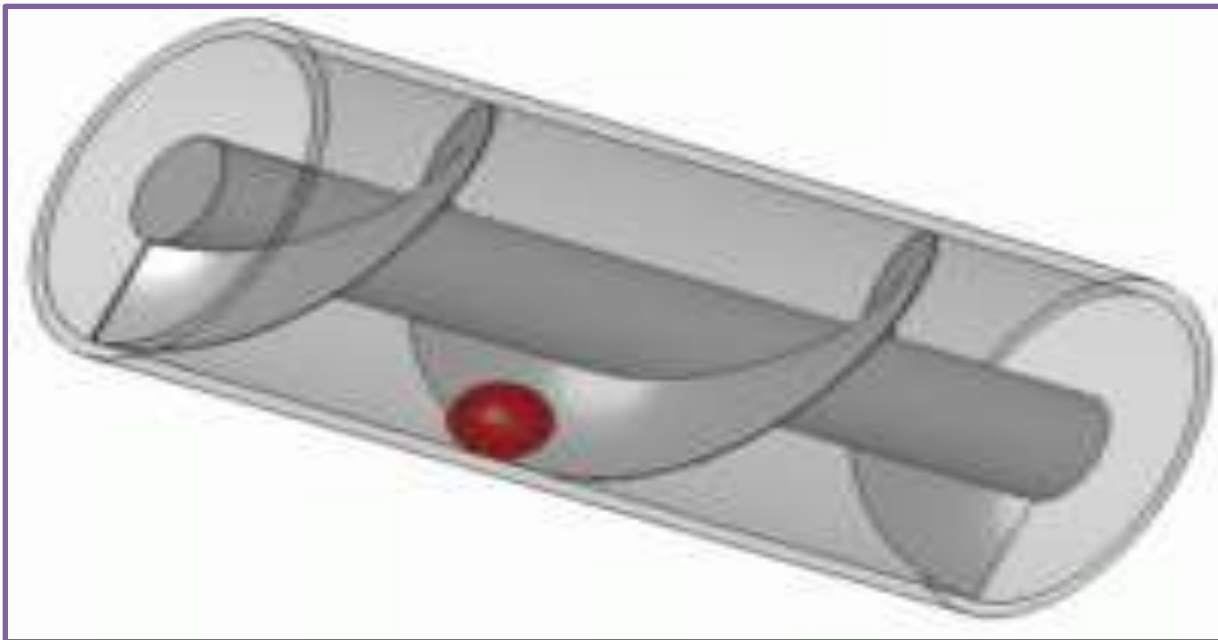
TYPES OF SCREW PUMPS

Screw pumps can have one , two or three screws

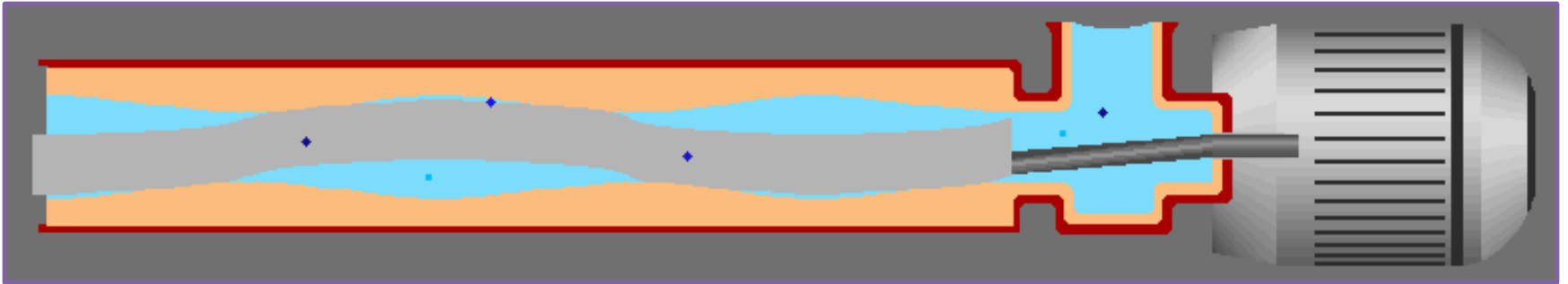
The types of screw pumps are the:

Single Screw Pump

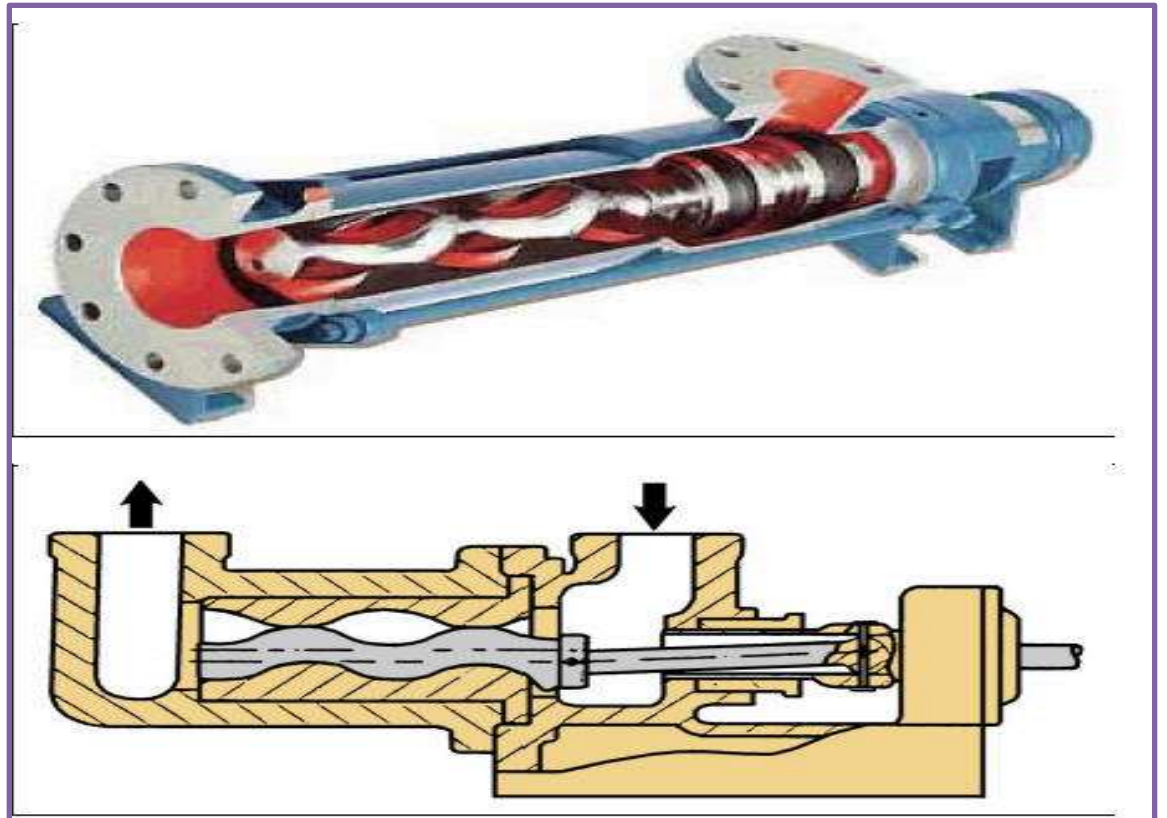
Multiple Screw Pump



Single Screw Pumps



It consists of a spiral-shaped rotor that turns in an internal-helix liner. The rotor is usually metal. The liner is rubber.

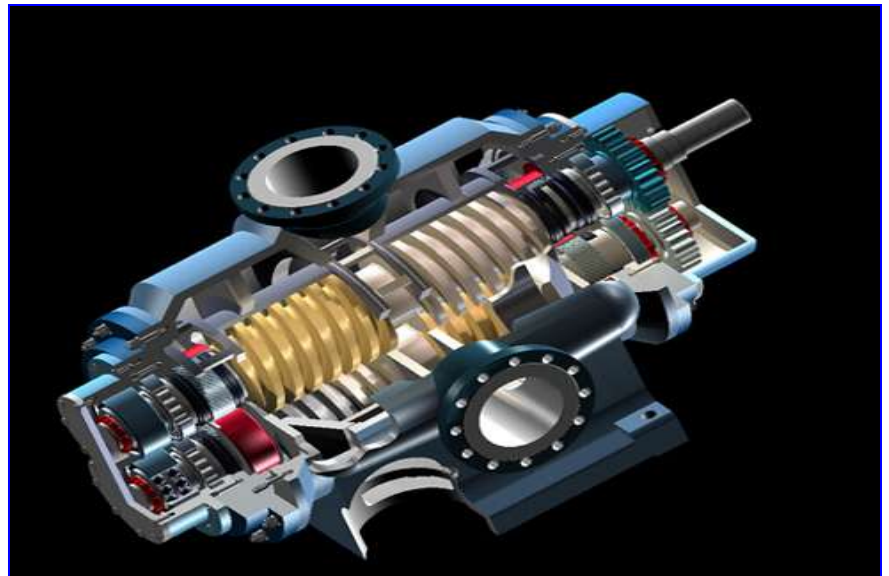
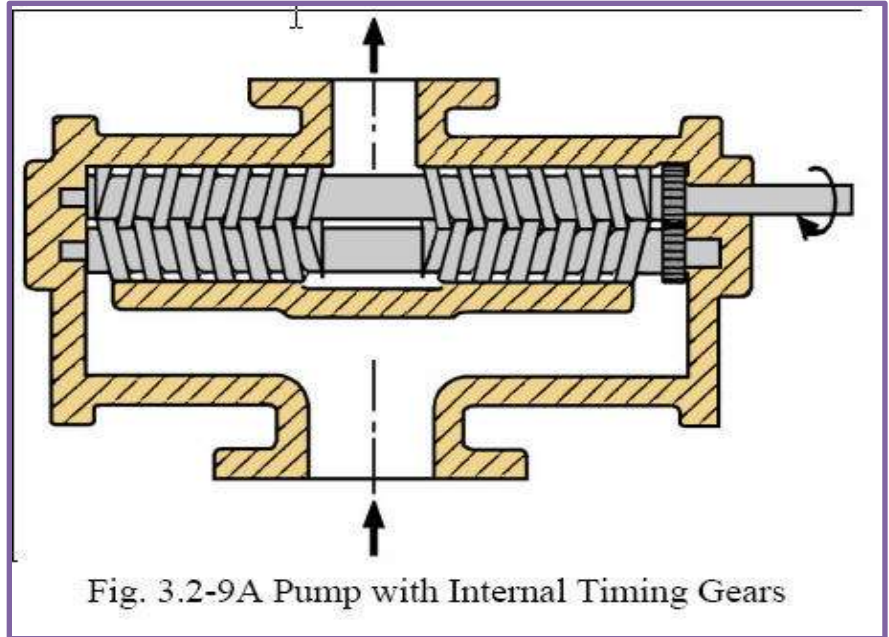


Multiple Screw Pumps

Multiple screw pump increases the pumping capacity of a single screw type by providing additional rotors to move fluid.

Multiple screw pumps are driven by a single rotor called the **power rotor**.

Two screw pumps are often called **timed screw pumps**



Multiple Screw Pumps

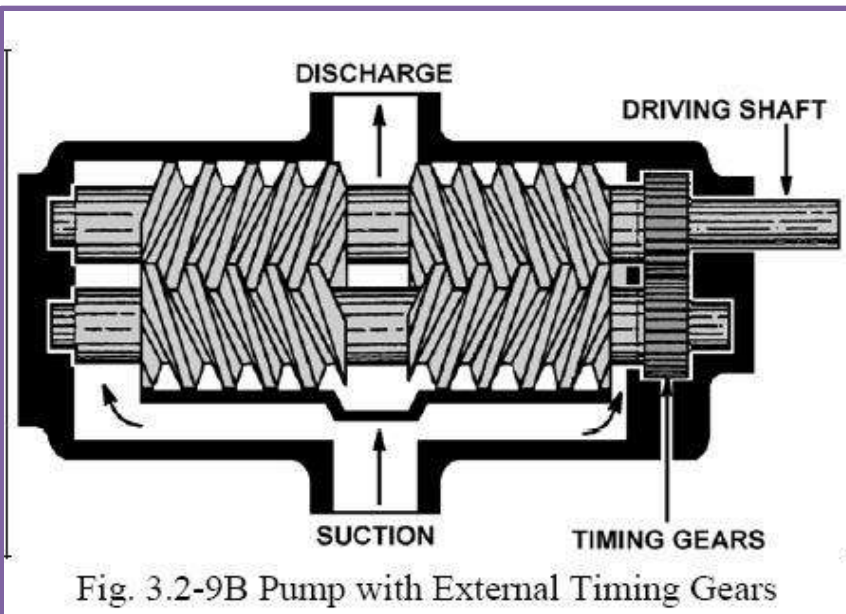
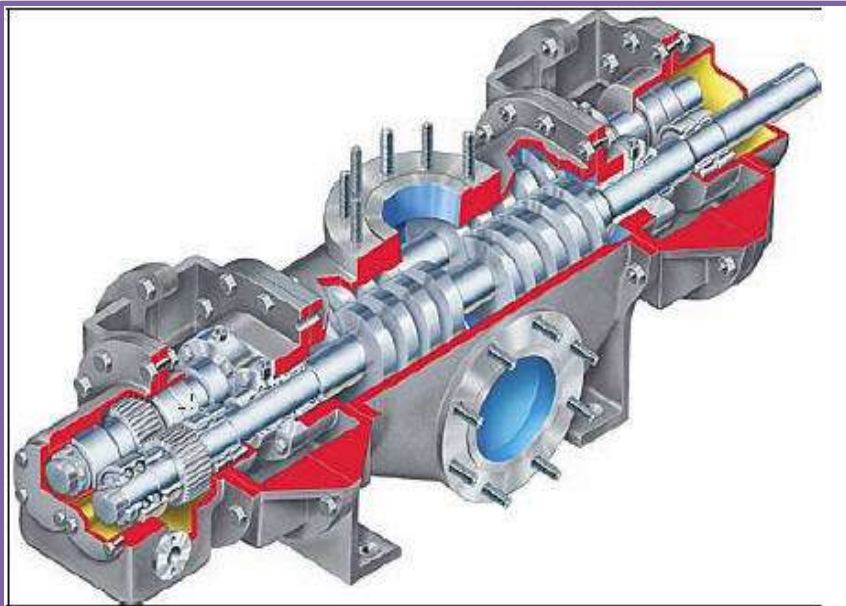


Fig. 3.2-9B Pump with External Timing Gears

Multiple Screw Pumps

Three-screw pumps have two idler screws. The idlers are threaded to mesh with the power rotor. (untimed screw pumps)

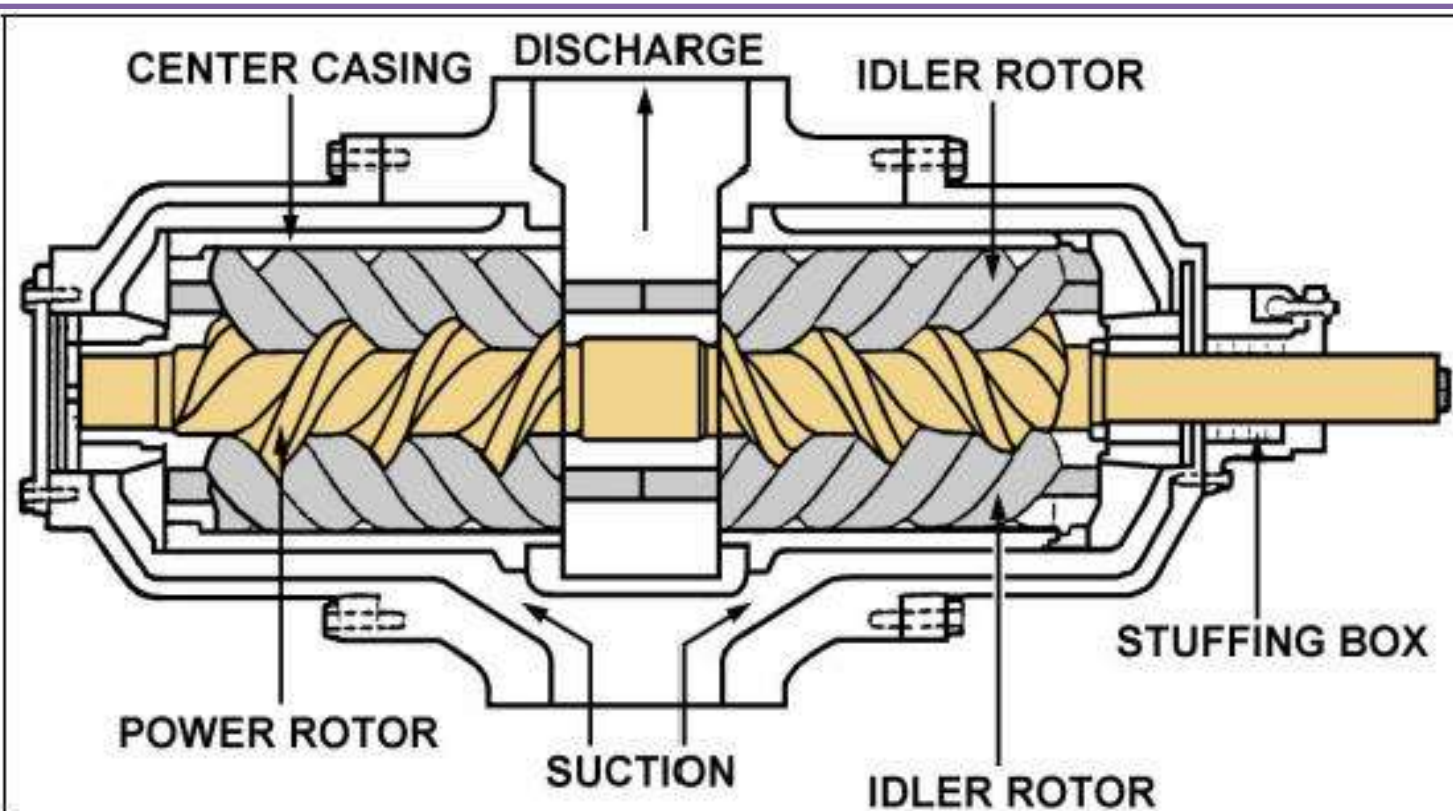


Fig. 3.2-10 Three-Screw Pump

Centrifugal and axial pumps

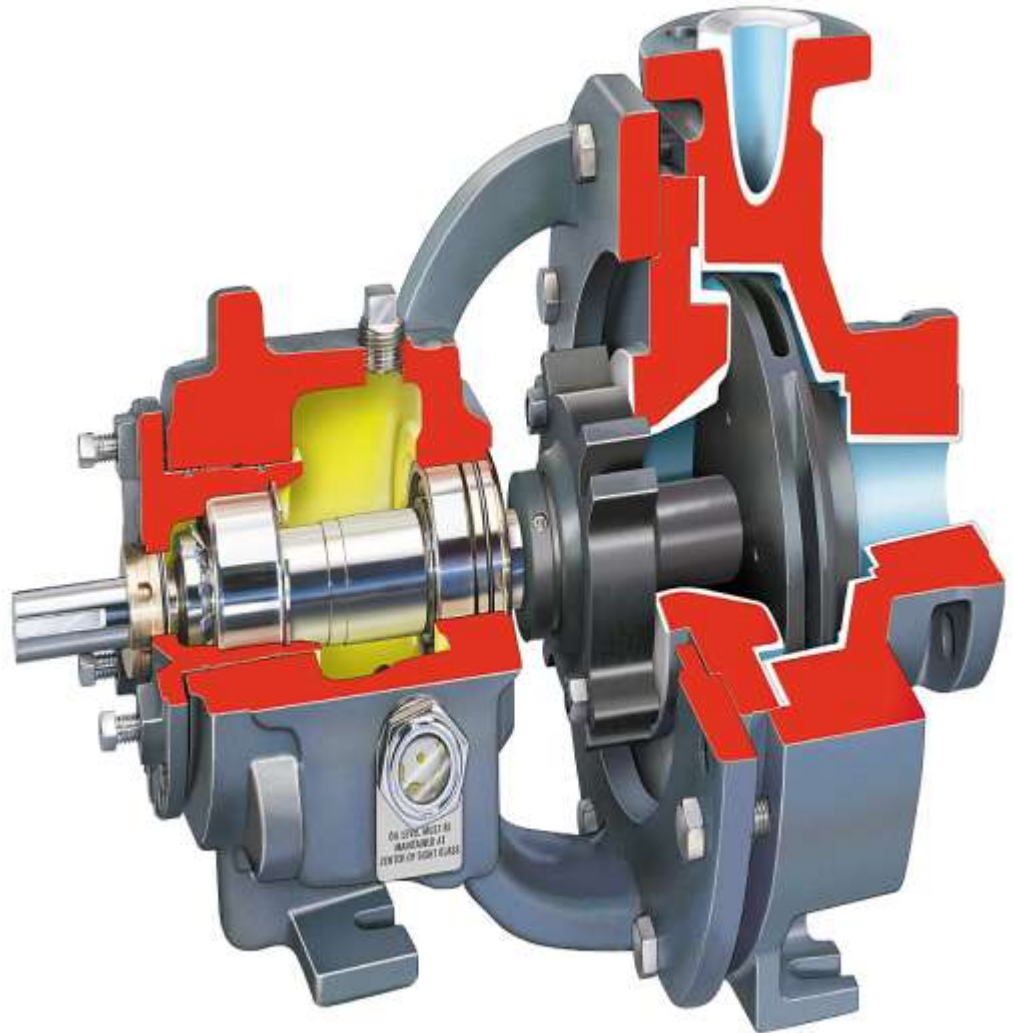
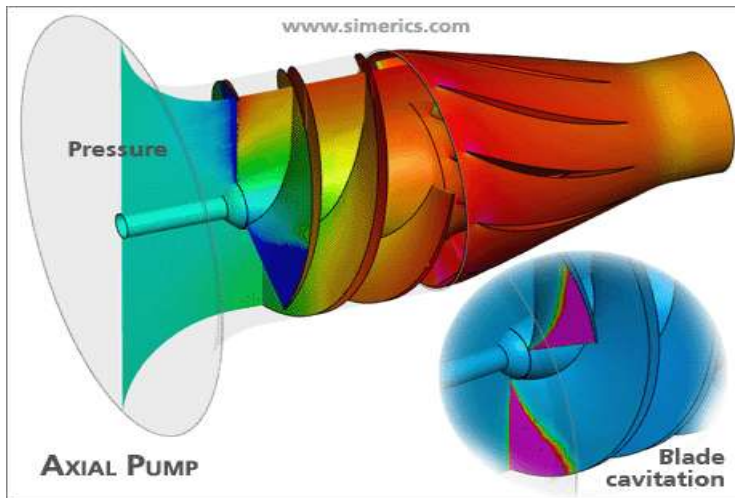


Initial Pump Selection

Centrifugal and axial pumps

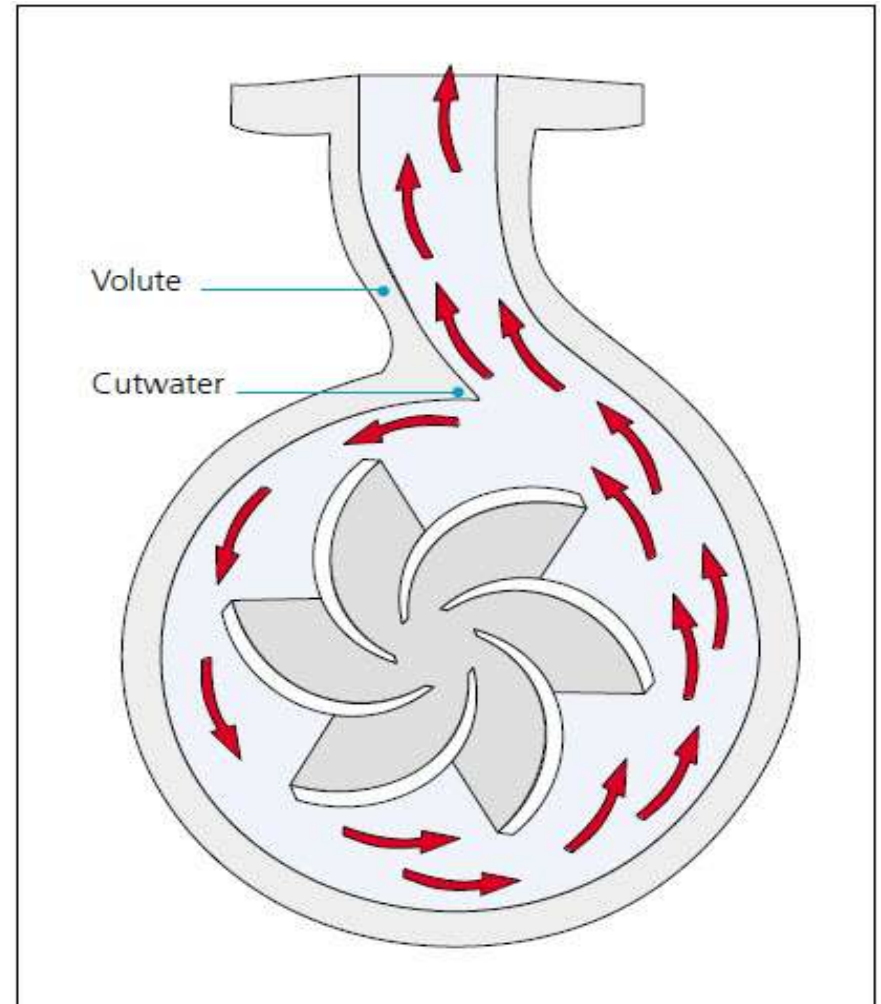
Centrifugal and axial pumps impart kinetic energy to a fluid and rely on the conversion of this kinetic energy to potential energy to increase fluid pressure

centrifugal pumps are used typically in high-flow, low-head applications in which fluid viscosity is not prohibitively high

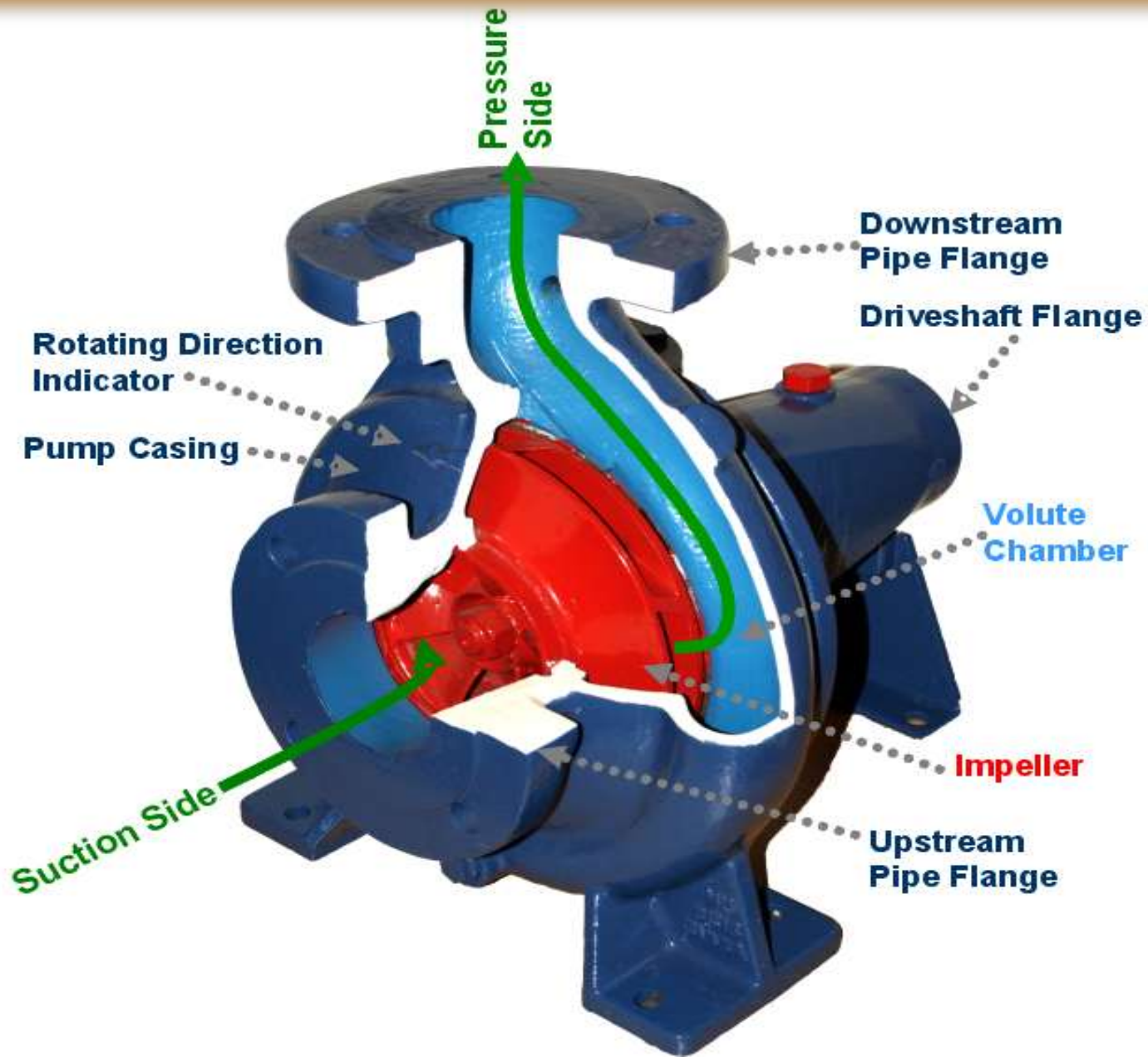


Initial Pump Selection

Centrifugal pumps

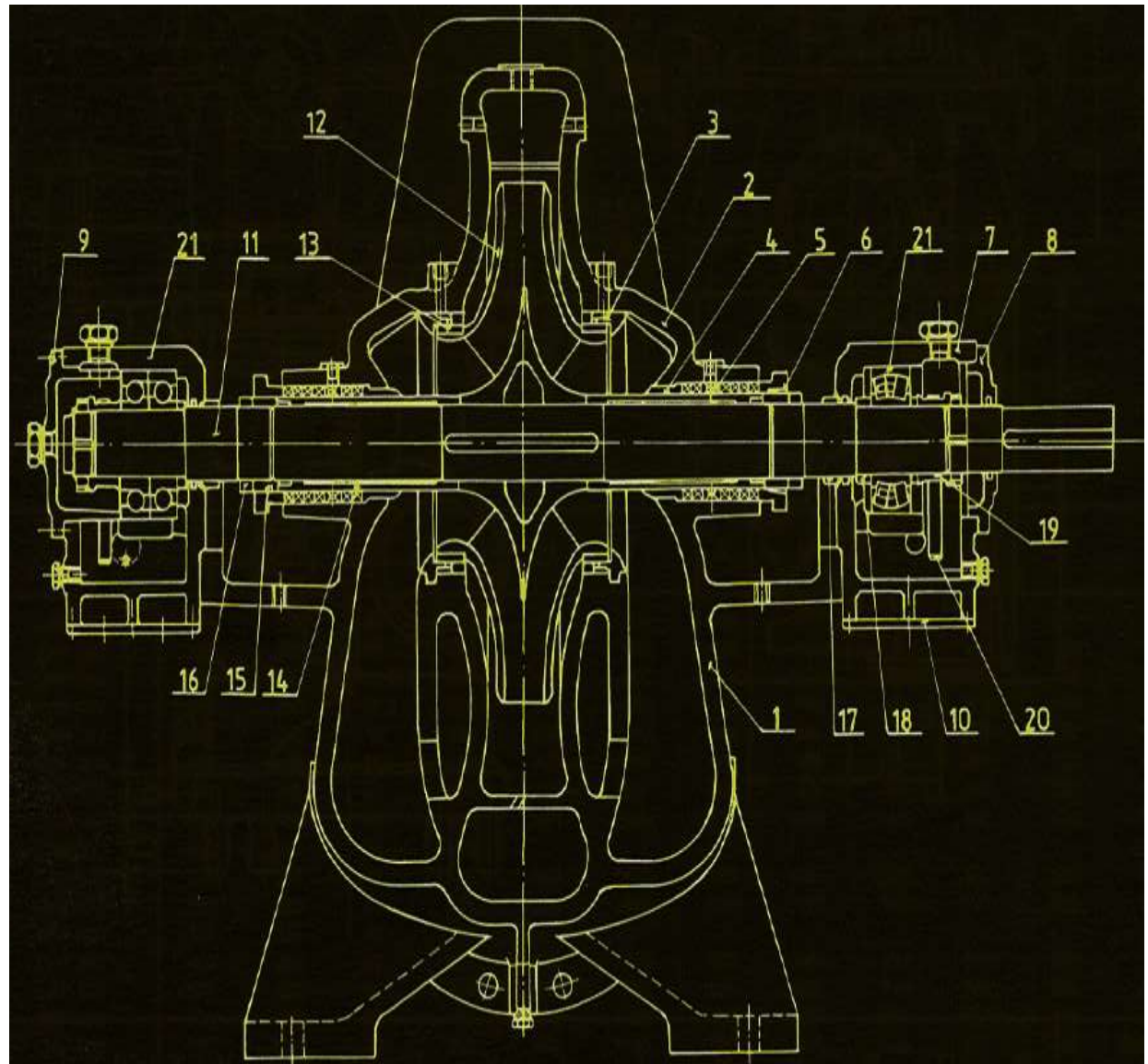


Pumps sectional drawing



pumps, typical sectional drawing

1. Casing half, lower
2. Casing half, upper
3. Casing wear ring
4. Neck bush
5. Lantern ring
6. Stuffing gland
7. Bearing housing
8. Bearing cover I.
9. Bearing cover II.
10. Cooling cover
11. Shaft
12. Impeller
13. Impeller ring
14. Shaft protecting sleeve
15. Shaft nut
16. Lock nut
17. Labyrinth ring
18. Shoulder ring
19. Distance sleeve
20. Lubrication ring
21. Bearing



Pumps, typical sectional drawing



SIMULATION SYSTEMS Ltd

**Centrifugal Pump
Disassembling Manual**

Learn objectives

After presentation of the topic D 630-90 pump disassembling trainee should be able to make the centrifugal one stage pump disassembling in accordance with "Technical conditions for workover job".

To see the next frame, click "Next" button, please.

Initial Pump Selection

Axial pumps

Axial-flow pumps with pull-out rotor and with blading adjustable during operation

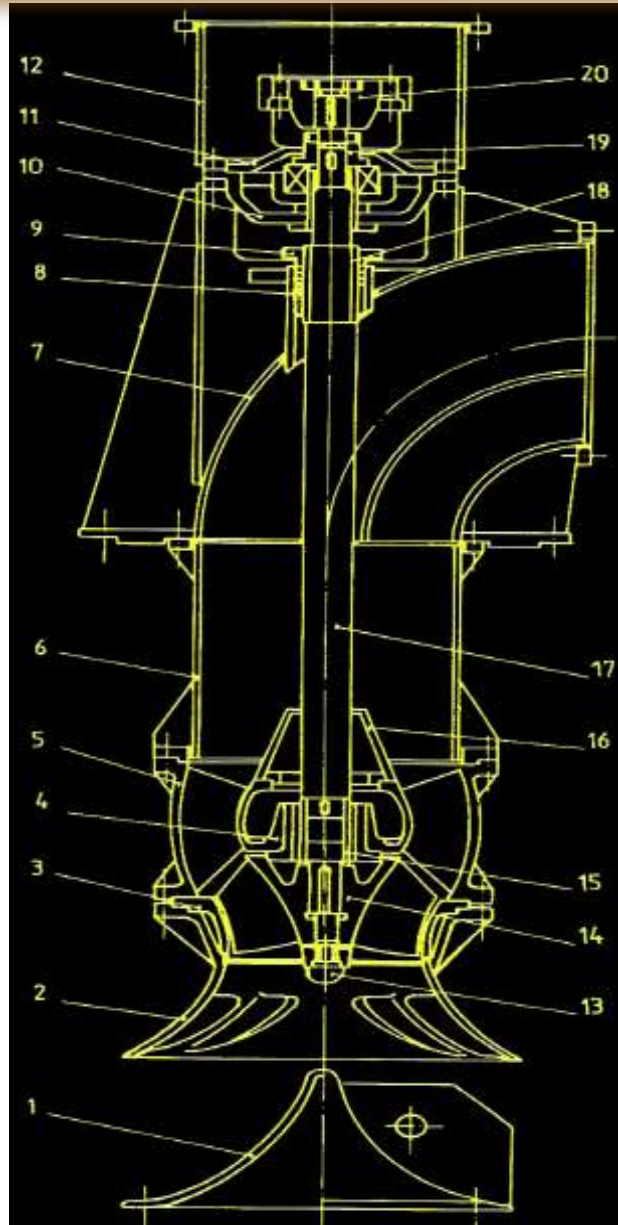


Initial Pump Selection

Mixed-flow pumps



Vertical shaft

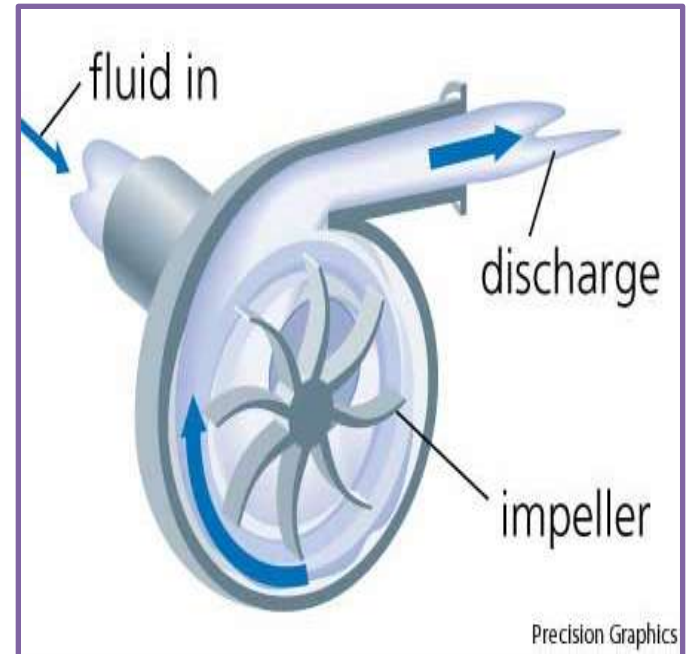


1. Suction cone
2. Suction bell
3. Wearing ring
4. Guide bearing casing
5. Guide vanes casing
6. Tube
7. Delivery elbow
8. Neck bush
9. Stuffing box
10. Thrust bearing casing
11. Thrust bearing cover
12. Motor stool
13. Cover
14. Shaft nut
15. Blade
16. Fixing plate
17. Impeller hub
18. Shaft sleeve
19. Shaft
20. Packing
21. Shaft sleeve
22. Oil retaining tube
23. Bearing bell
24. Coupling

ADVANTAGES OF CENTRIFUGAL PUMPS

Advantages

- Simple in construction and cheap
- Handle liquid with large amounts of solids
- No metal to metal fits
- No valves involved in pump operation
- Maintenance costs are lower

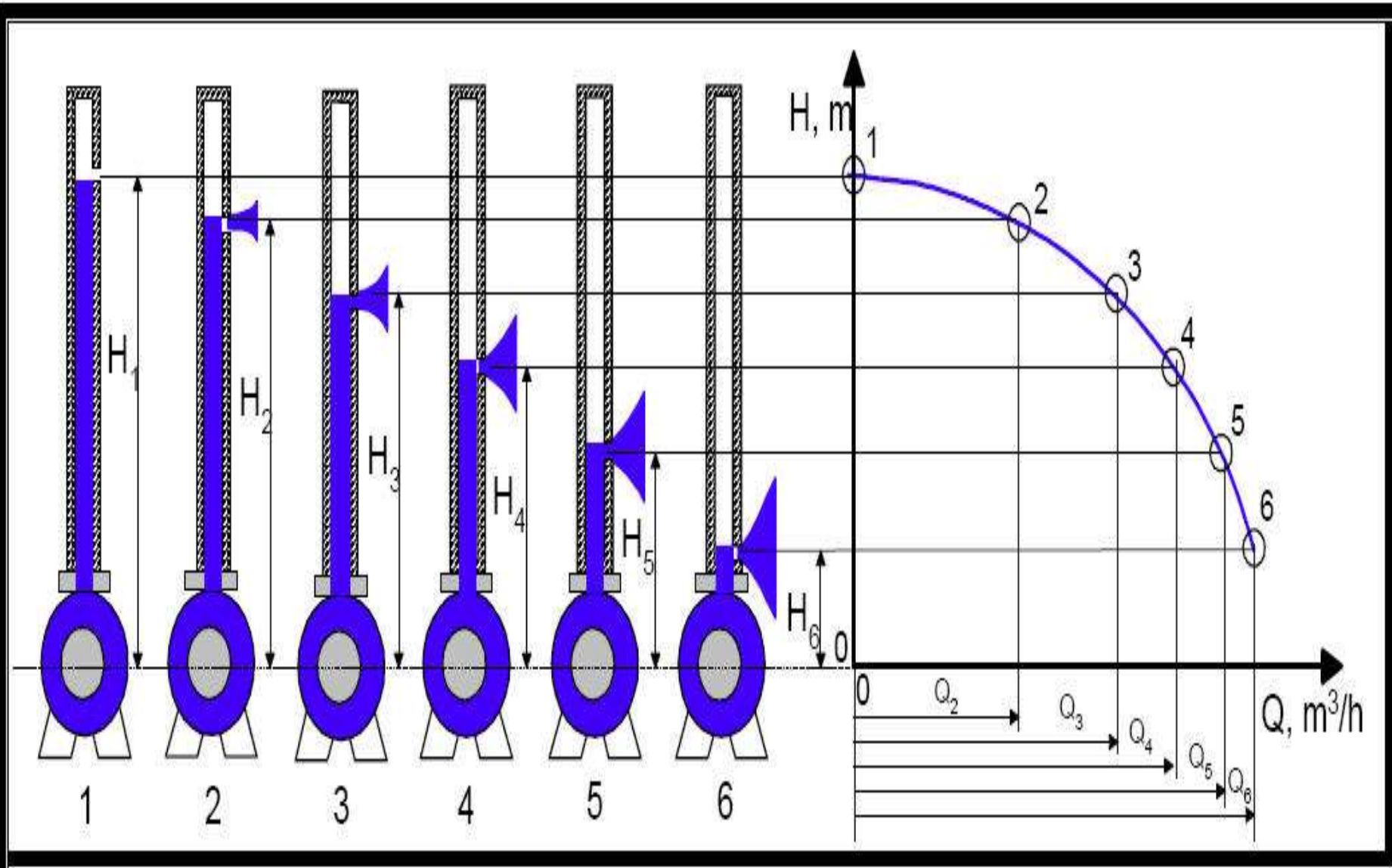


Disadvantages

Cannot handle highly viscous fluids efficiently
Cannot be operated at high heads
Maximum efficiency holds over a narrow range of conditions

Initial Pump Selection

HQ Curve



Initial Pump Selection

The amount of fluid power that a system consumes is a product of head and flow, according to this equation:

$$\text{Fluid power} = \frac{HQ (\text{s.g.})}{3,960}$$

where

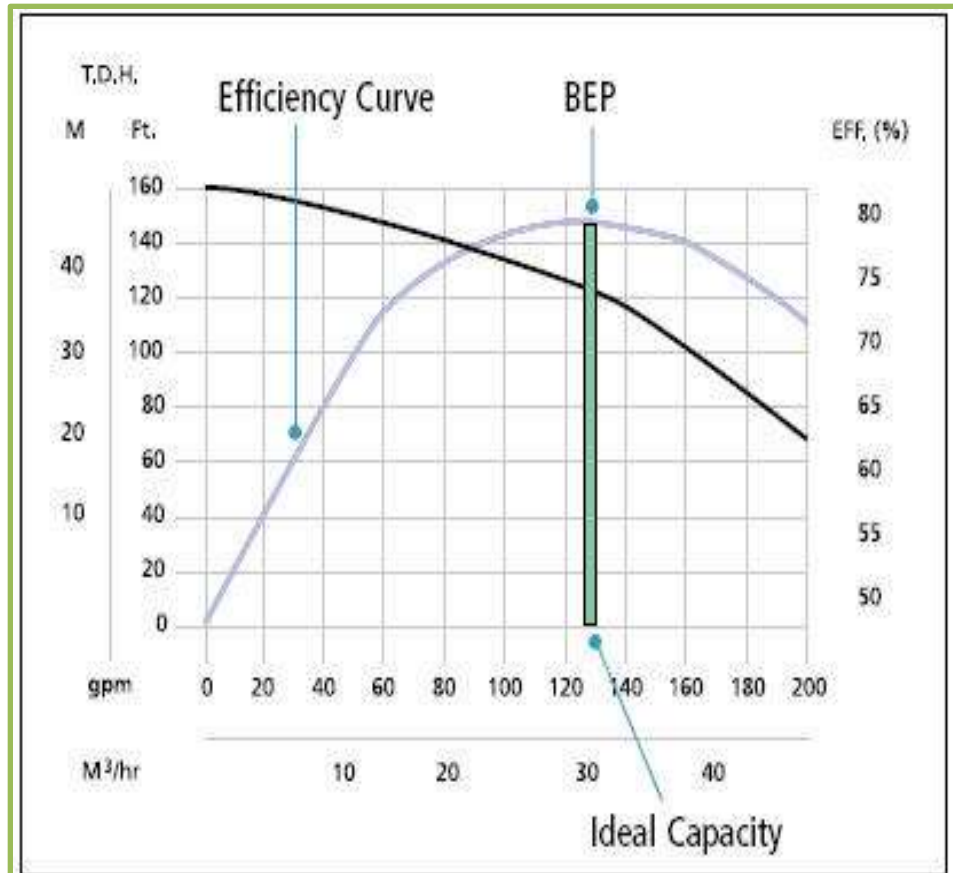
H = head (ft)

Q = flow rate (gallons per minute [gpm])

s.g. = specific gravity of the fluid

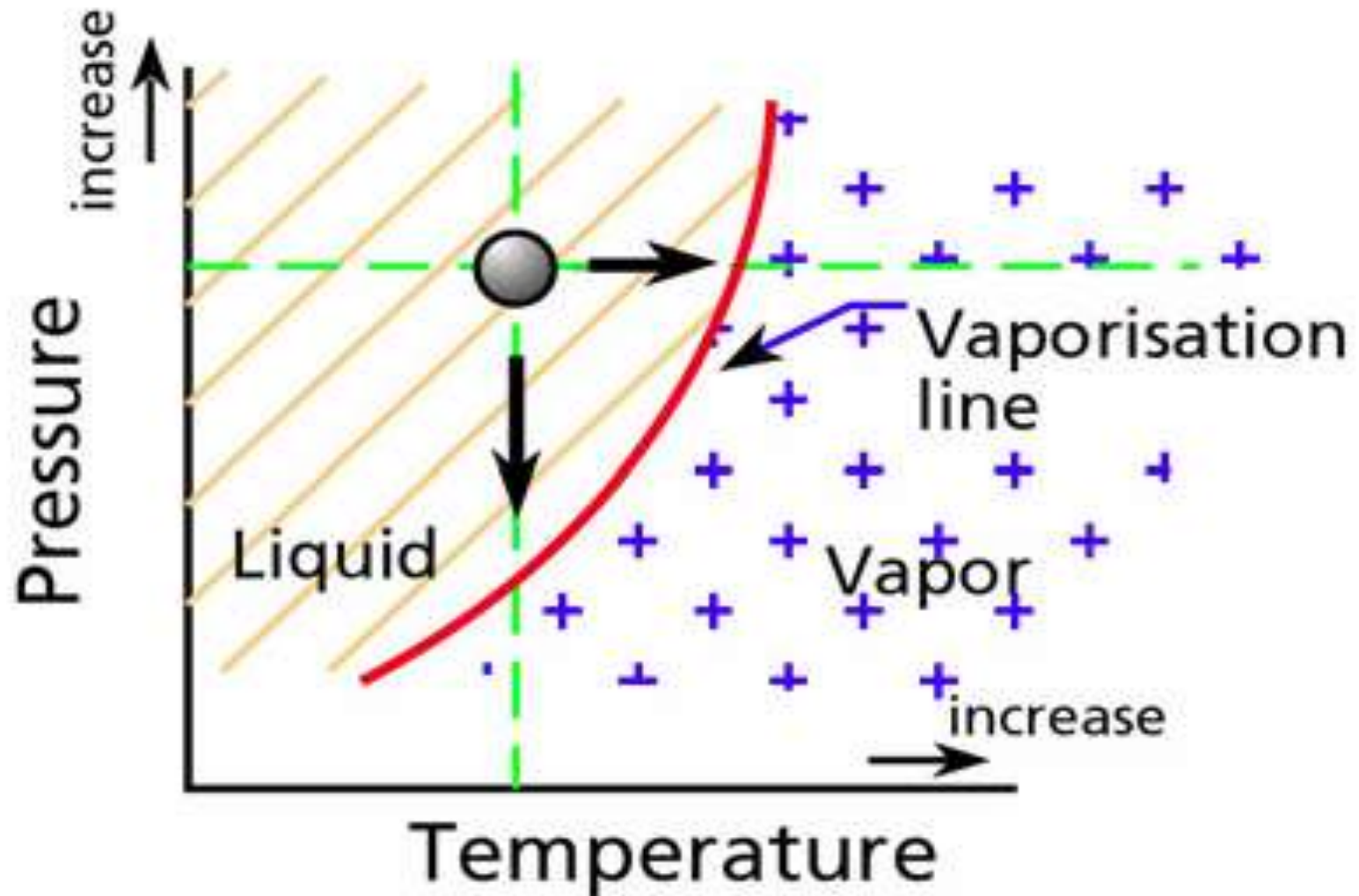
3,960 is a units conversion to state fluid power in terms of horsepower

The operating point of centrifugal pumps at which their efficiency is highest is known as the best efficiency point (BEP). Efficiencies range widely, from 35% to more than 90%, and they are a function of many design characteristics



Efficiency curve illustrating decreasing efficiencies as the capacity moves away from the ideal capacity and BEP

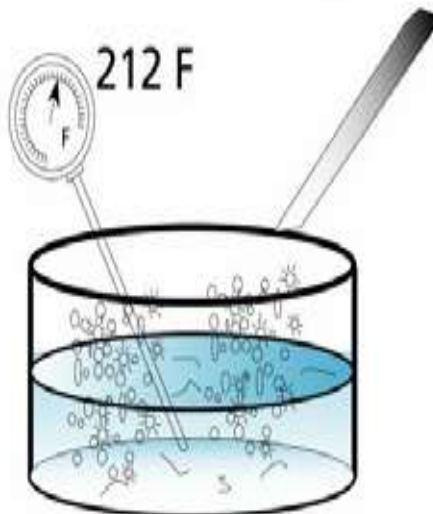
Vapor pressure vs. temperature



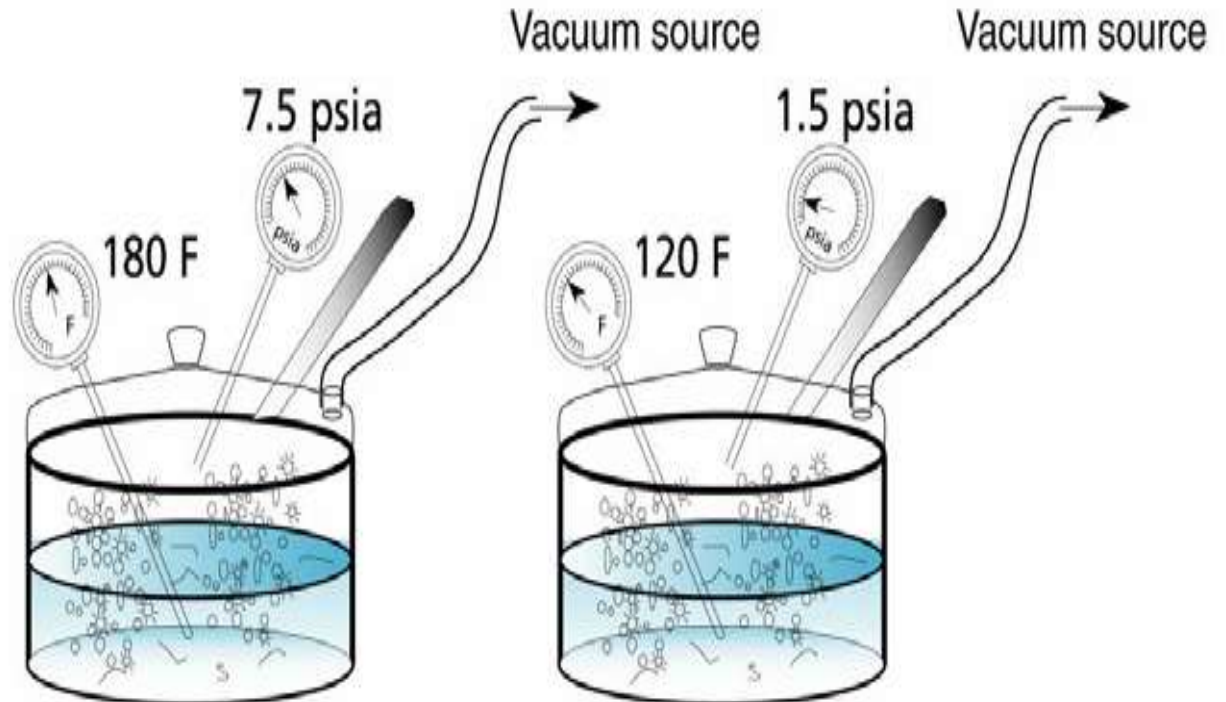
Boiling water with low pressure

Water boils at 212 F
when the pressure
is 14.7 psia

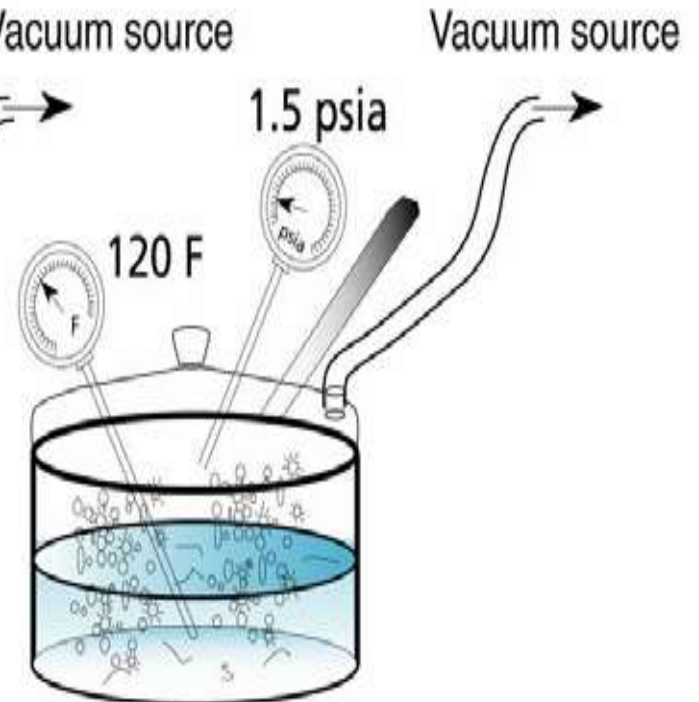
Atmospheric pressure
at sea level is 14.7 psia



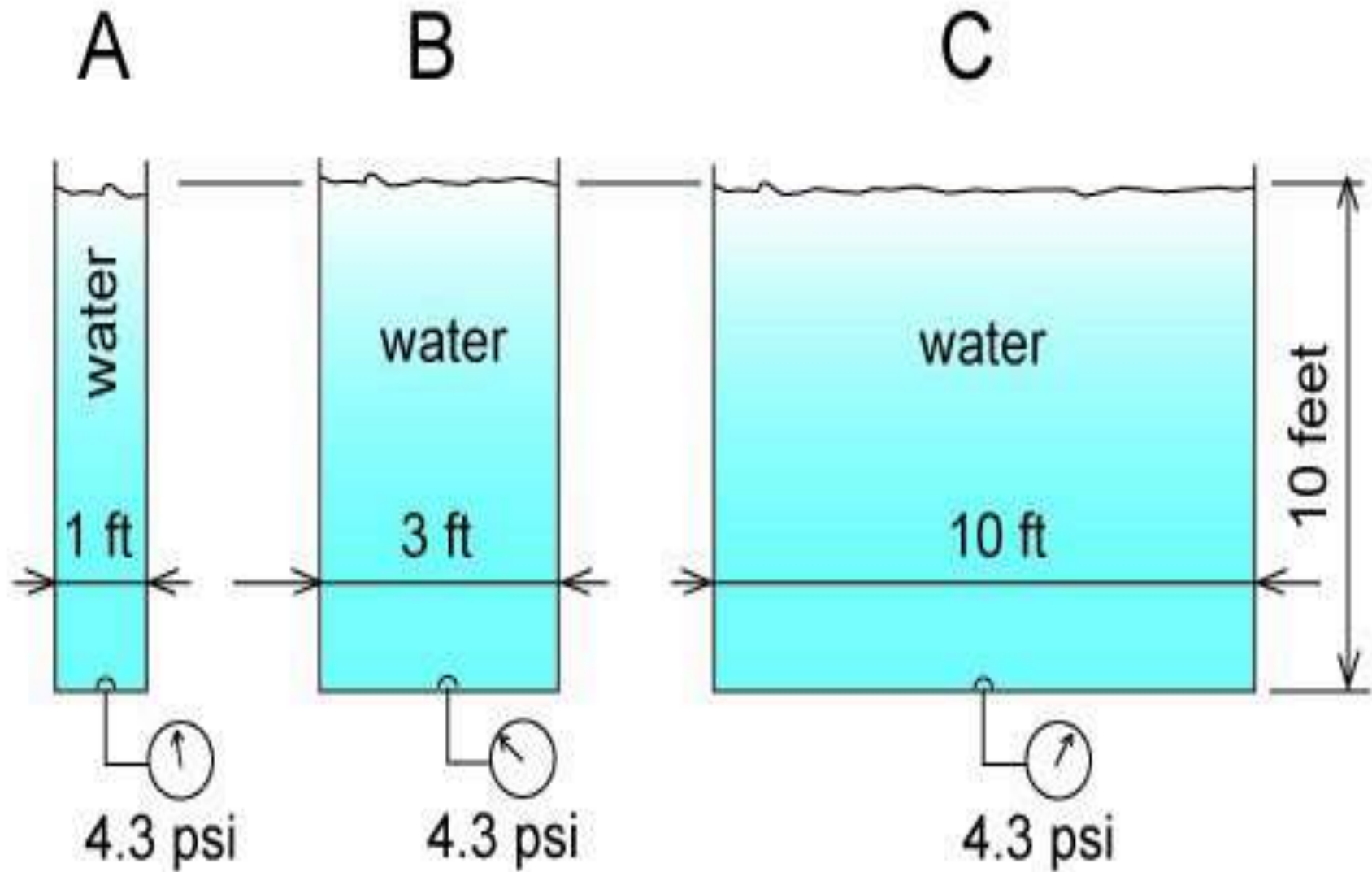
Water boil at 180 F
when the pressure
is 7.5 psia



Water boils at 120 F
when the pressure
is 1.5 psia



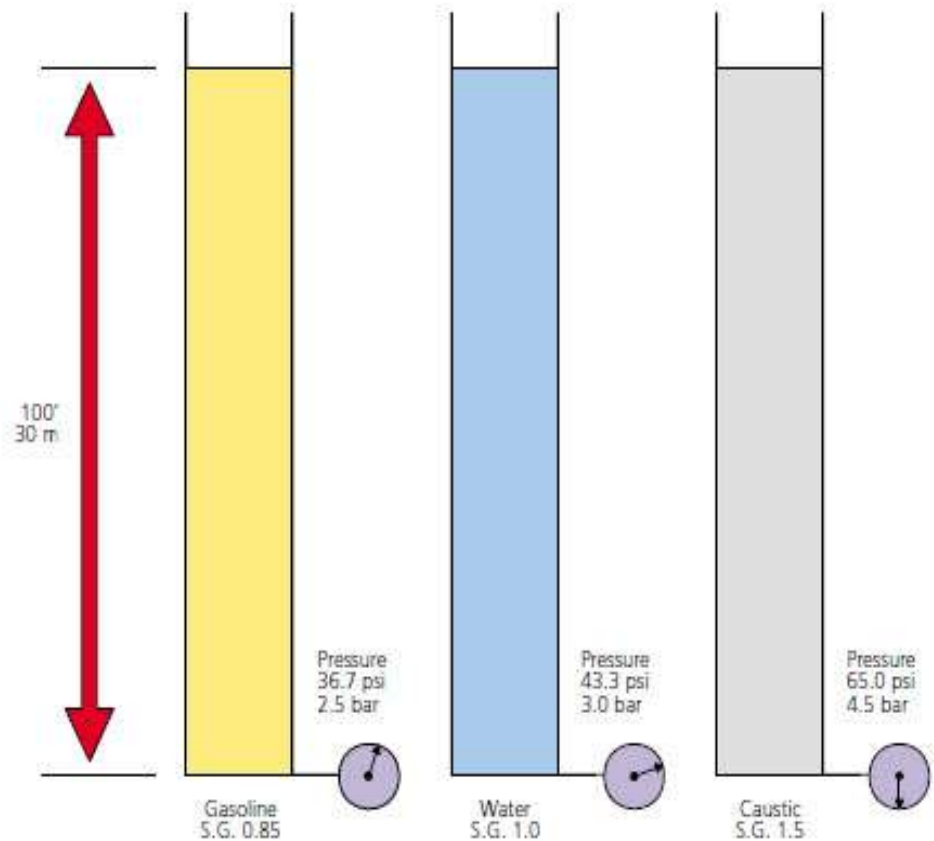
Pressure



Specific Gravity

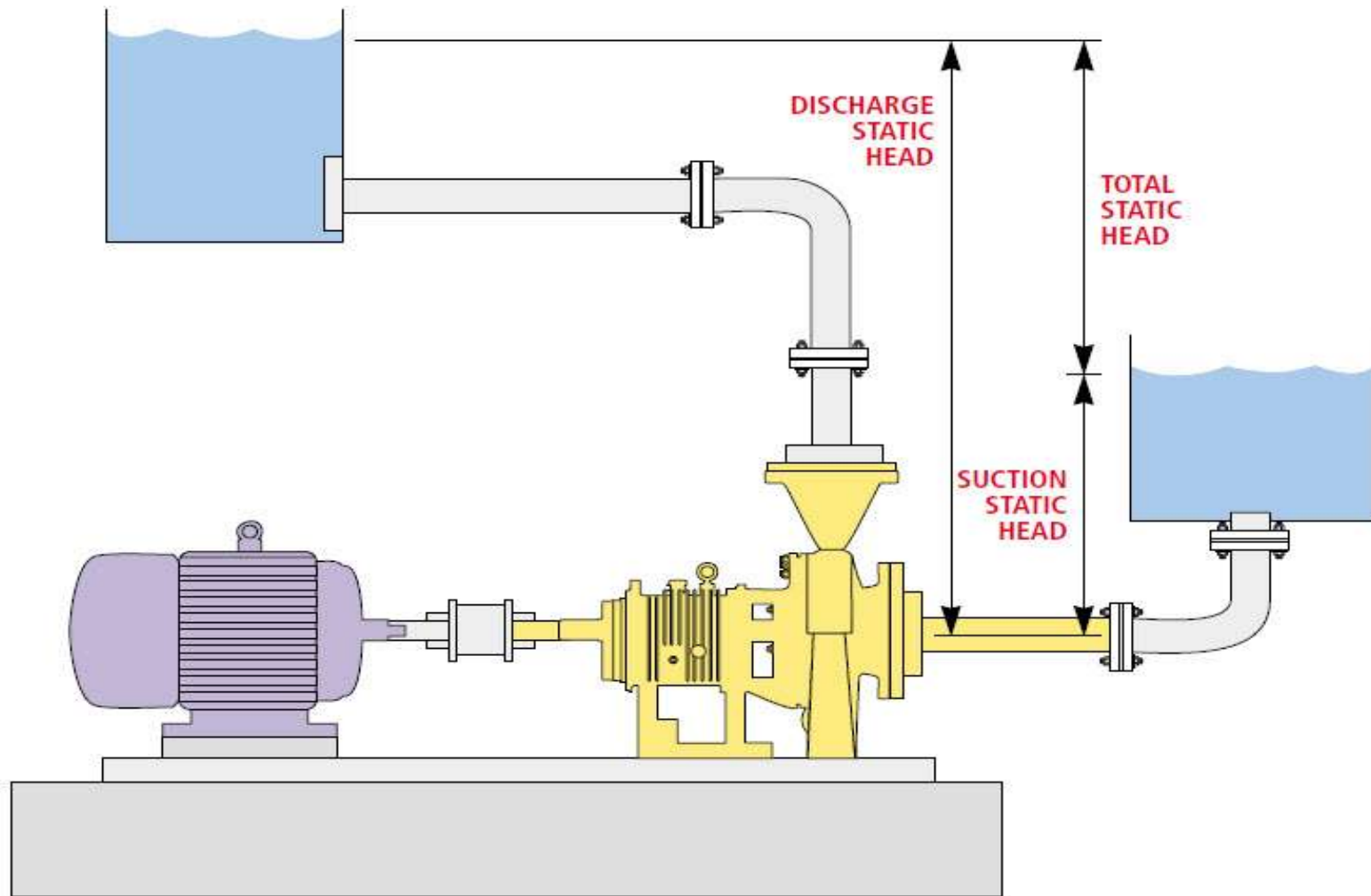
Specific gravity is the density ratio of a liquid as compared to water at a given temperature. Water is used as the standard at 14.69 psia (1.013 bar abs) and at 60°F (15.5°C).

Its specific gravity is 1.0 at this standard temperature and pressure.



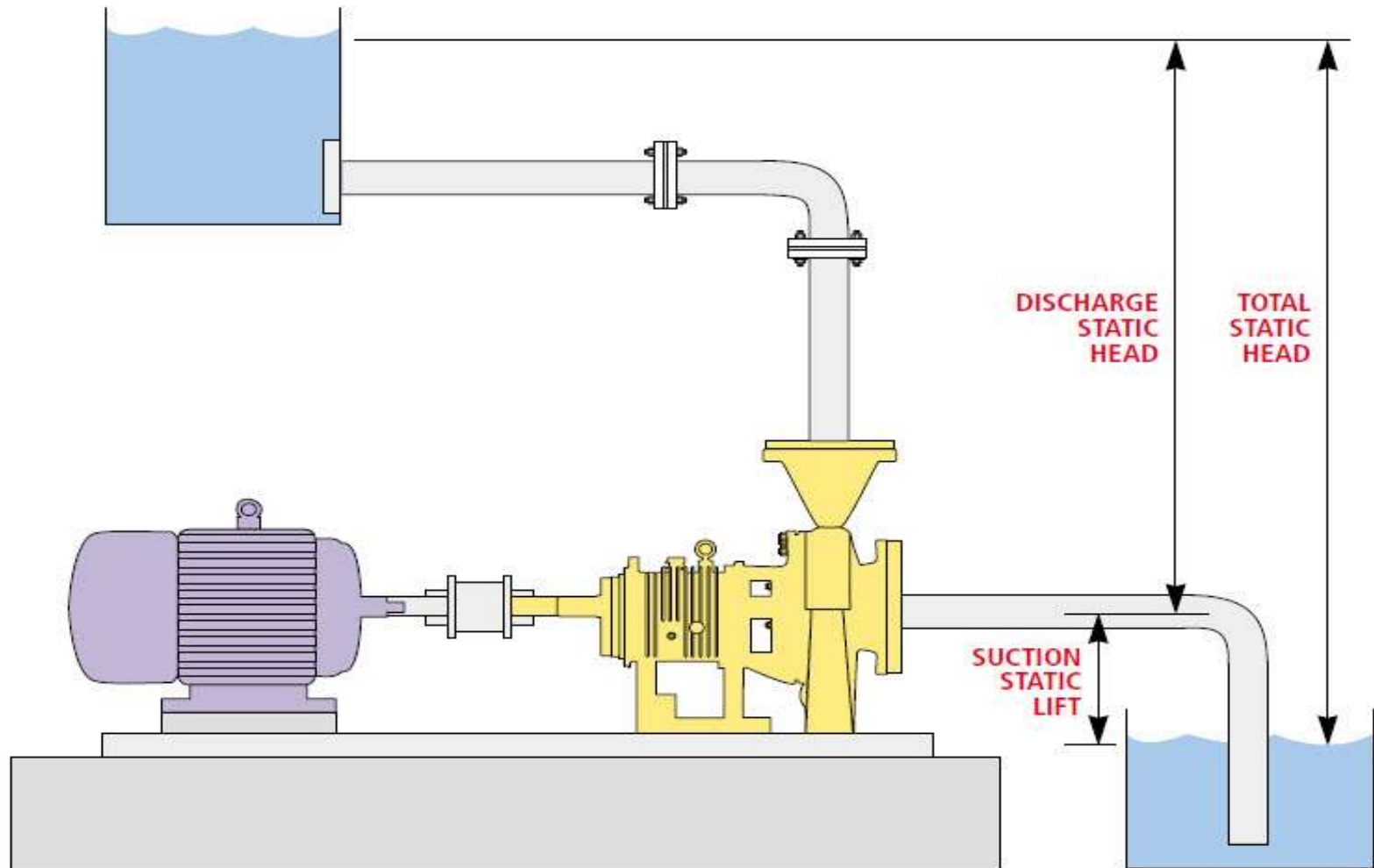
Initial Pump Selection

Static Head



Initial Pump Selection

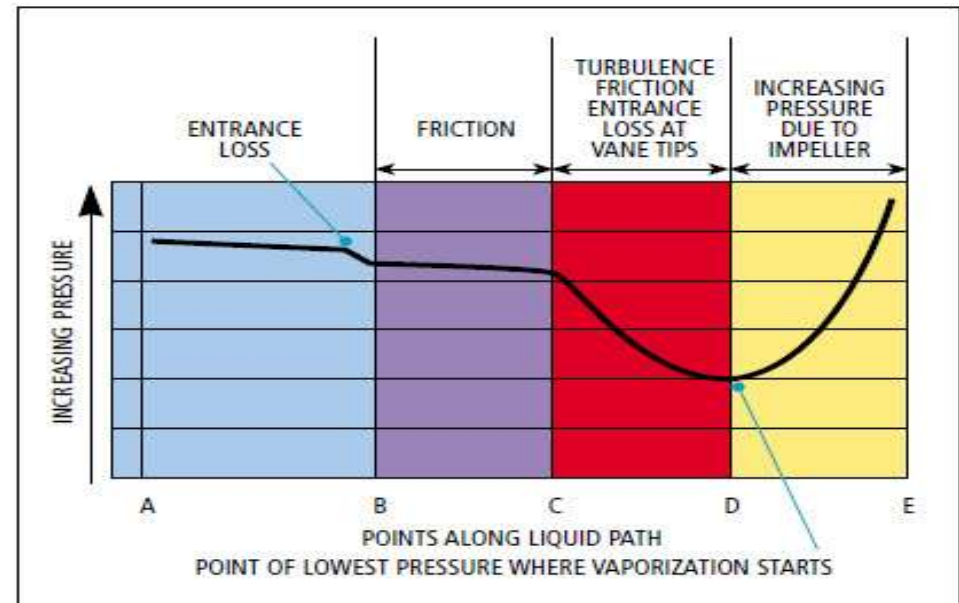
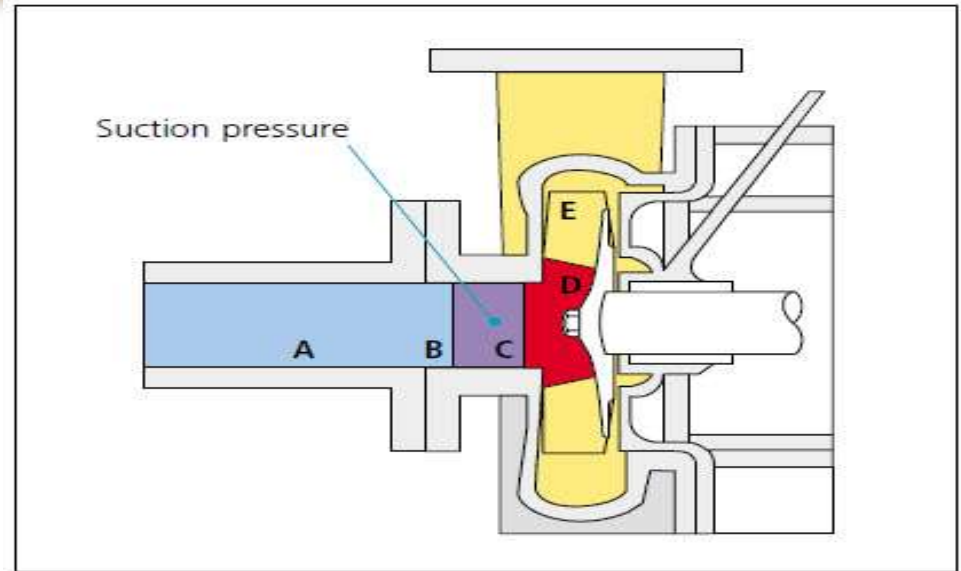
Static Lift



Net Positive Suction Head (NPSH)

is defined as the minimum hydraulic head condition in which a pump can meet its head and capacity requirements without the liquid vaporizing inside the pump.

Vaporization of the liquid causes cavitations. This cavitations reduces a pump's performance and may damage the pump.



Cavitations



Initial Pump Selection

$$\text{NPSHA} = \frac{2.31 (P_a - P_v)}{\text{spgr}} + (H_e - H_f)$$

where

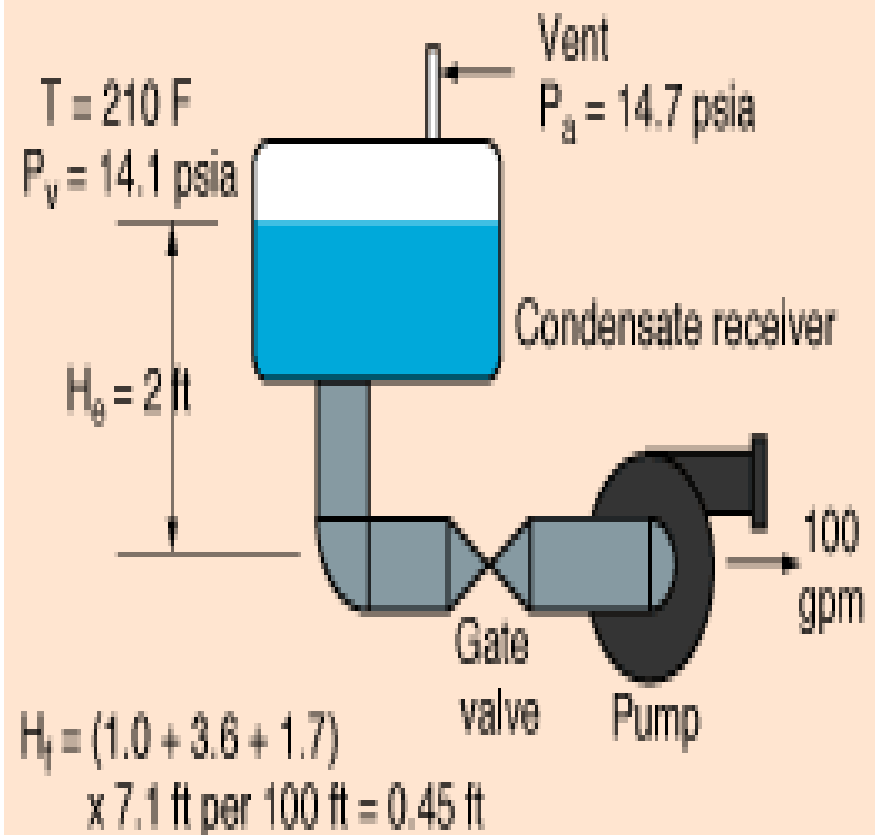
P_a = Pressure in the receiver, psia

P_v = Vapor pressure of the liquid at its maximum temperature, psia

H_e = Elevation head, ft.

H_f = Friction losses in the suction piping at the required flow rate, ft

spgr = Specific gravity

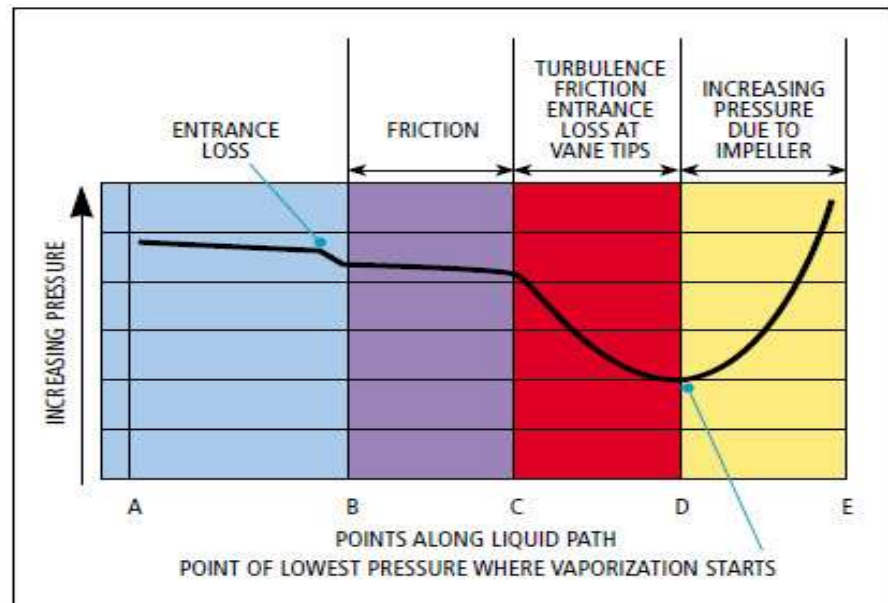
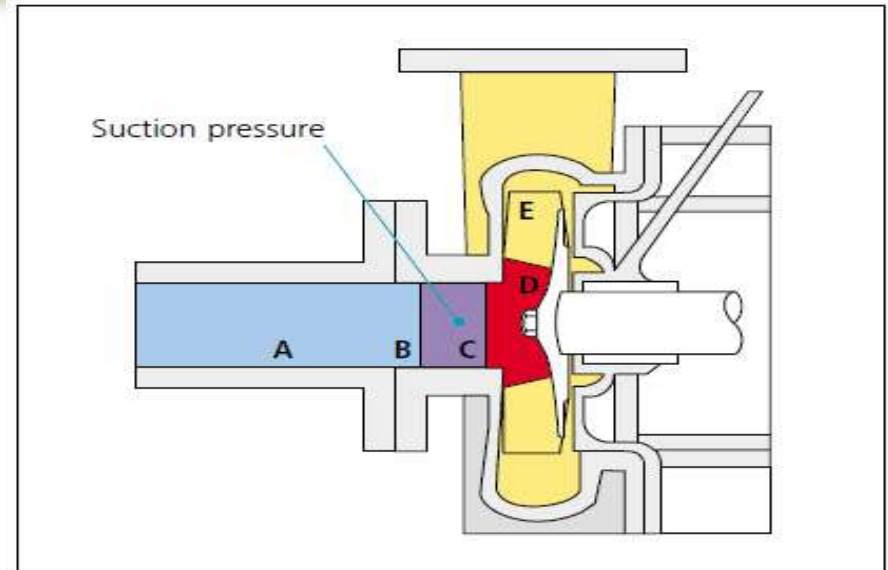


NPSH Available and NPSH Required

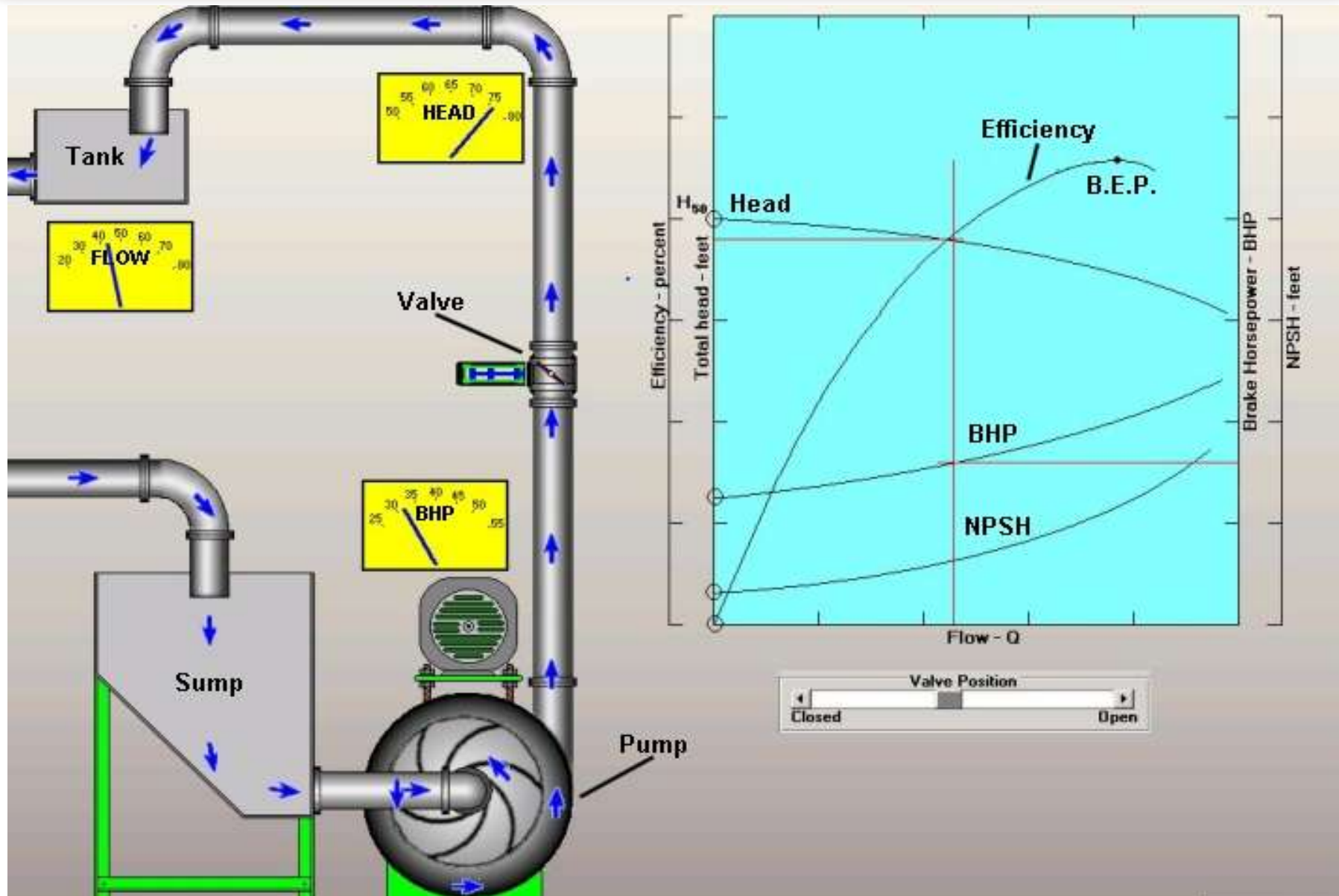
The standard tests for NPSHR tell us that even if NPSHA equals NPSHR there still is still a mild incipient cavitation occurring. Therefore, we need a little safety margin. A good margin to use is:

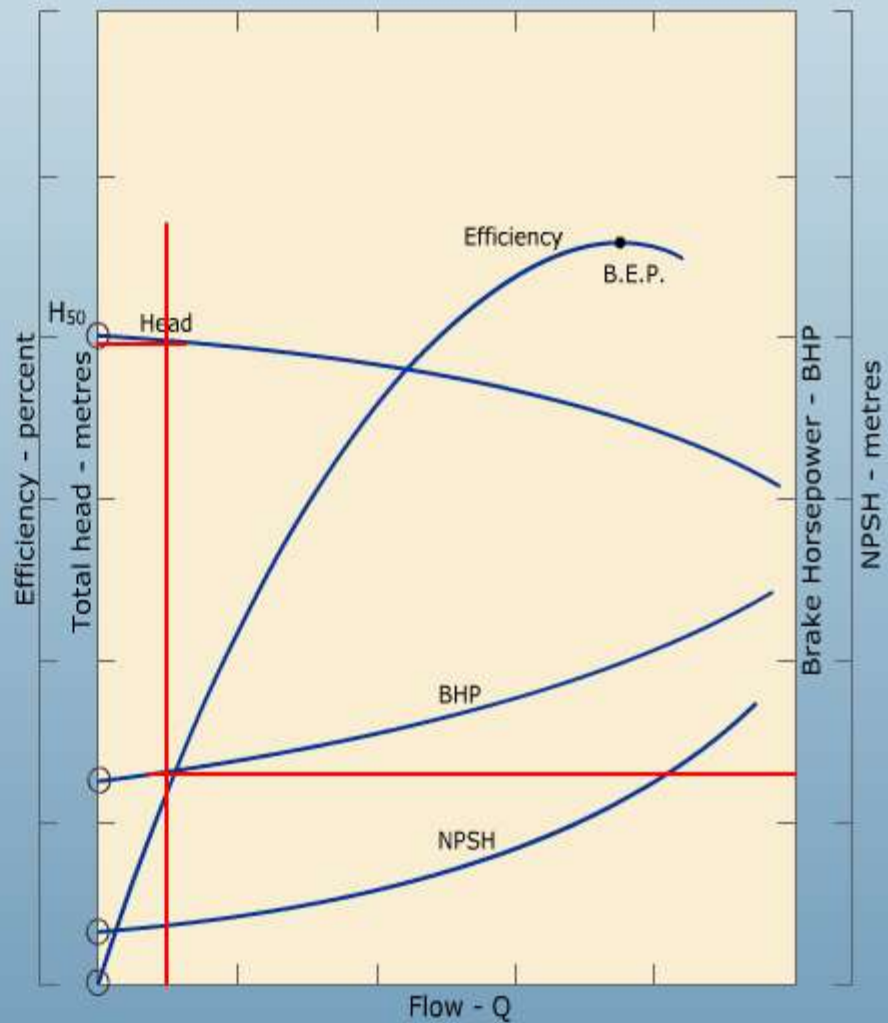
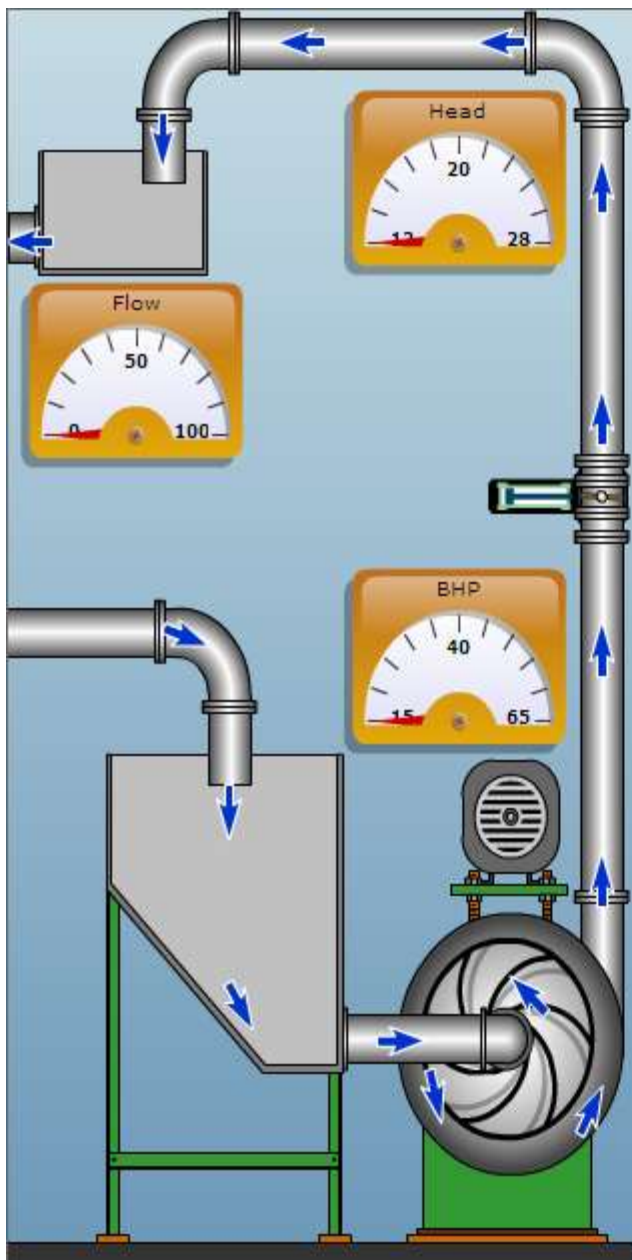
$$\text{NPSHA} > \text{NPSHR} + 3 \text{ ft. (1m)}$$

This margin can vary with pump type, impeller type, and fluid being pumped. However for most Overhung Impeller Centrifugal Pumps the 3 ft (1m) safety margin is usually satisfactory.



Initial Pump Selection





Valve Position

Closed Open

Narration

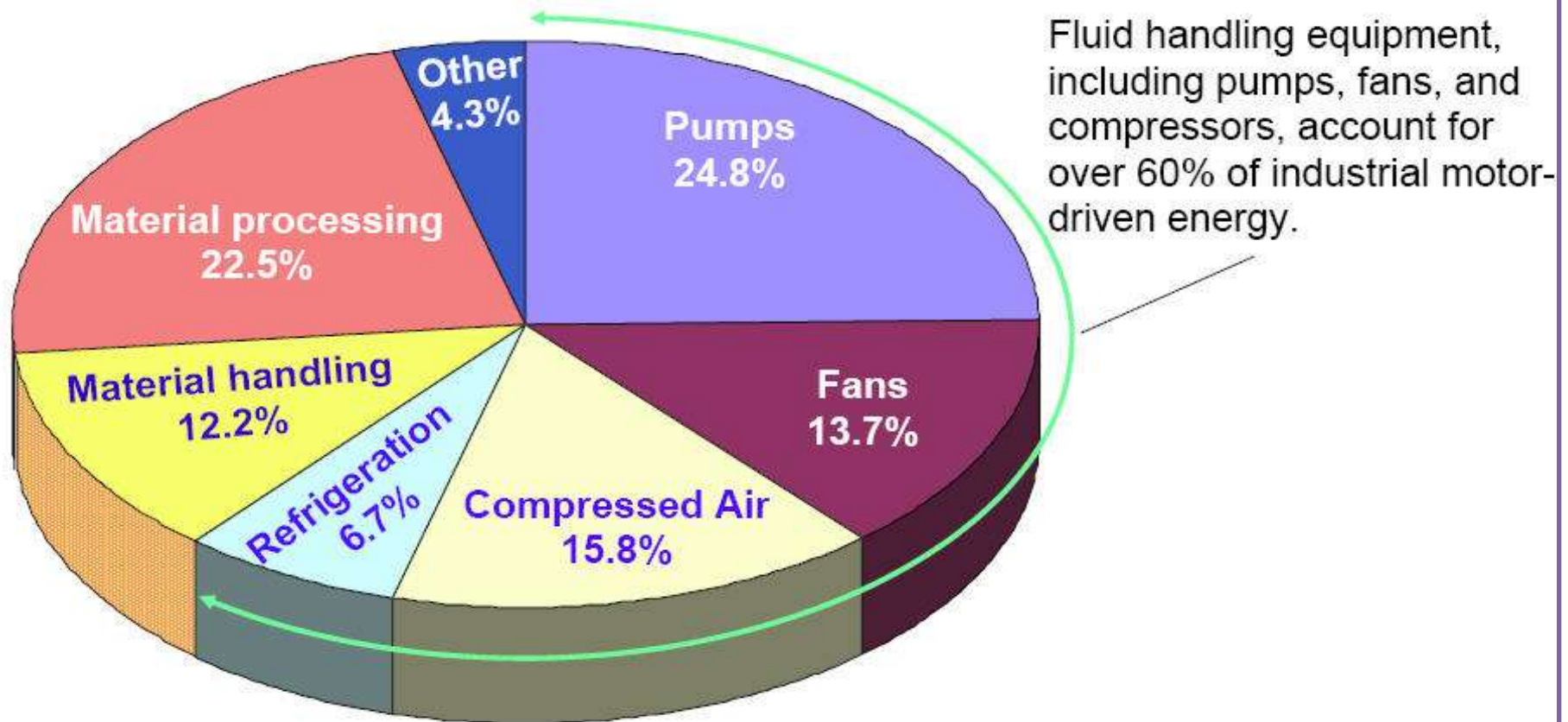
Prime Movers

Most pumps are driven by electric motors. Although some pumps are driven by direct current (dc) motors, the low cost and high reliability of alternating current (ac) motors make them the most common type of pump prime mover.



Prime Movers

Pumps are the largest industrial user of motor-driven electrical energy





Piping

Piping is used to contain the fluid and carry it from the pump to the point of use.

aspects of piping are its dimensions, material type, and cost.

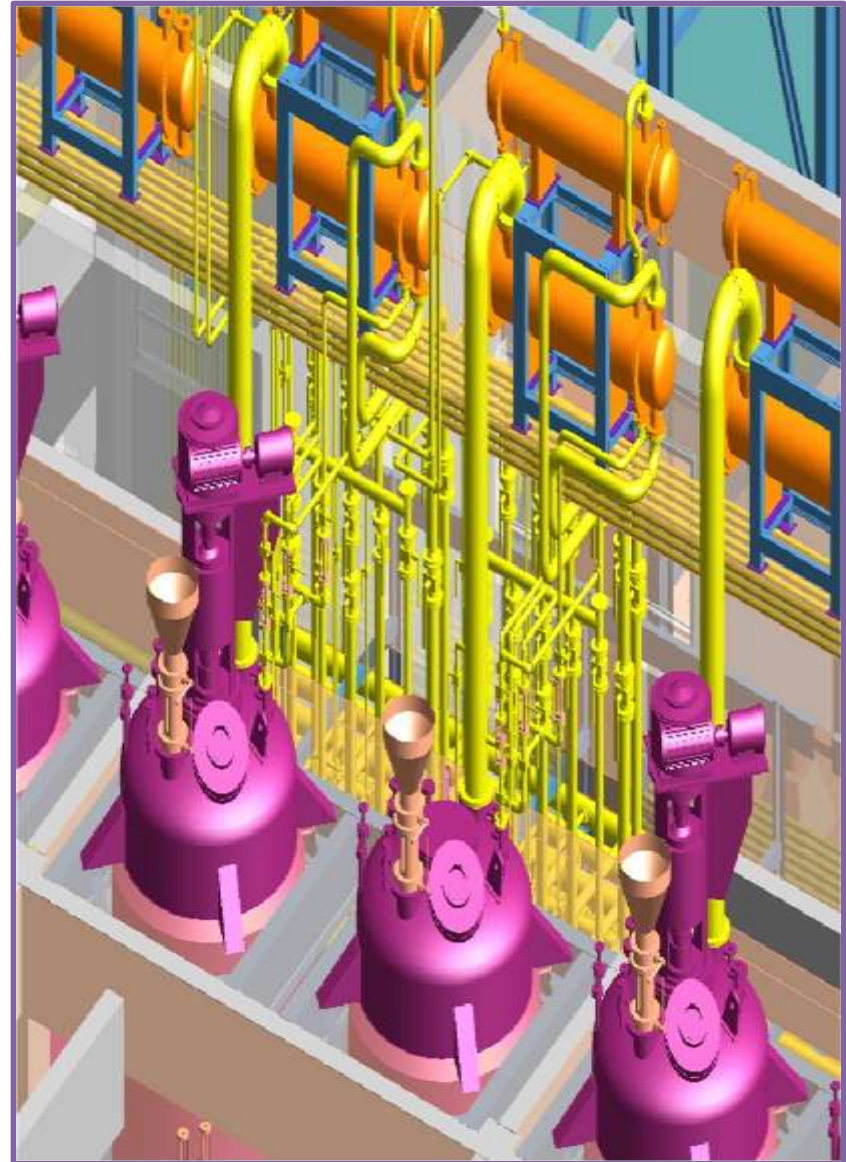
The flow resistance at a specified flow rate of a pipe decreases as the pipe diameter gets larger; however, larger pipes are heavier, take up more floor space, and cost more than smaller pipe.



Piping

In systems that operate at high pressures small-diameter pipes can have thinner walls than large-diameter pipes and are easier to route and install.

Small-diameter pipes restrict flow, can be especially problematic in systems with surging flow characteristics. Smaller pipes also operate at higher liquid velocity, increasing erosion effects, wear, and friction head. Increased friction head affects the energy required for pumping



Valves

The flow in a pumping system may be controlled by valves.

Some valves have:

distinct positions.

shut or open.

throttle flow.

selecting the correct valve for an application depends on:

ease of maintenance.

Reliability.

leakage tendencies.

Cost.

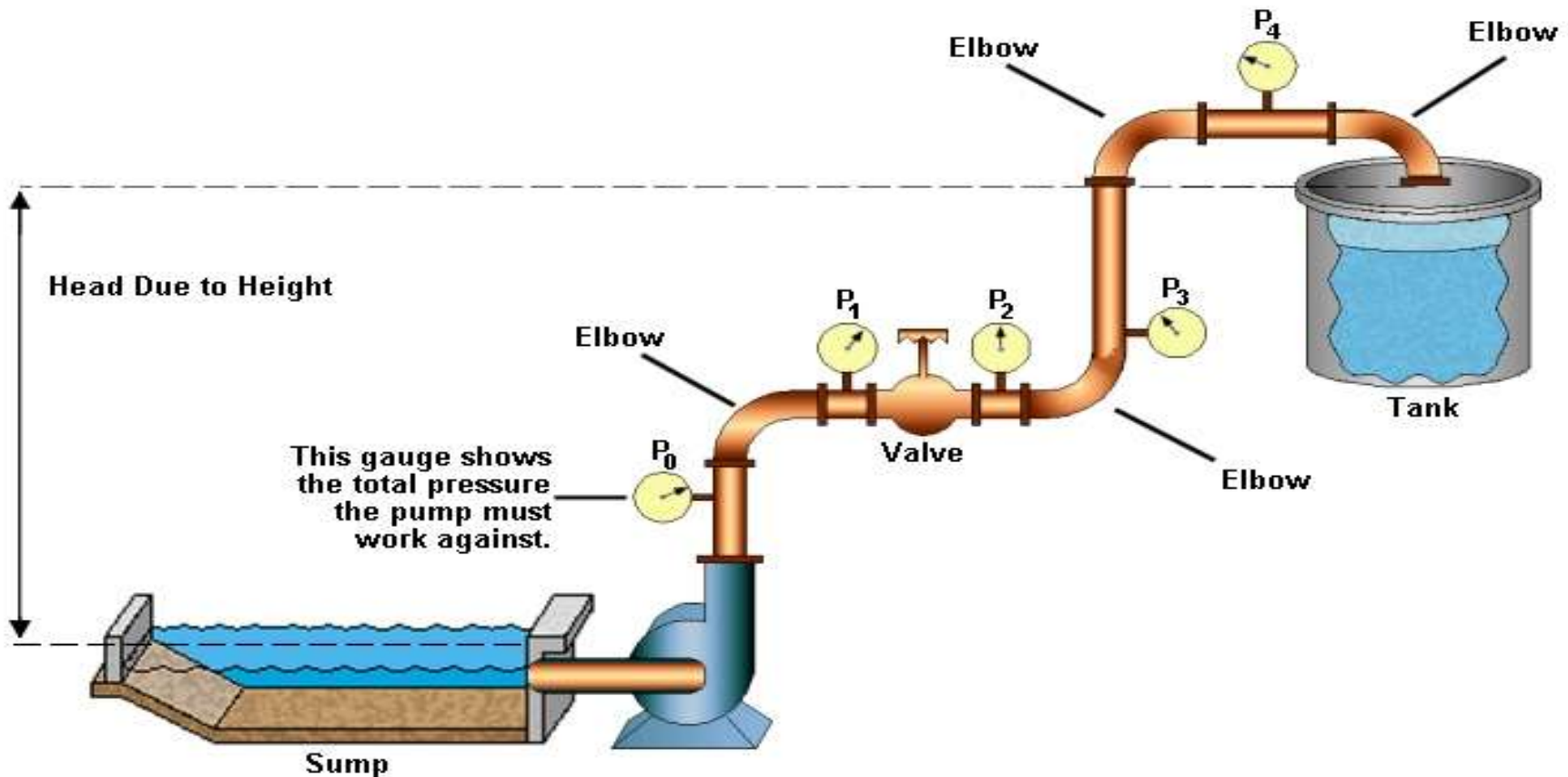
frequency with which the valve will be open and shut.



Valves

End-Use Equipment

The essential purpose of a pumping system may be to provide cooling, to supply or drain a tank or reservoir, or to provide hydraulic power to a machine.



Pumping System Basics

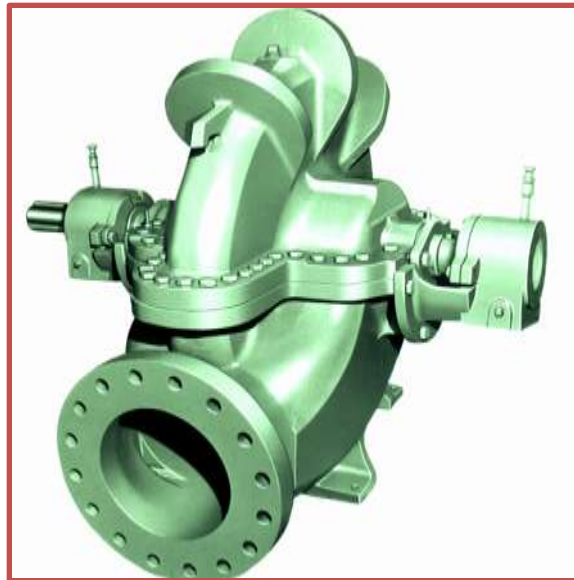


Design Practices

Fluid system designs are usually developed to support the needs of other systems.

In cooling system applications, the requirements flow is determine. Pump capabilities are then calculated based on the system layout and equipment characteristics

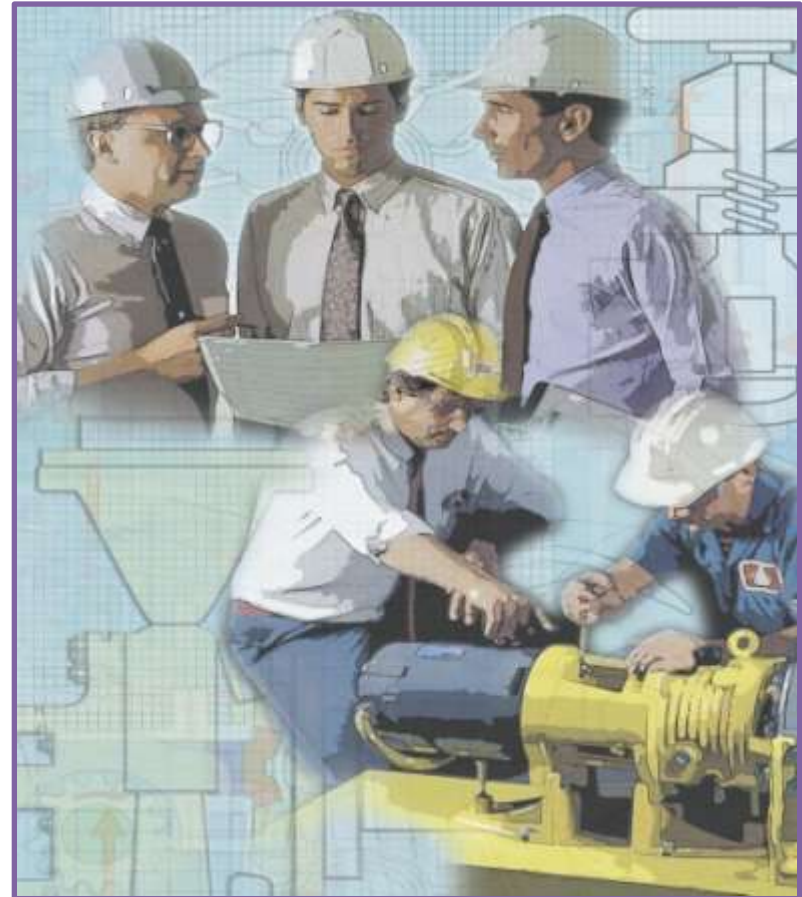
The most challenging aspect of the design process is cost-effectively matching the pump and motor characteristics to the needs of the system



Analyzing System Requirements

fully understand system requirements
(peak demand, average demand, and the variability of demand)
with respect to time of day and time of year

Problems with oversized pumps often develop because the system is designed for peak loads, while normal operating loads are much smaller. Excess flow energy is then forced into the system. In addition to increasing operating costs, this excess flow energy creates unnecessary wear on components such as valves, piping, and piping supports.



Initial Pump Selection

Pump selection starts with a
basic knowledge of:

System operating conditions.

Fluid properties.

Pressures.

Temperatures.

System layout.

System Operating Costs.

These conditions determine the
type of pump that is required to
meet certain service needs.

positive displacement

centrifugal.

Axial flow pumps

flow rate and head!

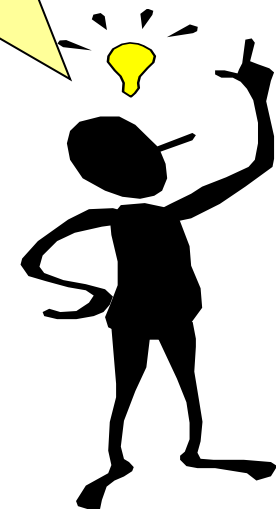
efficiency

suction inlet conditions

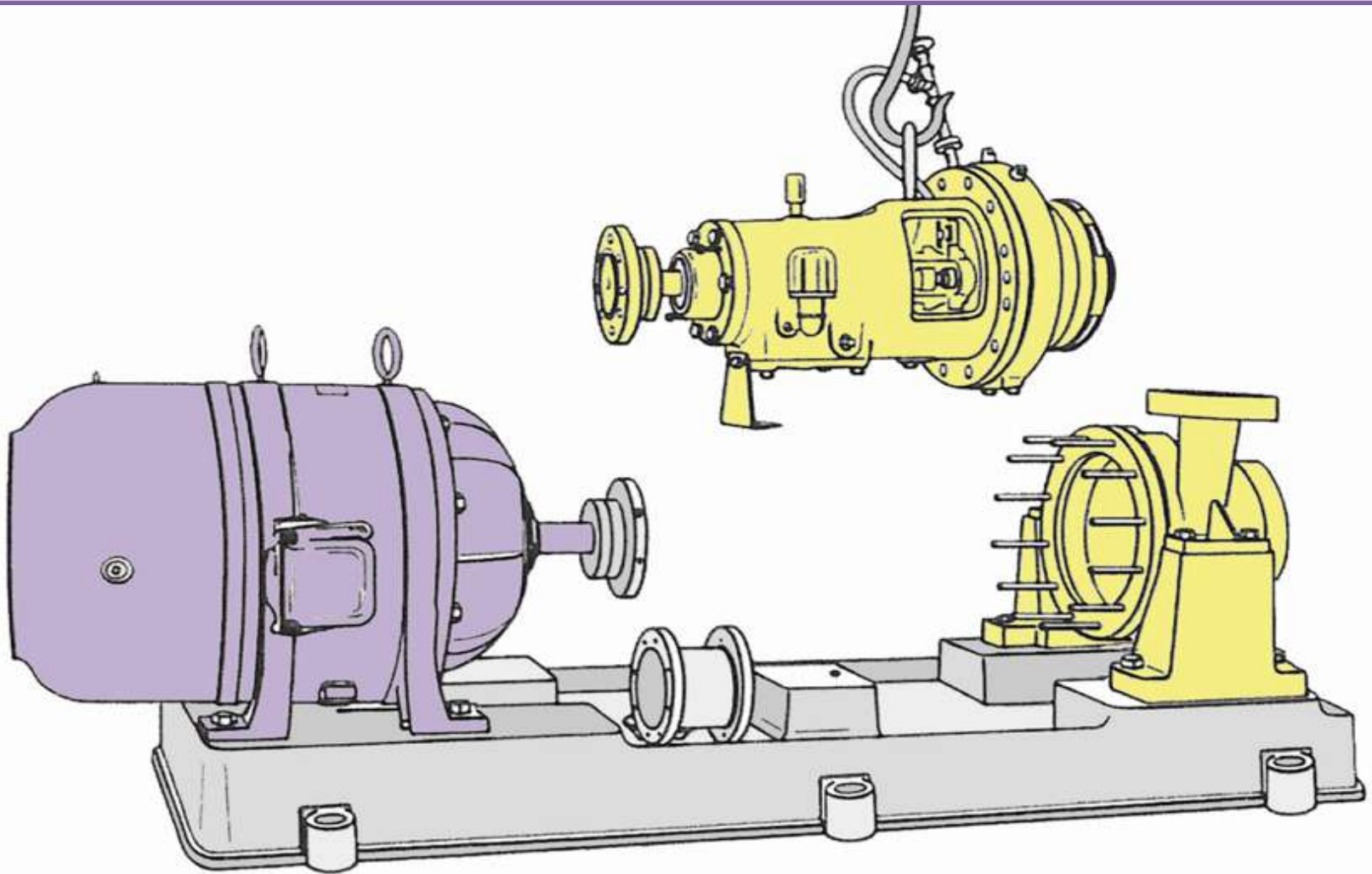
operating life

maintenance.

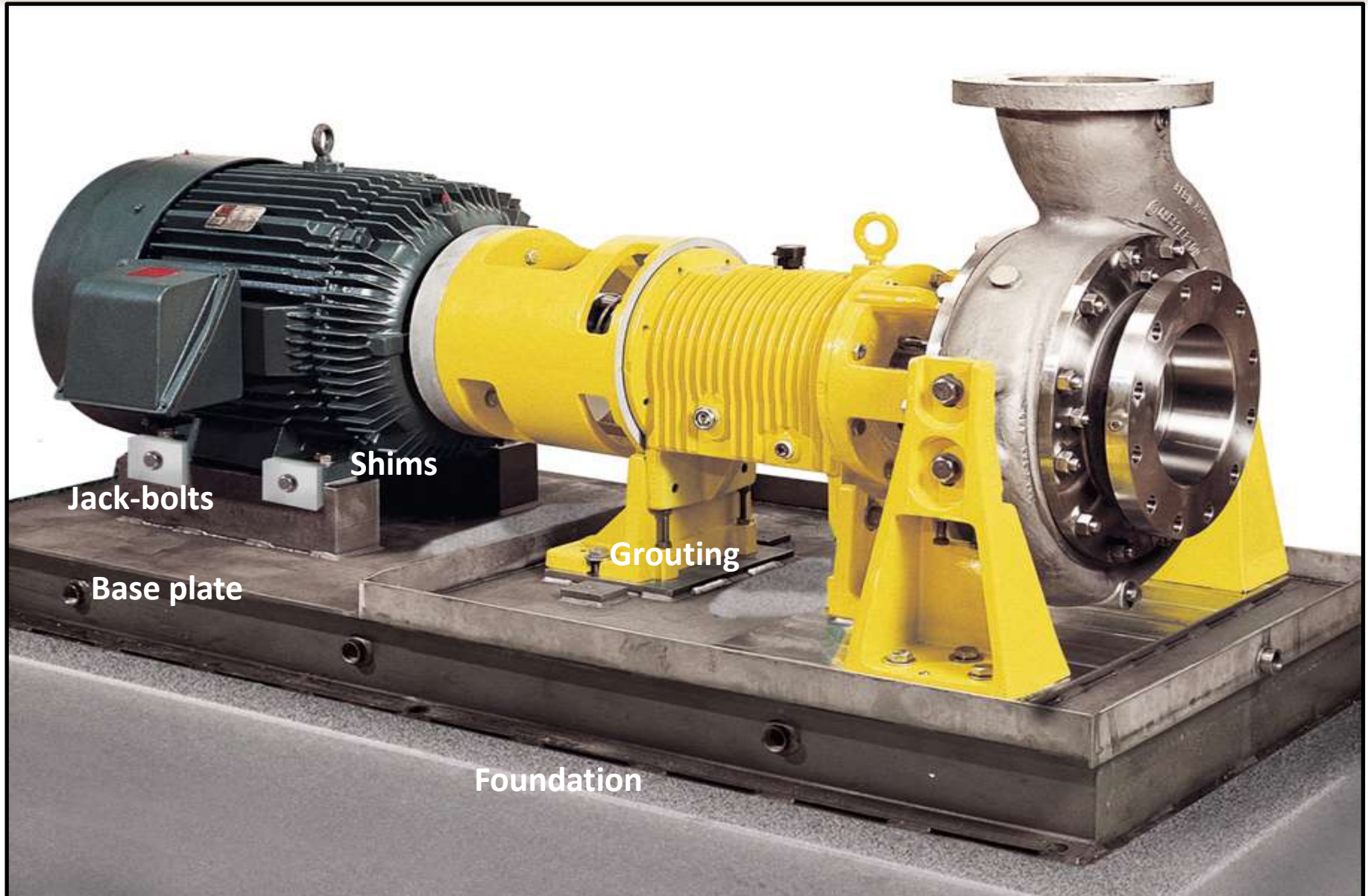
Costs



Pumps Installation

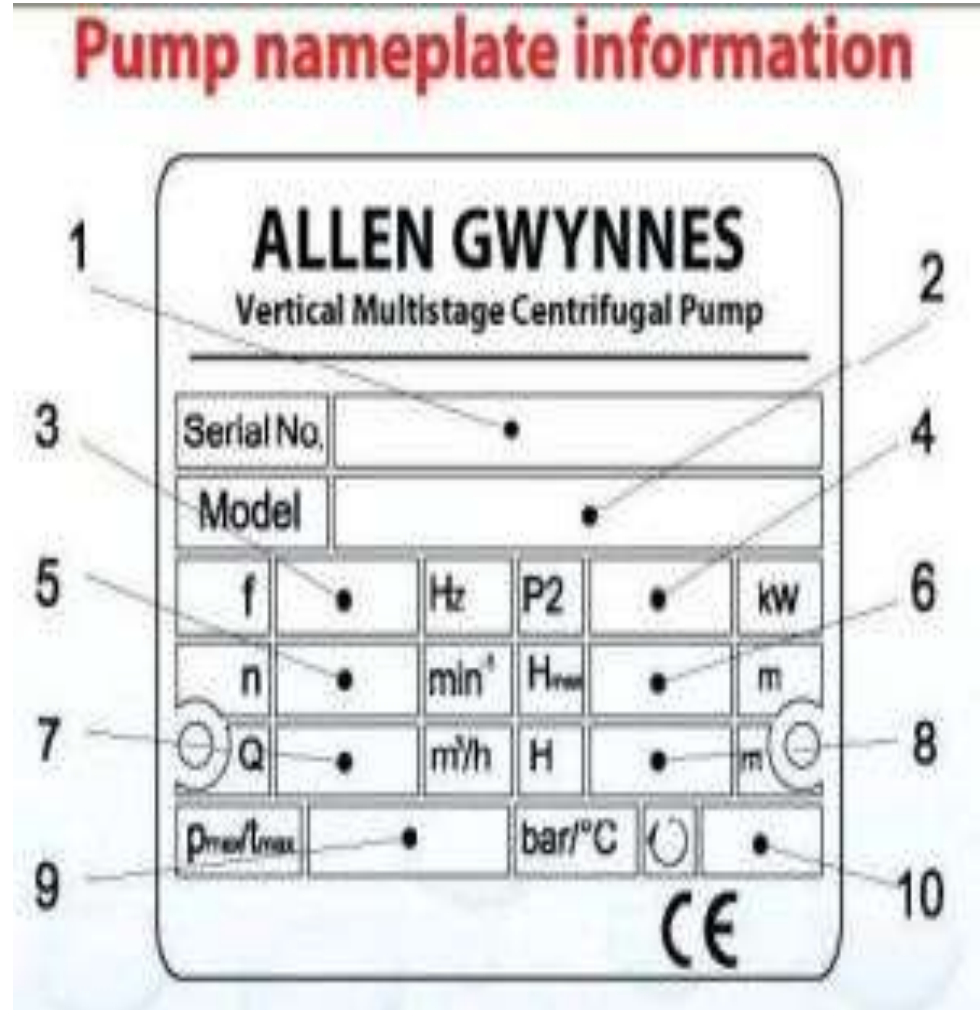


Pumps Installation



Pump nameplate information

1. Serial number
2. Pump Model
3. Frequency
4. Rated Power
5. Speed
6. Maximum Head
7. Capacity
8. Head Range
9. Maximum Operating Pressure
10. Rotating Direction



Transport, Handling

- 1-Check the pump/pump unit immediately upon delivery/receipt of dispatch for damage or missing parts.
- 2-The pump/pump unit must be transported carefully and by competent personnel. Avoid serious impacts.
- 3-Keep the pump/pump unit in the same position in which it was supplied from the factory.
- 4-Take note of the instructions on the packaging.
- 5-The intake and discharge side of the pump must be closed with plugs during transport and storage



Transport, Handling



Dispose of all packing materials in accordance with local regulations.

6-Lifting devices (e.g. fork-lift truck, crane, crane device, pulleys, sling ropes, etc.) must be sufficiently strong and must only be used by authorized persons.

7-The weight of the pump/pump unit is given in the Data Sheet.

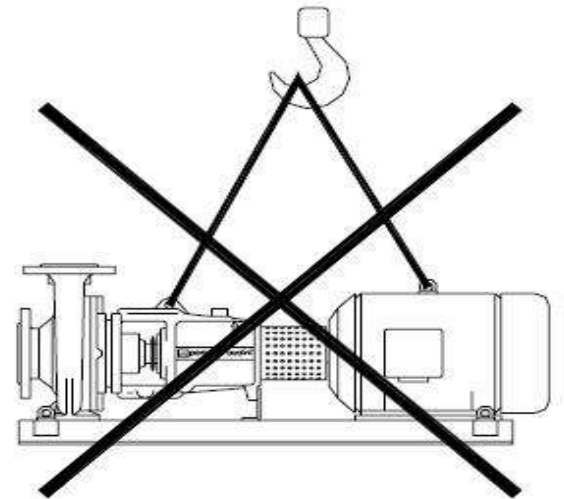
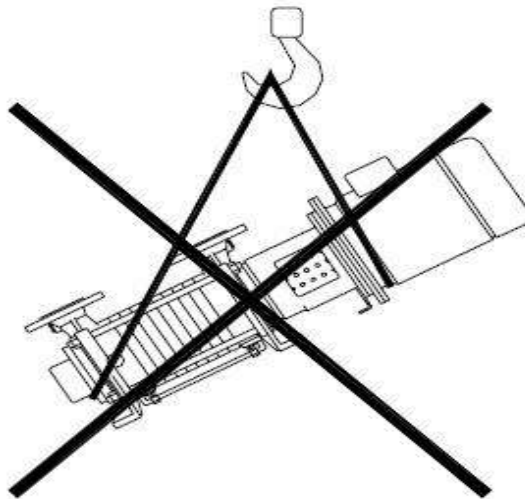
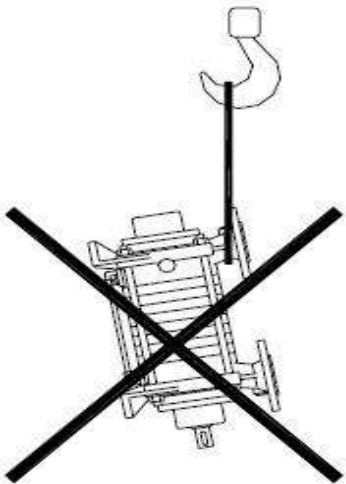
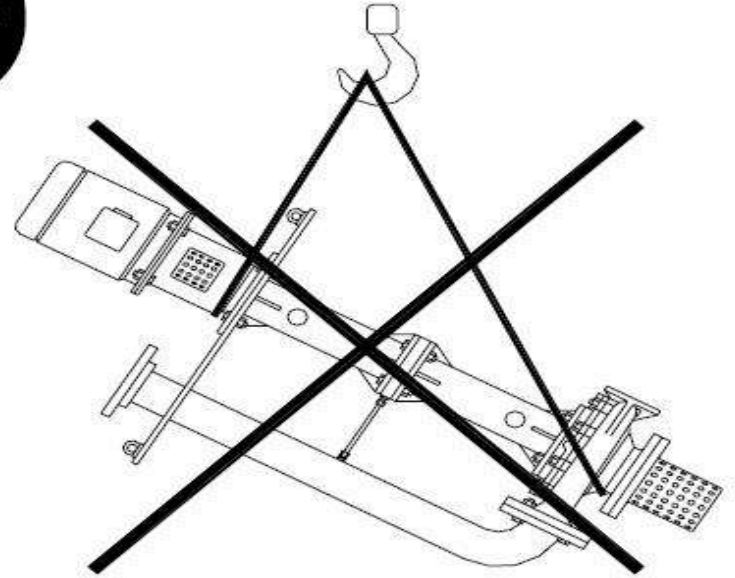
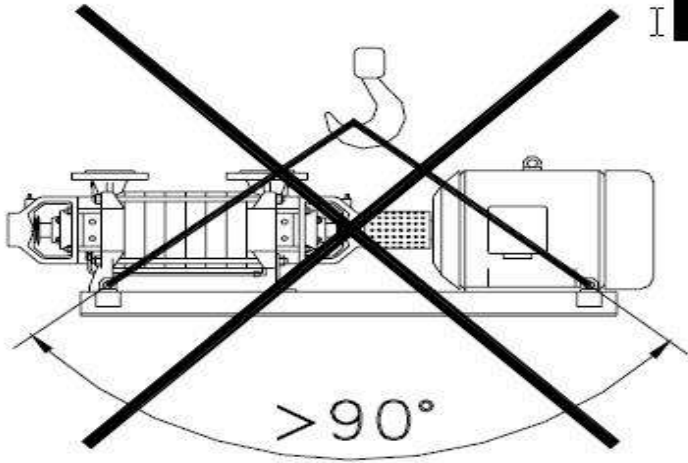
.

8-The pump/pump unit may only be lifted by solid points such as the casing, flanges or frame.

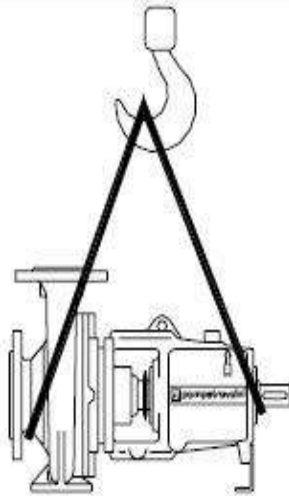
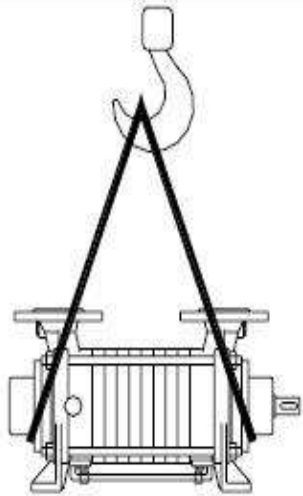
9-The following illustration shows the correct method of carrying by crane.

Transport, Handling

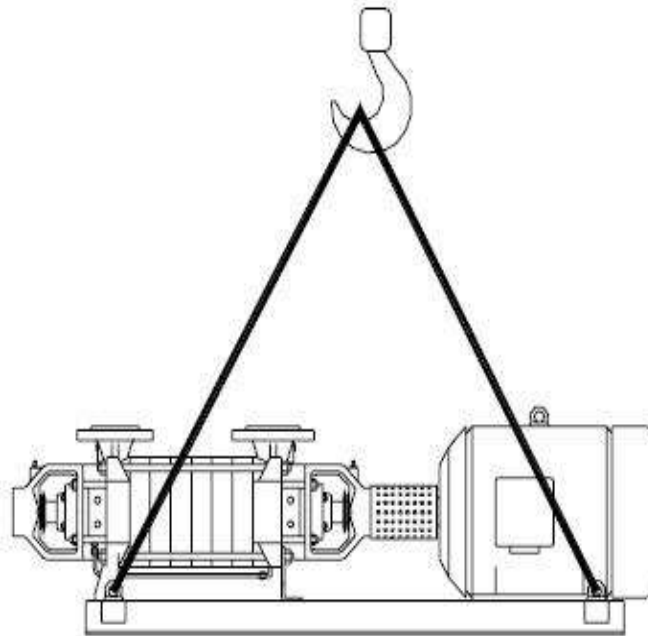
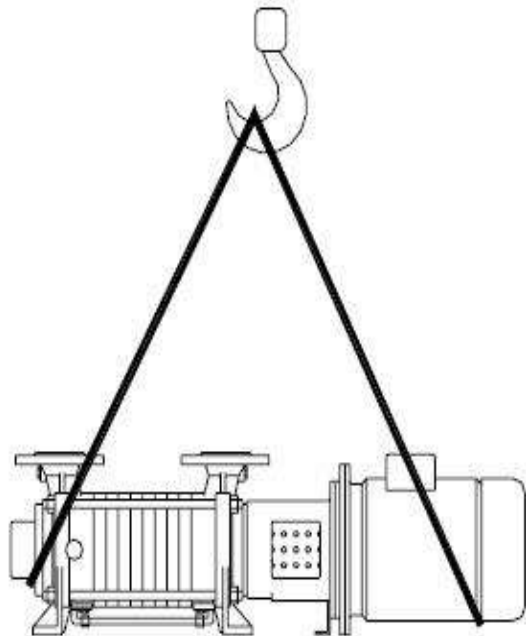
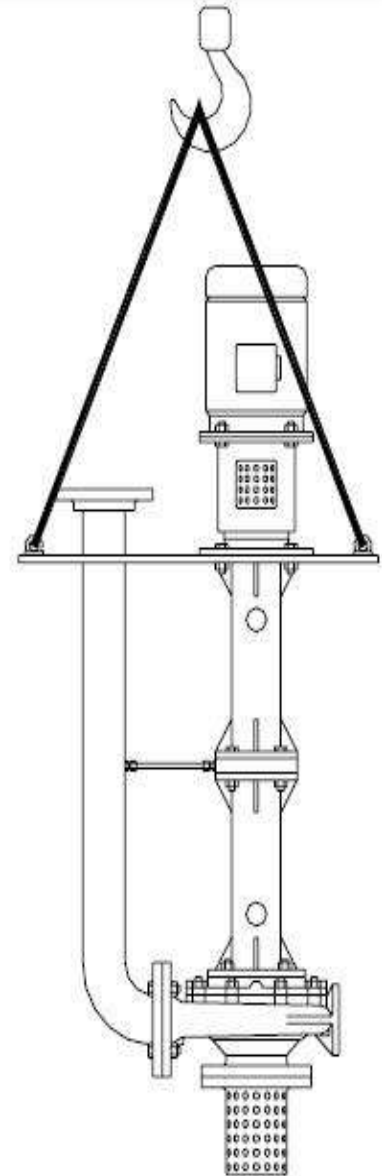
NO



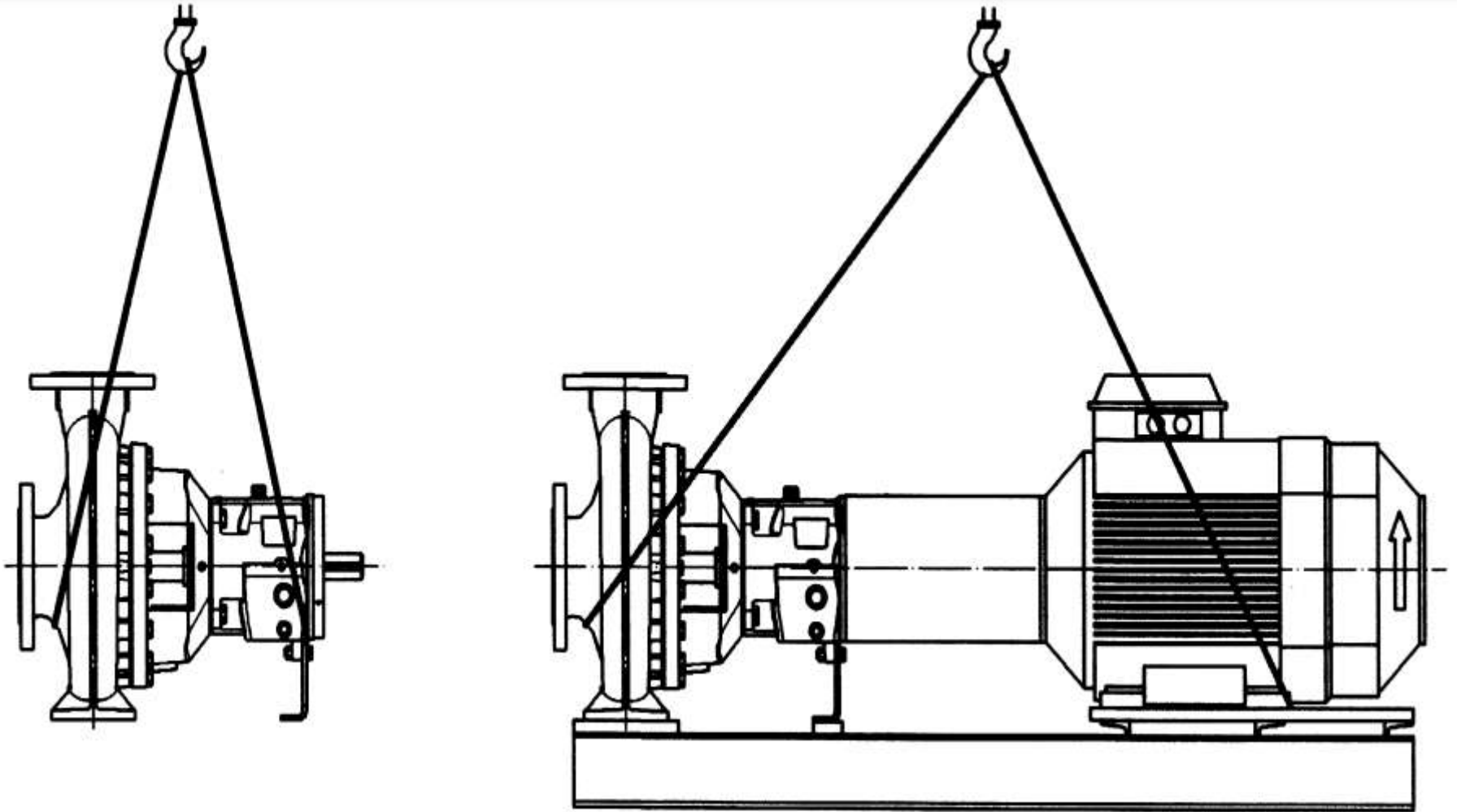
Transport, Handling



OK



Transport, Handling



Do not stand underneath suspended loads.

Pumps Storage

Pumps or pump units that are stored for a long time (6 months max) before use must be protected against moisture, vibrations and dirt (e.g. by wrapping in oil paper or plastic sheeting).

Pumps must basically be stored in a place where they are protected from the weather, e.g. under cover. During this time, all suction and discharge branches and all other intakes and outlets must be closed with dummy flanges or plugs.

Please contact factory for storage instructions for storage periods longer than 6 months

Cover the equipment with industrial strength plastic, preferably transparent to allow its visual inspection, including its nameplate, without uncovering the unit.

Pumps Storage

Drain the casing completely and dry it including :
bearing housing .

stuffing box.

seal chamber.

Apply a coat of soluble rust preventive solution both internally and externally

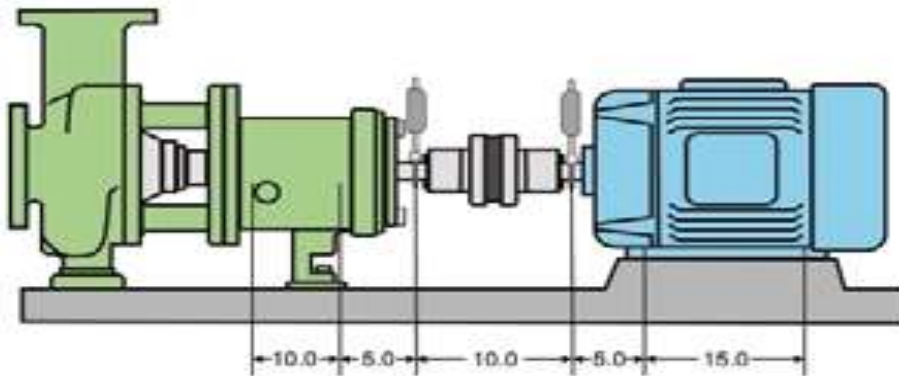
Remove the shaft coupling; it may cause the shaft to develop a permanent sag during prolonged storage.

Protect the bearing housing from moisture by placing bags of vapor phase inhibitor crystals around the housing

Store the unit in its normal position in a dry place.

Pumps Storage

Inspect the unit periodically and turn the shaft a few times plus 1/4 turn. Turning the shaft prevents pitting of finished surfaces. The extra 1/4 turn is to displace the sag and prevent the shaft from developing a permanent bow.

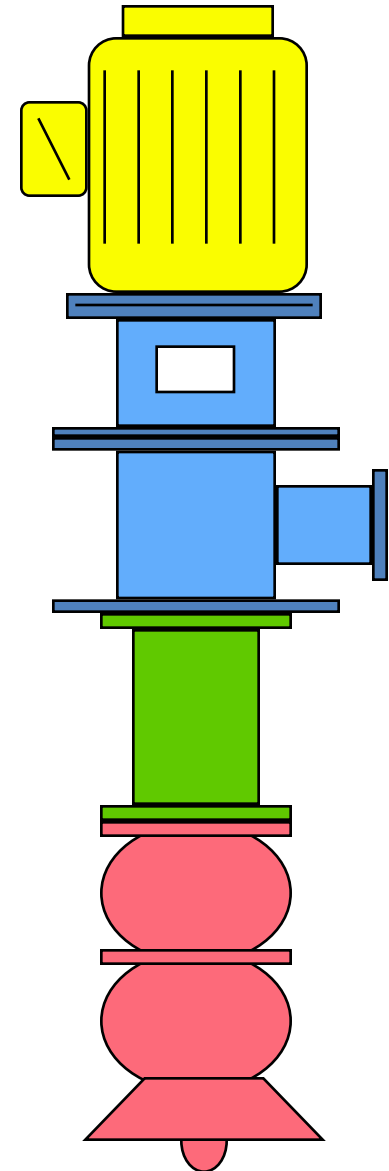


Pump Data

Pump shaft diameter at bearings: 2.55"
Radial bearing: 6313
Thrust bearing: 5313 A/C3
Radial bearing clearance (C3 Fit): .001"-.002"
Bearing Span: 9.25"

Motor Data

Frame: 444
HP: 150
Shaft Diameter: 3.375"
Drive end bearing: 6313
Opposite end bearing: NU318
Radial bearing clearance (C3 Fit): .001"-.002"



Pumps Installation

Mounting of pump onto
a base frame

Installation and Alignment
of Coupling

Connecting the pipes to
the pump

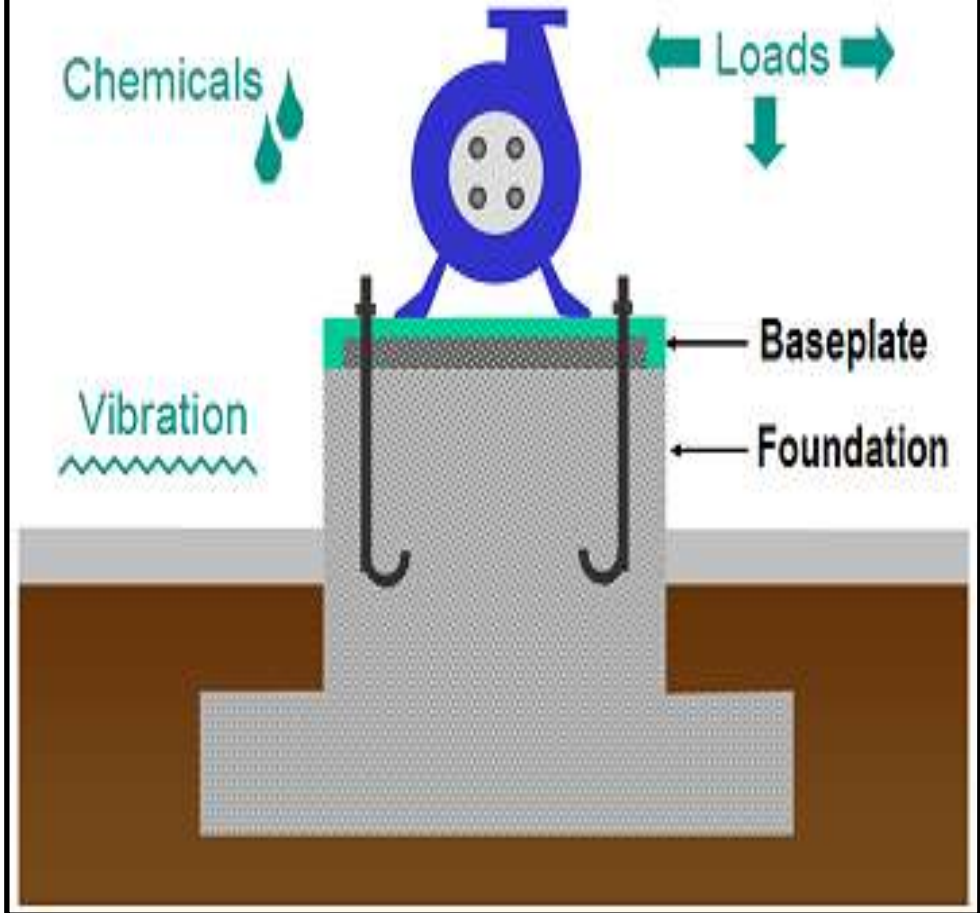
Electrical connection

Starting up

Operation and Monitoring

Shutting down

Traditional Baseplate System



Pumps Installation

Mounting of pump onto a base frame

The pump unit must be provided with a shared base frame made of steel or cast iron or a welded steel profile frame. This base frame must be placed on a foundation which can withstand all loads that arise during operation.



following is to be noticed

The base must withstand all loads occurring during operation.
The mounting surfaces of the pump feet and motor on the base frame must be flat

safe fastening

Space between pump and motor depending on the used coupling

Pumps Installation

Installation and Alignment of Coupling



Make sure that nobody can start the motor during work on the coupling.

Before starting installation **coupling**

carefully clean shaft ends
do not hit the coupling
coupling may be heated before
hand in an oil bath approx. 100°C
Secure coupling hubs against
axial sliding



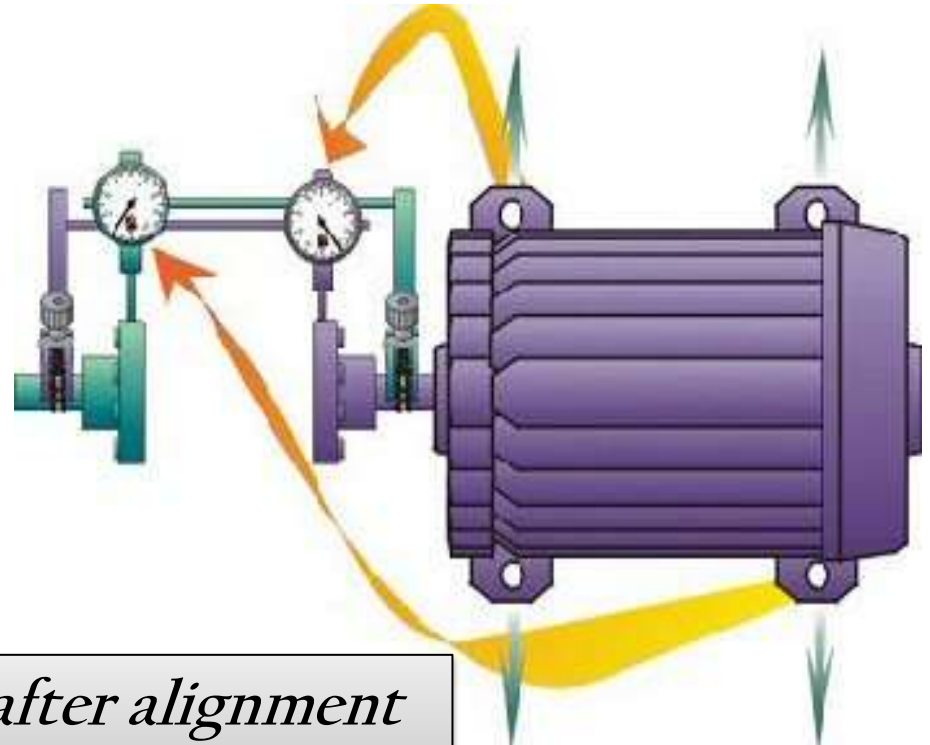
Pumps Installation

Installation and Alignment of Coupling



The installation and alignment of the coupling must be carried out with the utmost care and attention.

***Badly aligned couplings cause noise.
vibration .
increased wear on bearings,
couplings and shaft seals***



*Mount coupling guard after alignment
and before starting the unit.*

Pumps Installation

Connecting the pipes to the pump

The pipes must be of a size and design that liquid can flow freely

it is recommended that a check valve is installed in the discharge pipe shortly after the pump.

Particular attention is to be paid to ensuring that suction pipes are air tight and that the NPSH values are observed.

Do not install fittings or bends right before the suction nozzle.

When laying the pipes, make sure that the pump is accessible for maintenance, installation and disassembly.

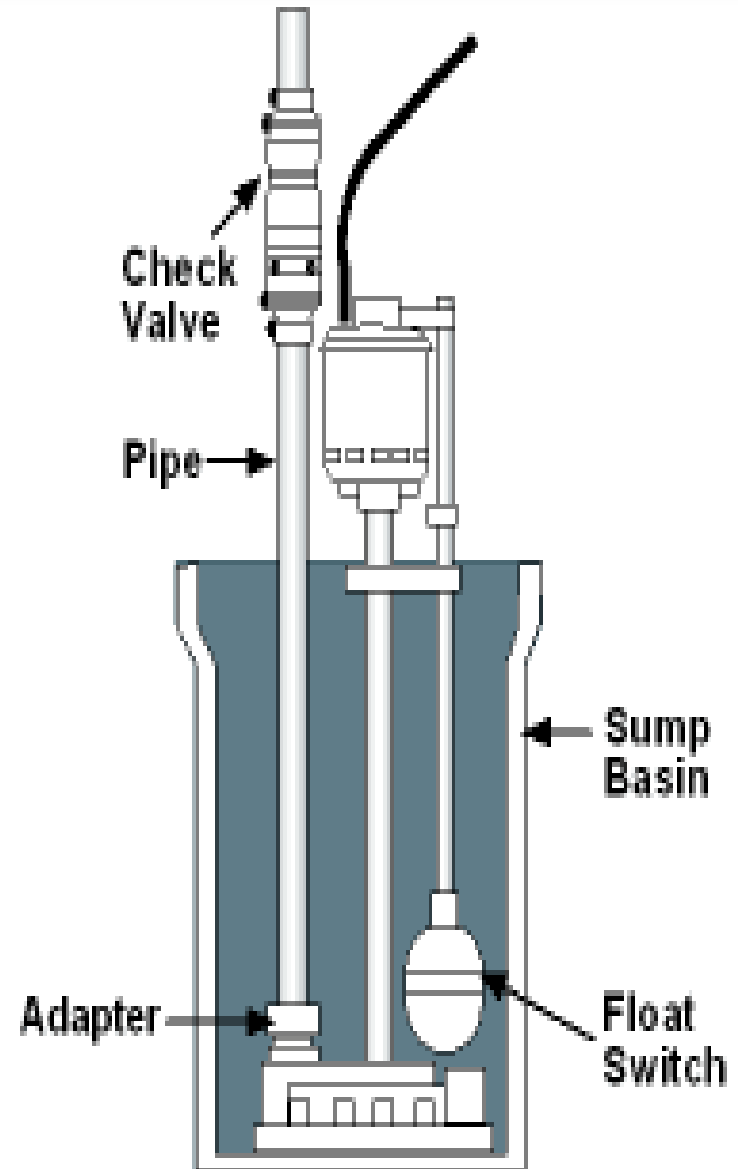
Pumps Installation

Connecting the pipes to the pump

If the pipe system is tested with the pump installed, do not exceed the maximum permitted casing pressure of the pump and/or shaft sealing.

In the case of pumps with stuffing boxes, replace packing after pressure test

Any sealing, flushing or cooling pipe connections must be installed

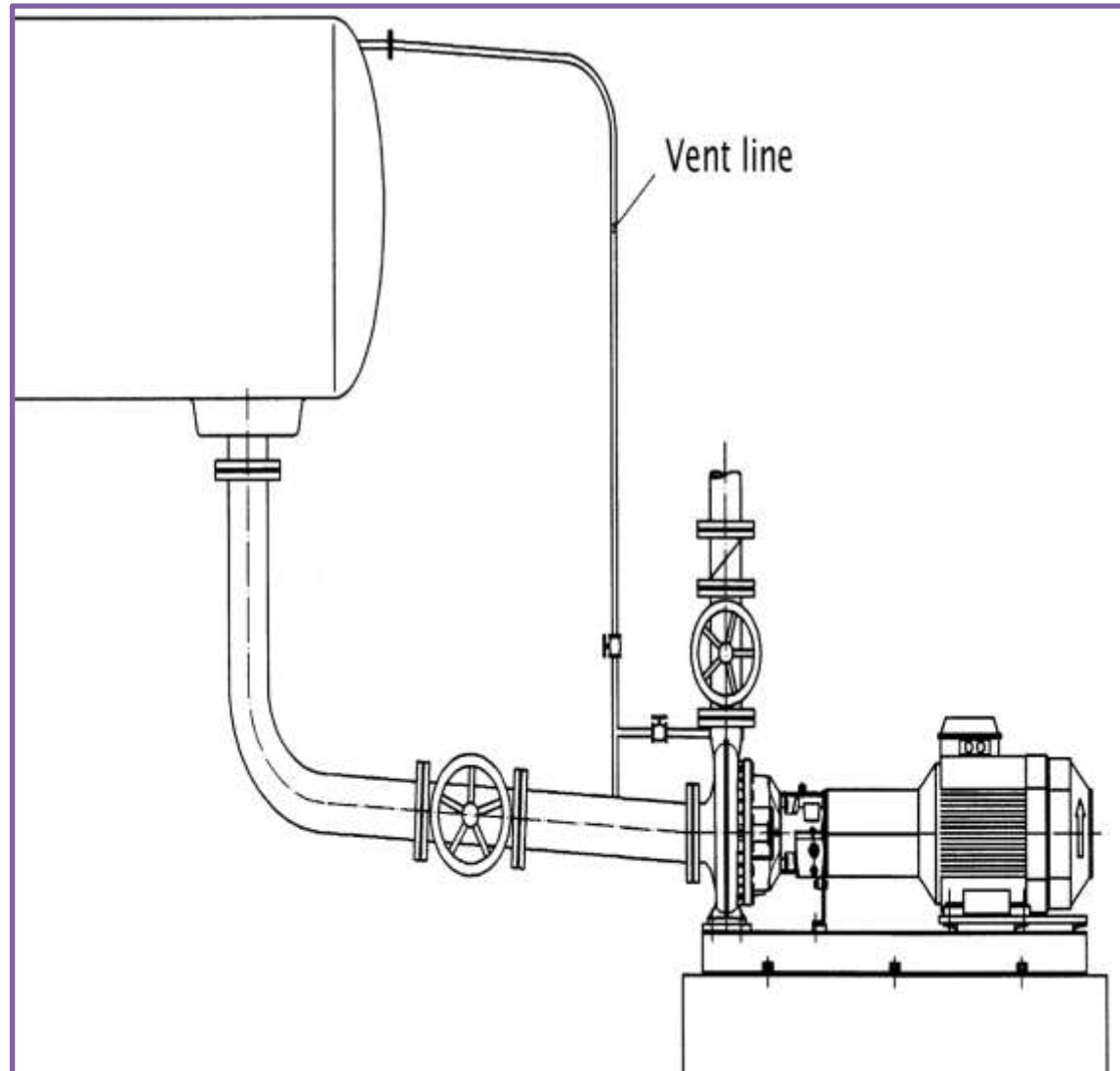


Pumps Installation

Connecting the pipes to the pump

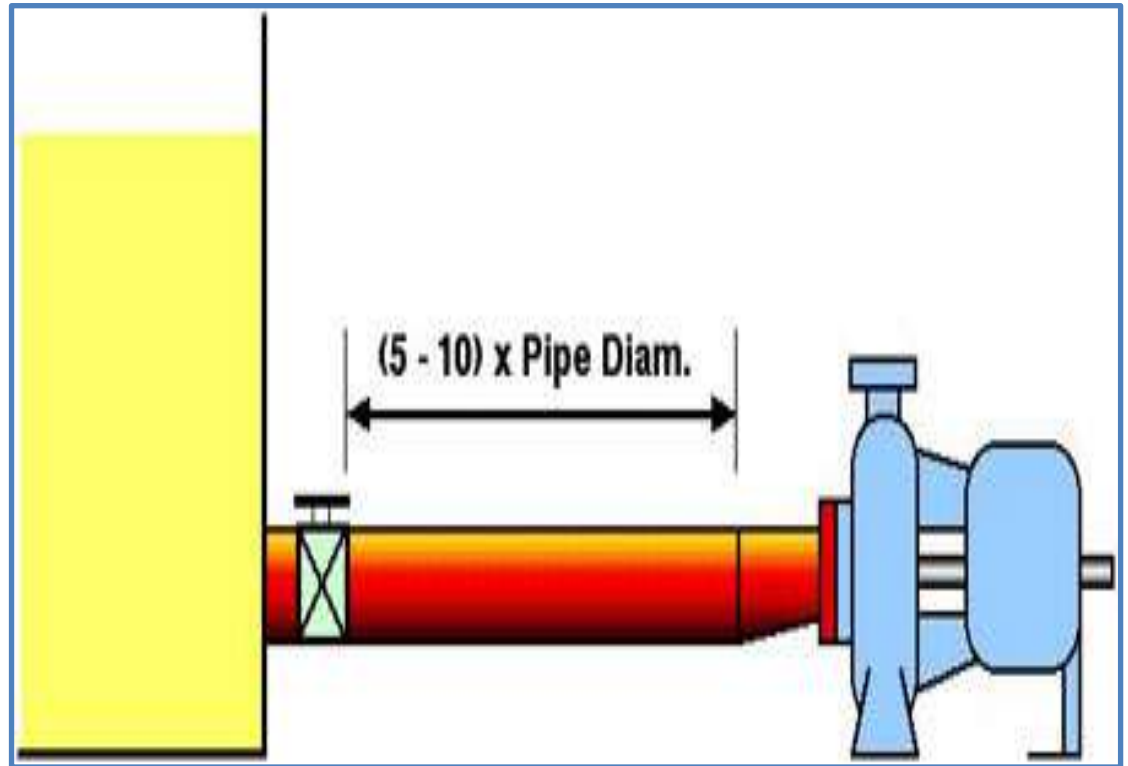
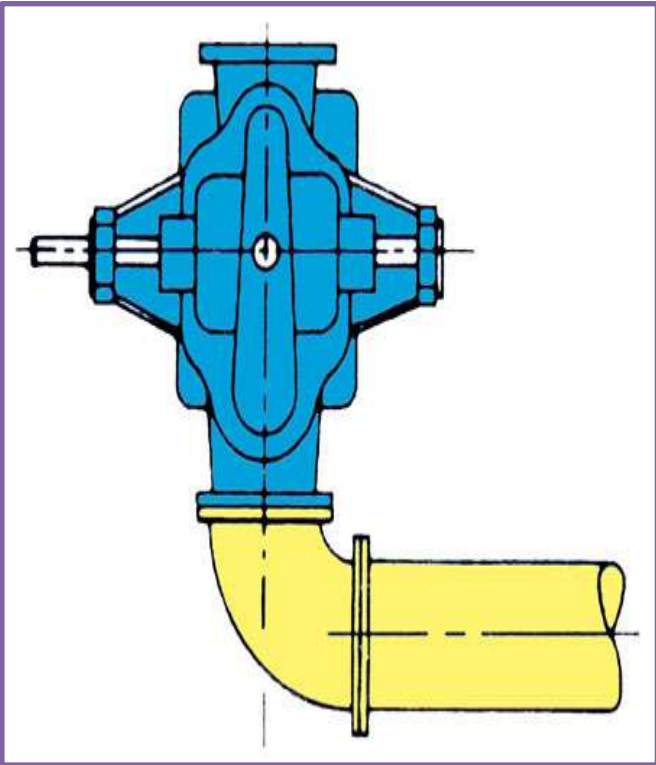
This vent will prevent air binding problem during operation and facilitate proper filling and vent of the pump during startup.

An additional flushed piping -- discharge branch-vent line -- makes it easier to de-aerate the pump before start-up.



Pumps Installation

Connecting the pipes to the pump



Pumps Installation

Electrical connection

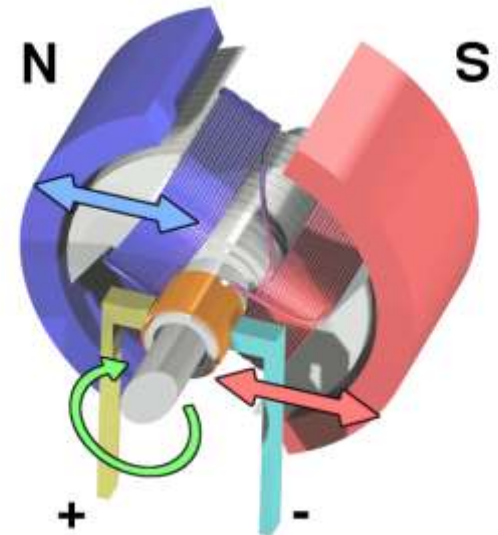


Electrical connection work may only be carried out by an authorized professional

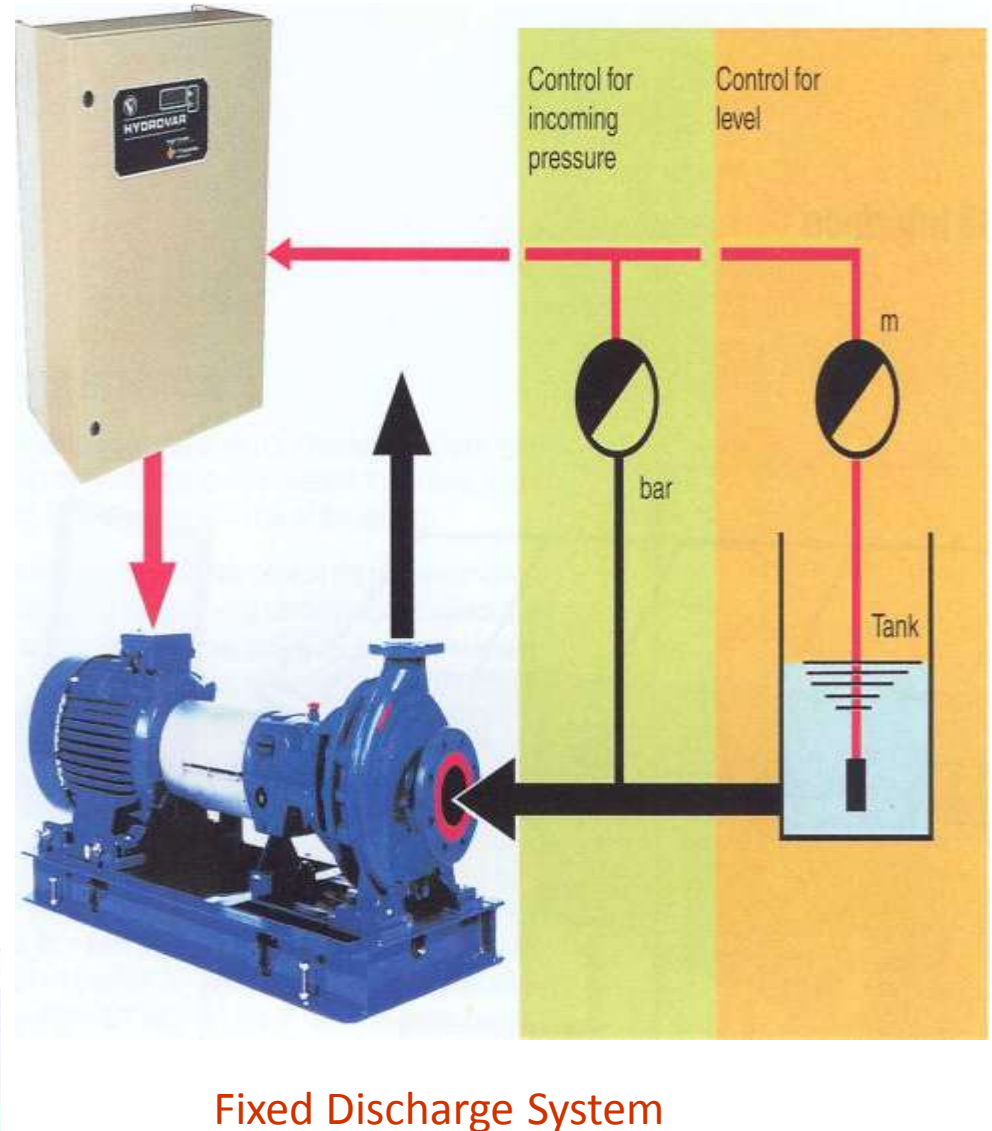
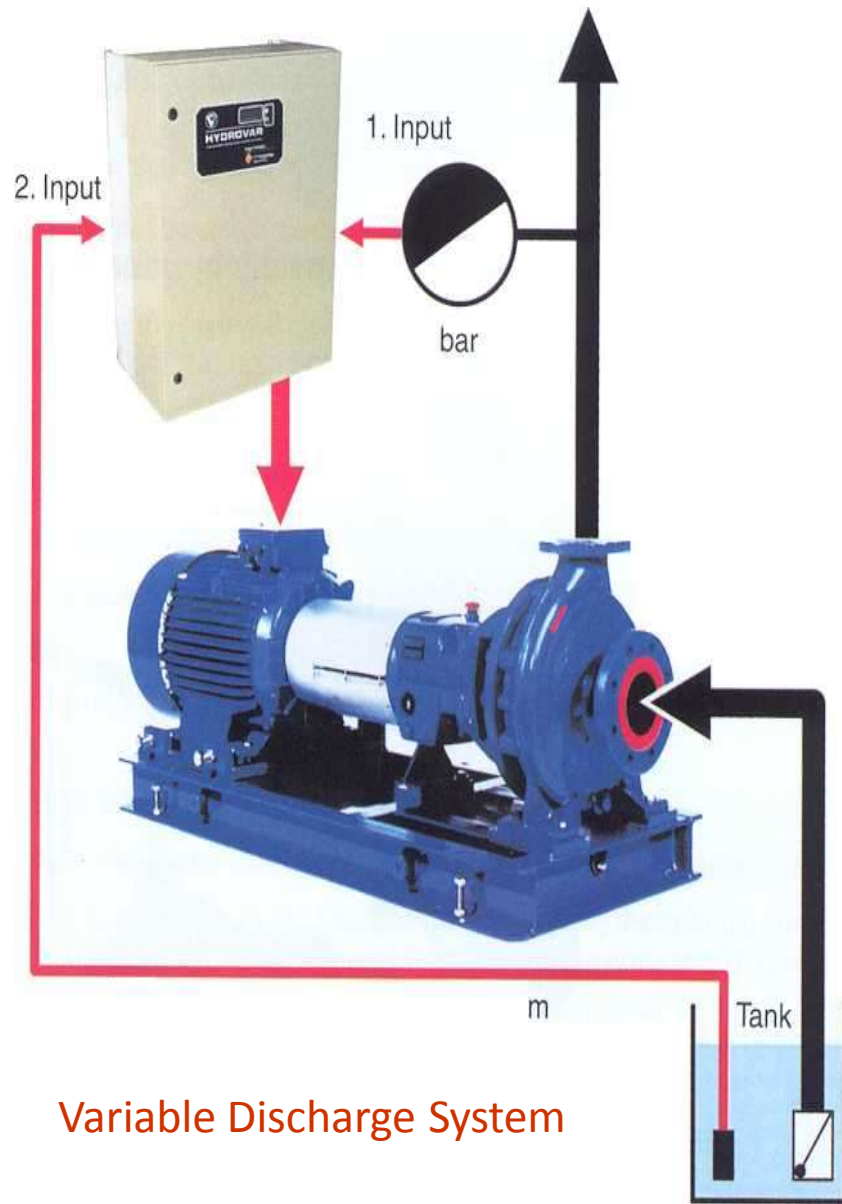
Before starting work, check that the information on the motor rating. The power supply cable accordance with the wiring diagram. A protective motor switch is to be provided.



The direction of rotation should only be checked when the pump is full. Dry running will cause damage to the pump.



Tank Transfer\Unloading



Pumps Installation

Starting up



The plant may only be started up by people who are familiar with the local safety regulations and with these Operating Instructions

Starting up for the first time

If pump is oil lubricated, first open oil drain and drain off any liquid that may have collected.

Fill until the fluid level is at the mid of the oil level sight glass.

For pumps with grease lubrication, no further lubrication is needed before initial start-up.



Pumps Installation

Starting up

- Pump and suction pipe must be filled completely with liquid when starting up.
 - Turn pump unit once again by hand and check that it moves smoothly and evenly.
 - Check that coupling guard is installed and that all safety devices are operational.
 - Switch on any sealing, flushing or cooling devices that are provided.
 - Open isolation valve in suction /intake pipe.
 - Set discharge side isolation valve to approx. 25% of rated flow quantity.
- With pumps with a discharge branch rated width less than 200, the isolation valve can remain closed when starting up
- Check direction of rotation by switching on and off briefly. It must be the same as the directional arrow on the bearing frame.
 - Start drive device.
 - As soon as it reaches normal operating speed, open discharge valve immediately and adjust the required operating point.

Pumps Installation

Starting up /Packing

During the first few hours of operation, slowly reduce the leakage rate as the pump is running by gradually tightening the packing gland. The guideline value is around 30 - 100 drops/minute



Packing that run dry will harden and then destroy the shaft sleeve and/or the shaft.



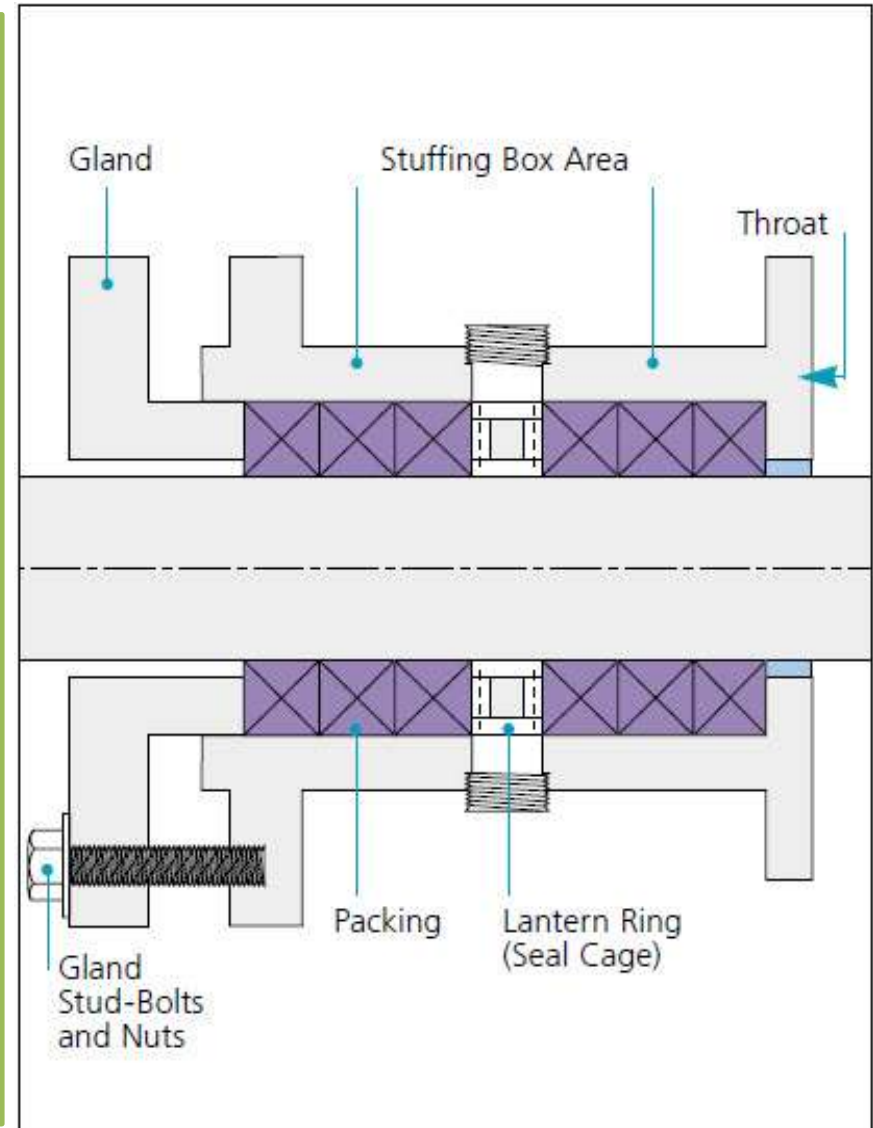
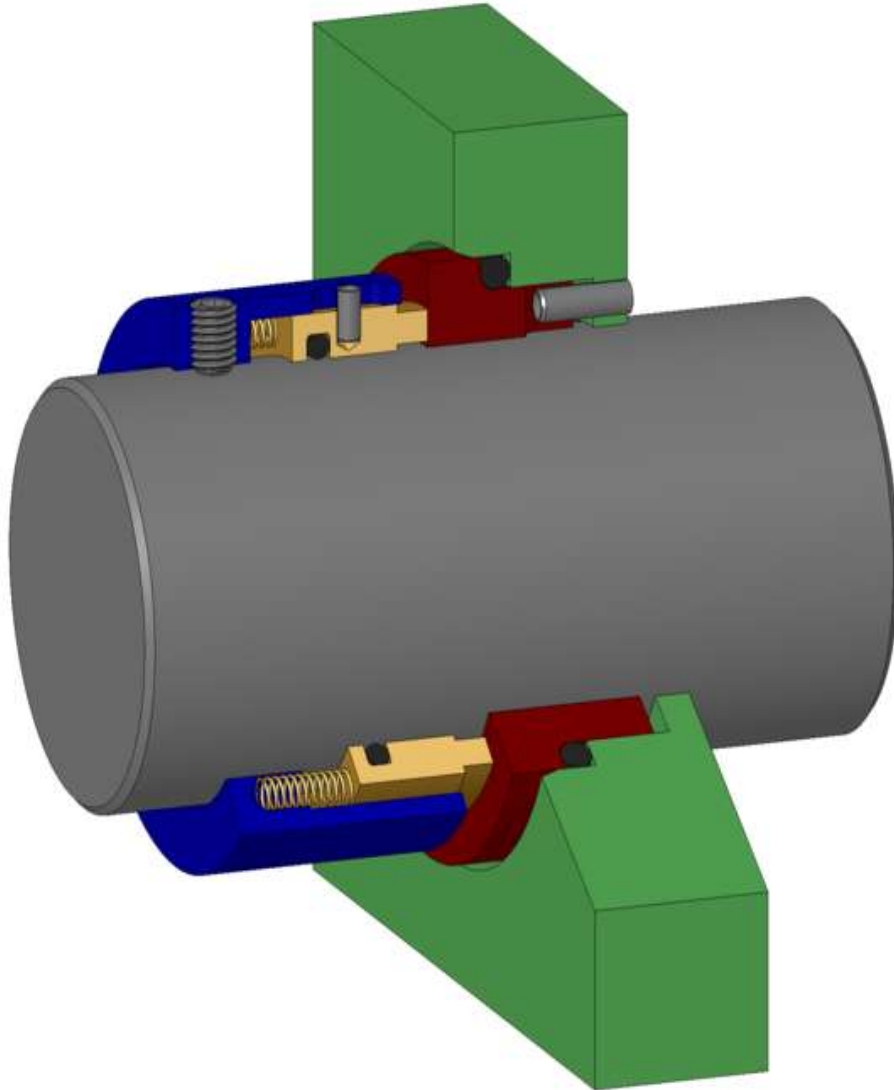
*If pump does not reach attended head or if atypical sounds or vibrations do occur:
Switch off pump and seek for causes*

Pumps Installation

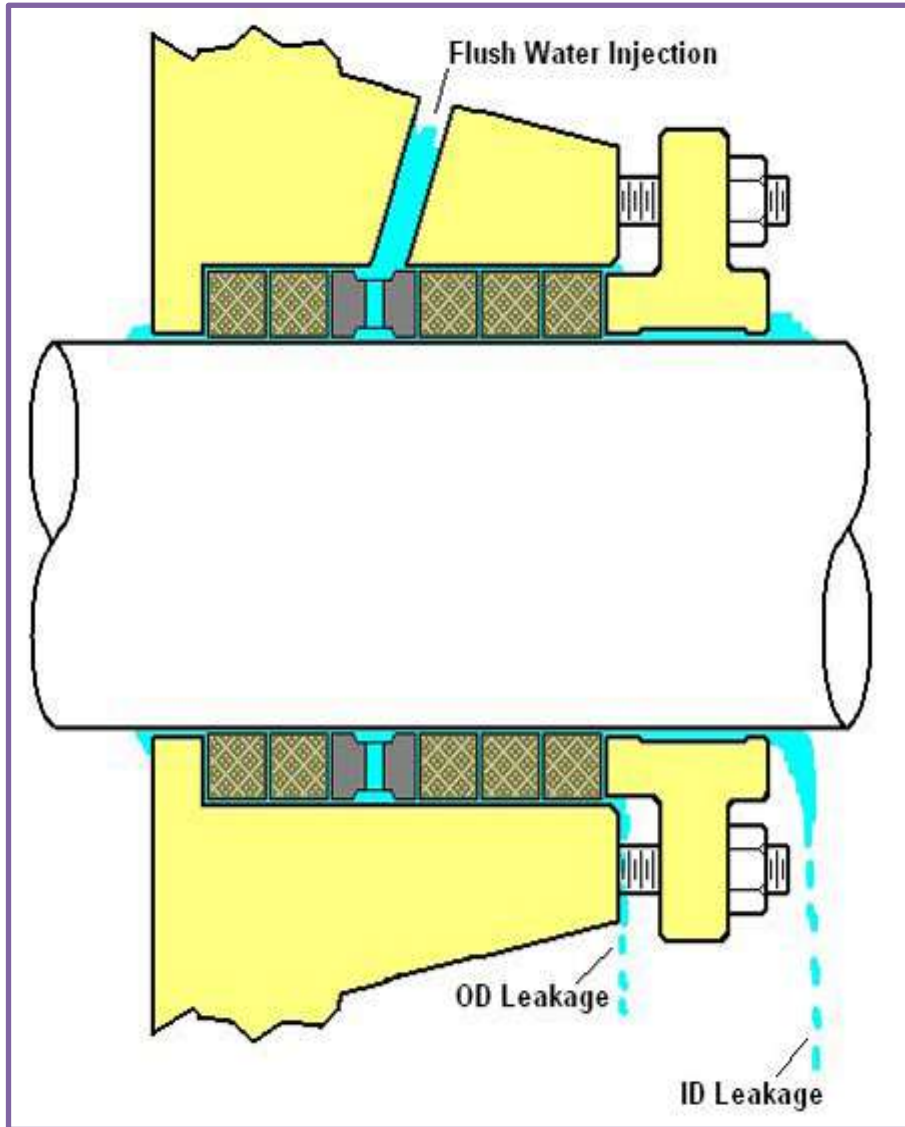
Starting up /Packing



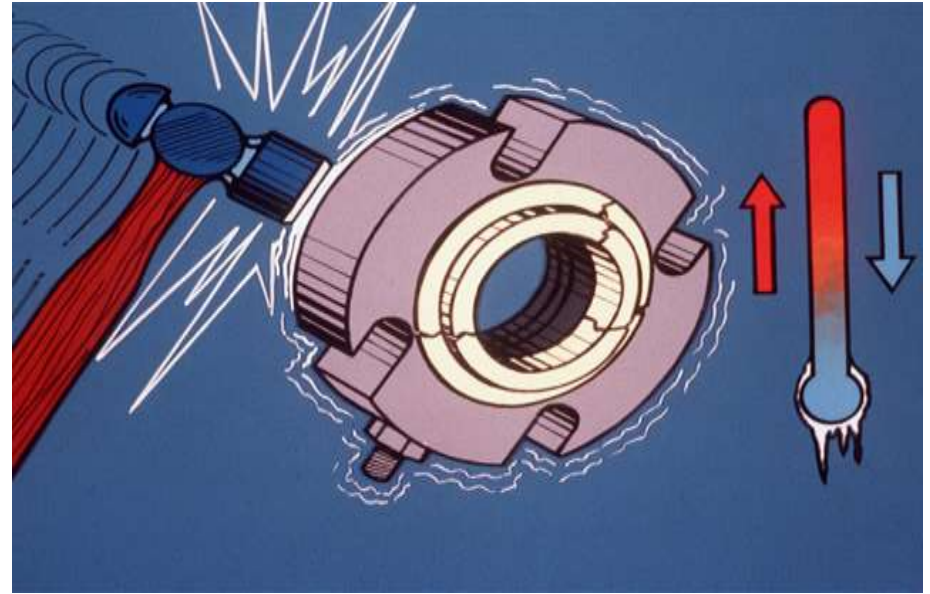
Packing & Mechanical Seal



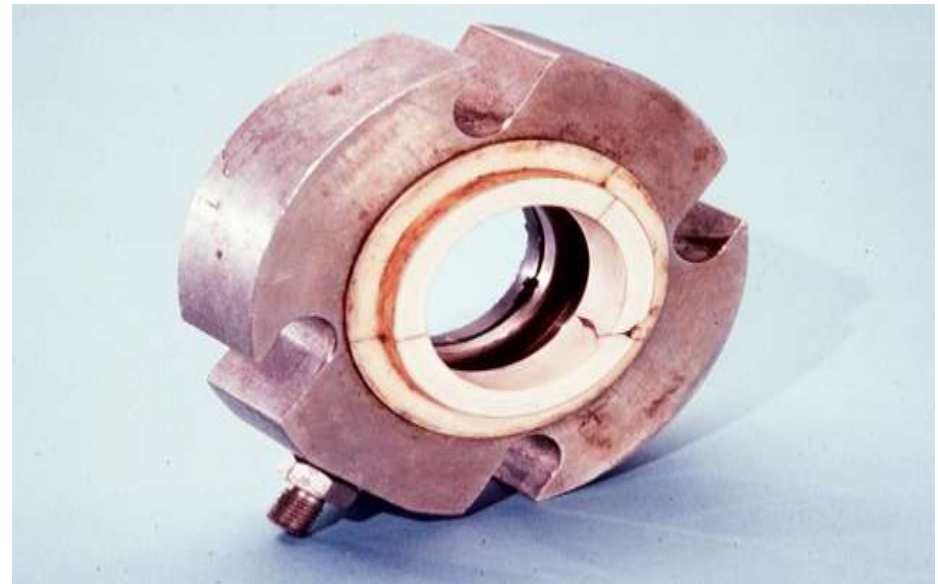
The Basic Sealing Problem:



MECHANICAL SEAL COMMON FAILURES



- RUN-DRY
- DEAD HEADING
- TEMPERATURE
- ALIGNMENT
- VIBRATION
- PARTICULATE / ABRASIVES
- CHEMICAL INCOMPATIBILITY

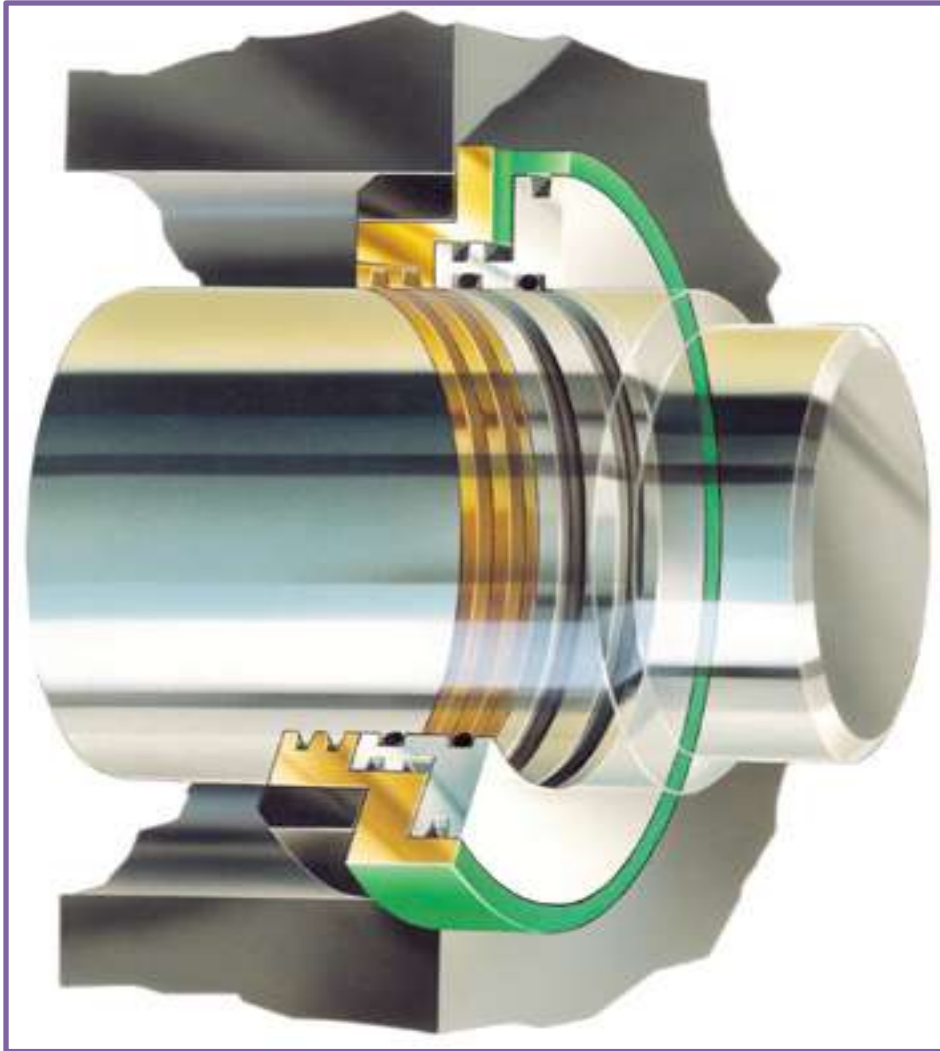


Stock number !?!!



Pumps Installation

Labyrinth seals



Pumps Installation

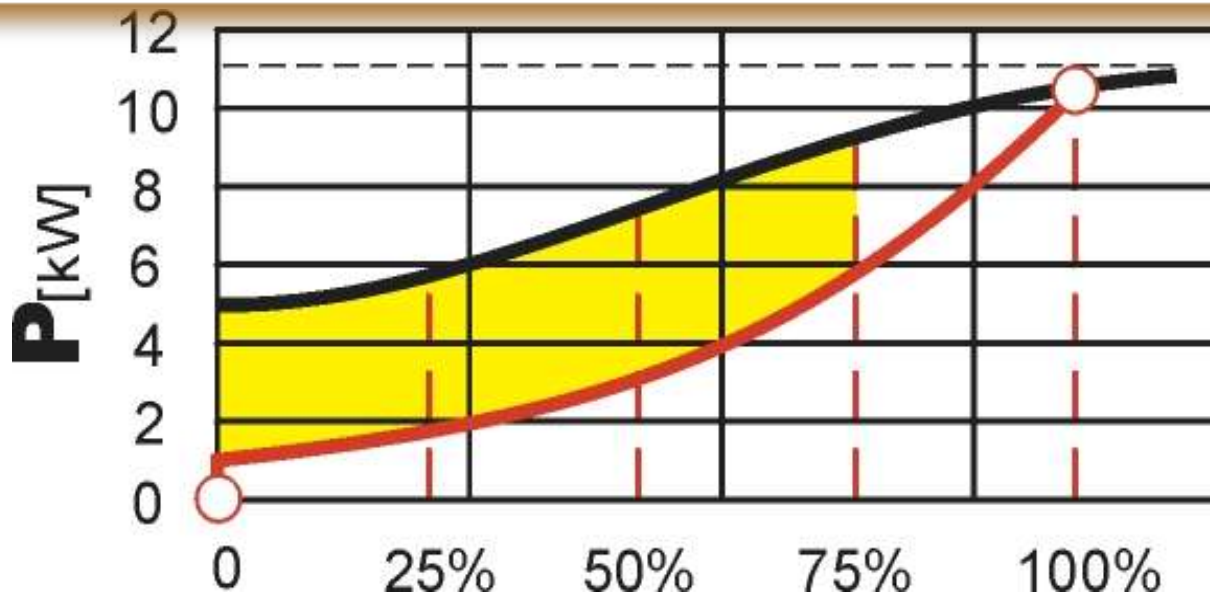
Operation and Monitoring

suction pressure:

Suction pressure is the actual pressure, positive or negative, at the pump suction connection as measured on a gauge. Pumps do not “suck” fluid as the pump suction



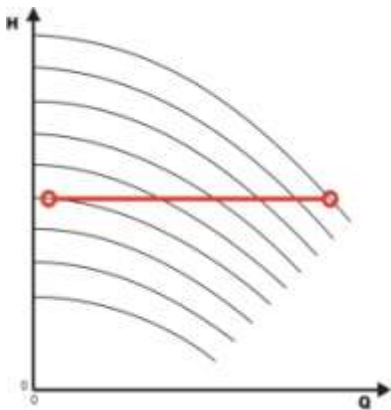
Reduces Operating Cost



capacity in %	power consumption as per curve		saving in kW	saving per 1/3 year (2920 hours)
	pump at constant speed	pump at variable speed		
25 %	5,8 kW	1,8 kW	4,0 kW	11.680 kWh
50 %	7,6 kW	3,2 kW	4,4 kW	12.848 kWh
75 %	9,2 kW	5,7 kW	3,5 kW	10.220 kWh
				34.748 kWh

Energy saving within 1 year (8.760 hours)

Process Application

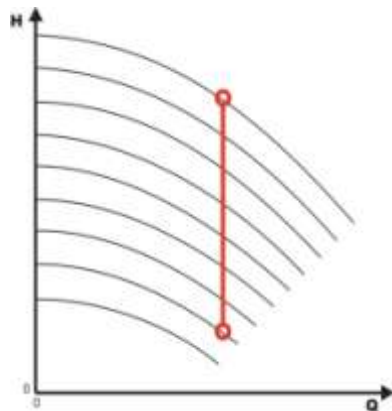
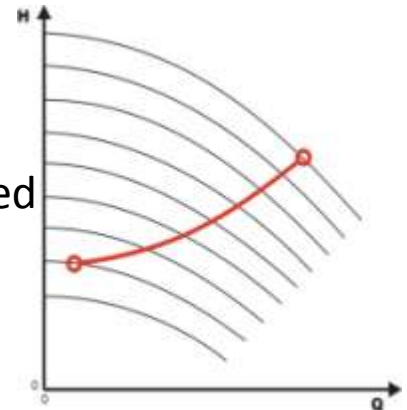


Constant Pressure

- Spray Nozzles
- Decoking
- Boiler Feed
- Fire Suppression

System Curve

- Pilot Plant
- Heat Exchanger Feed

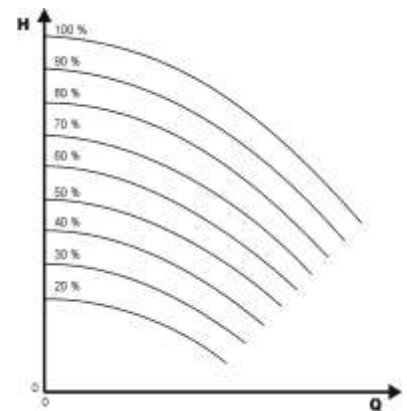


Constant Flow

- Distillation Tower
- Reactor Feed
- Filter Supply
- Pipe line

Actuator Mode

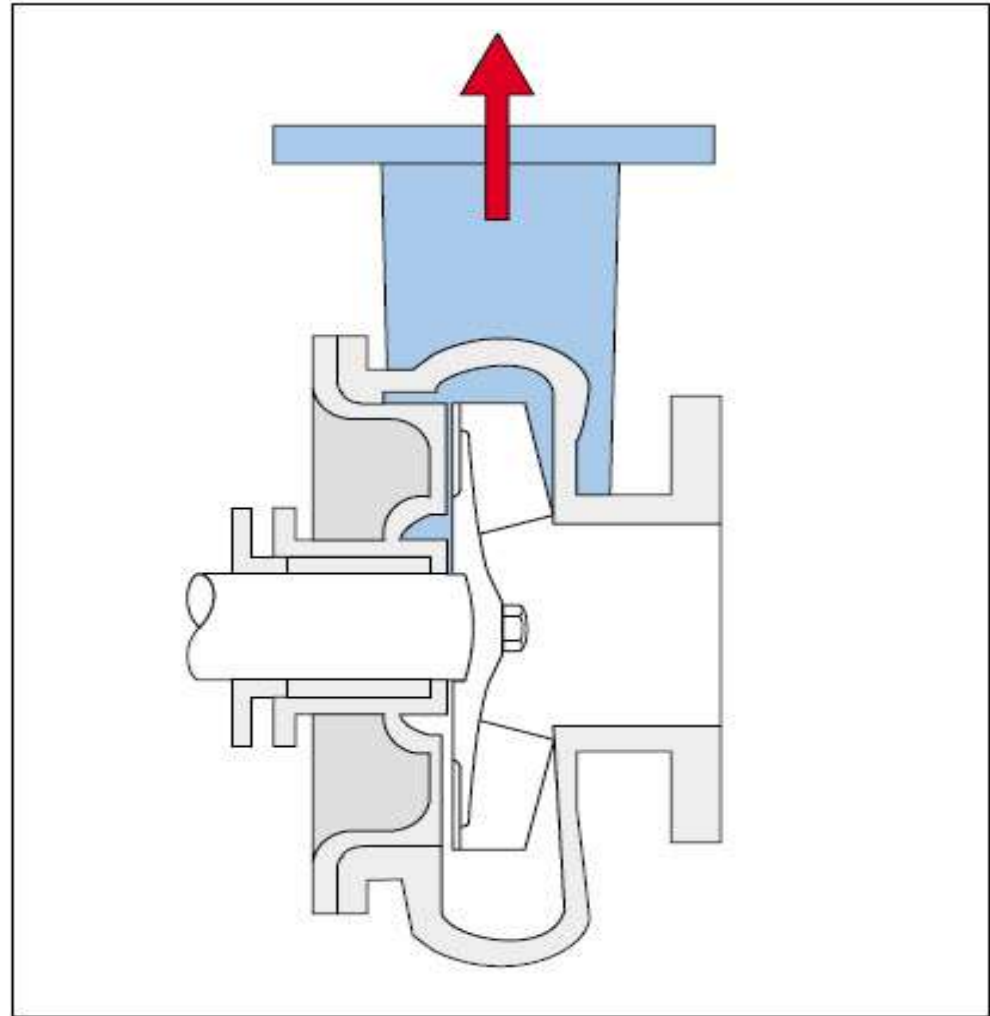
- Process Metering
- Tank\Sump Level Control
- Tank Unloading



Pumps Installation

pump discharge?

The pump discharge is the outlet or flange area where the fluid leaves the volute (casing). The discharge flange is usually oriented up (or vertically), but can also be mounted sideways (or horizontally) if the application requires it.



Troubleshooting a System Problem

Some pumping system problems are sufficiently expensive to justify a system assessment. Examples of these problems include inefficient operation, cavitations, poor flow control, and high maintenance

Inefficient Operation.

Inefficient system operation can be caused by a number of problems as:

- improper pump selection.

- poor system design.

- excessive wear-ring clearances.

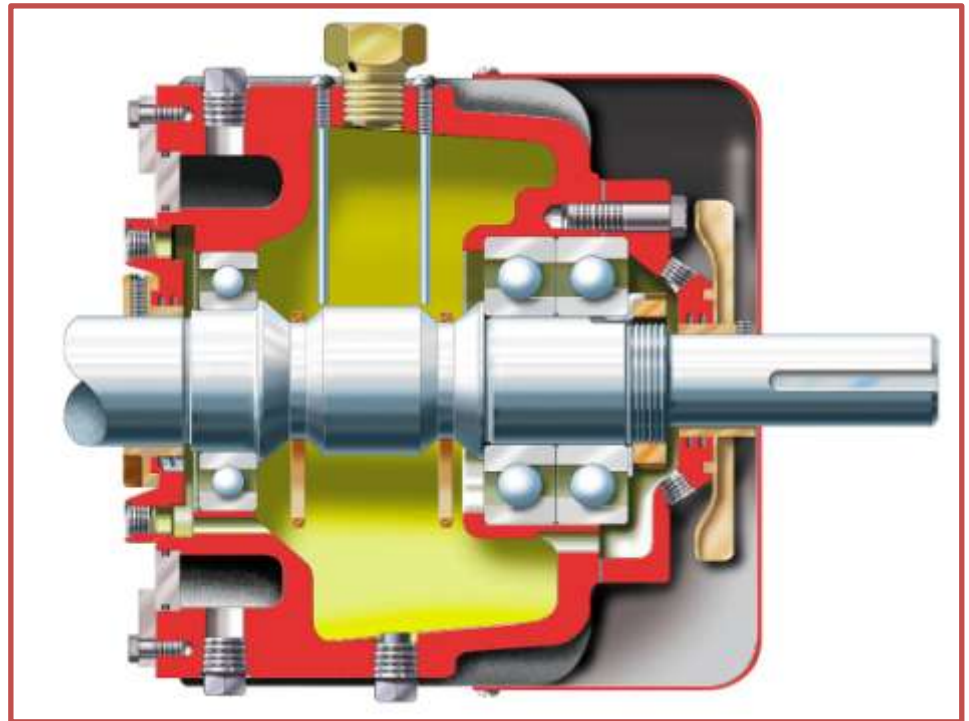
- wasteful flow control practices.

Indications of inefficient system operation include:

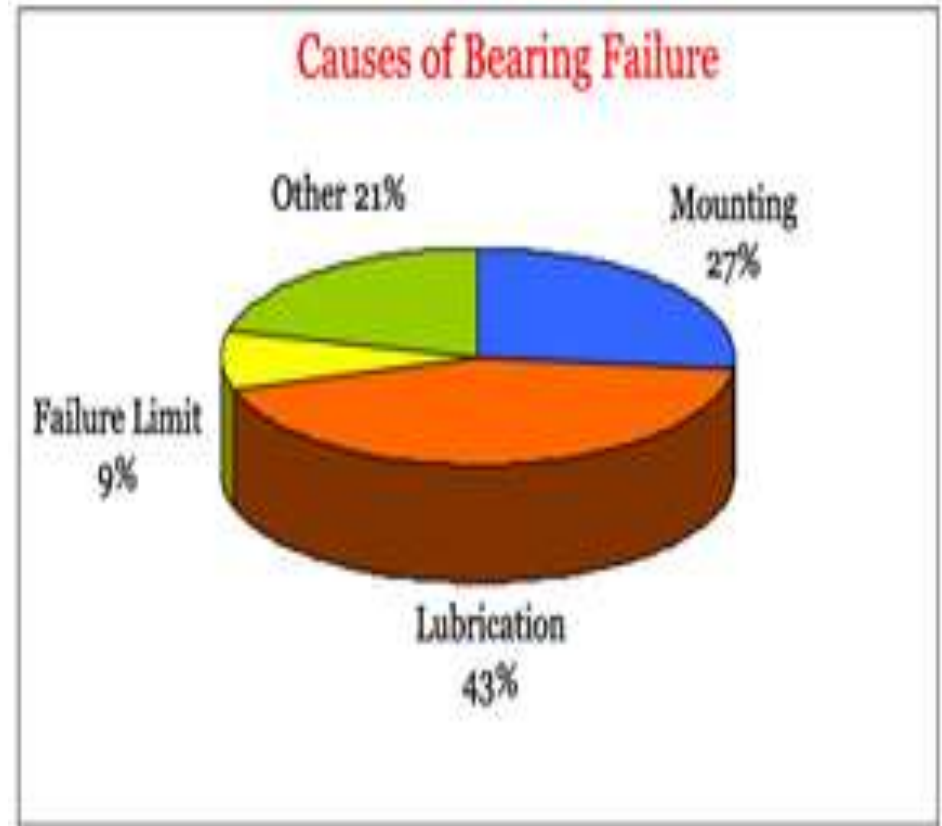
- high energy costs.

- excessive noise in the pipes and across valves.

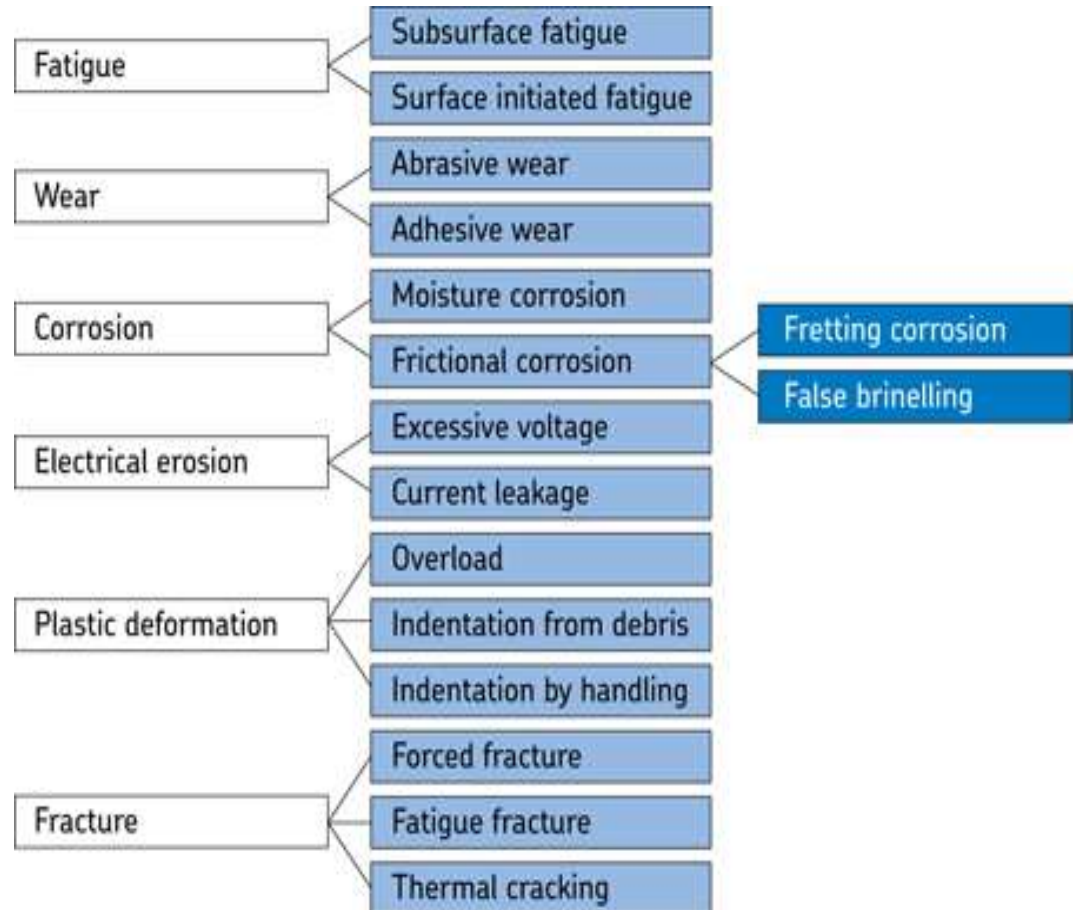
- high maintenance requirements



Bearing Failures and Their Causes



Bearing Failures and Their Causes



Troubleshooting a System Problem

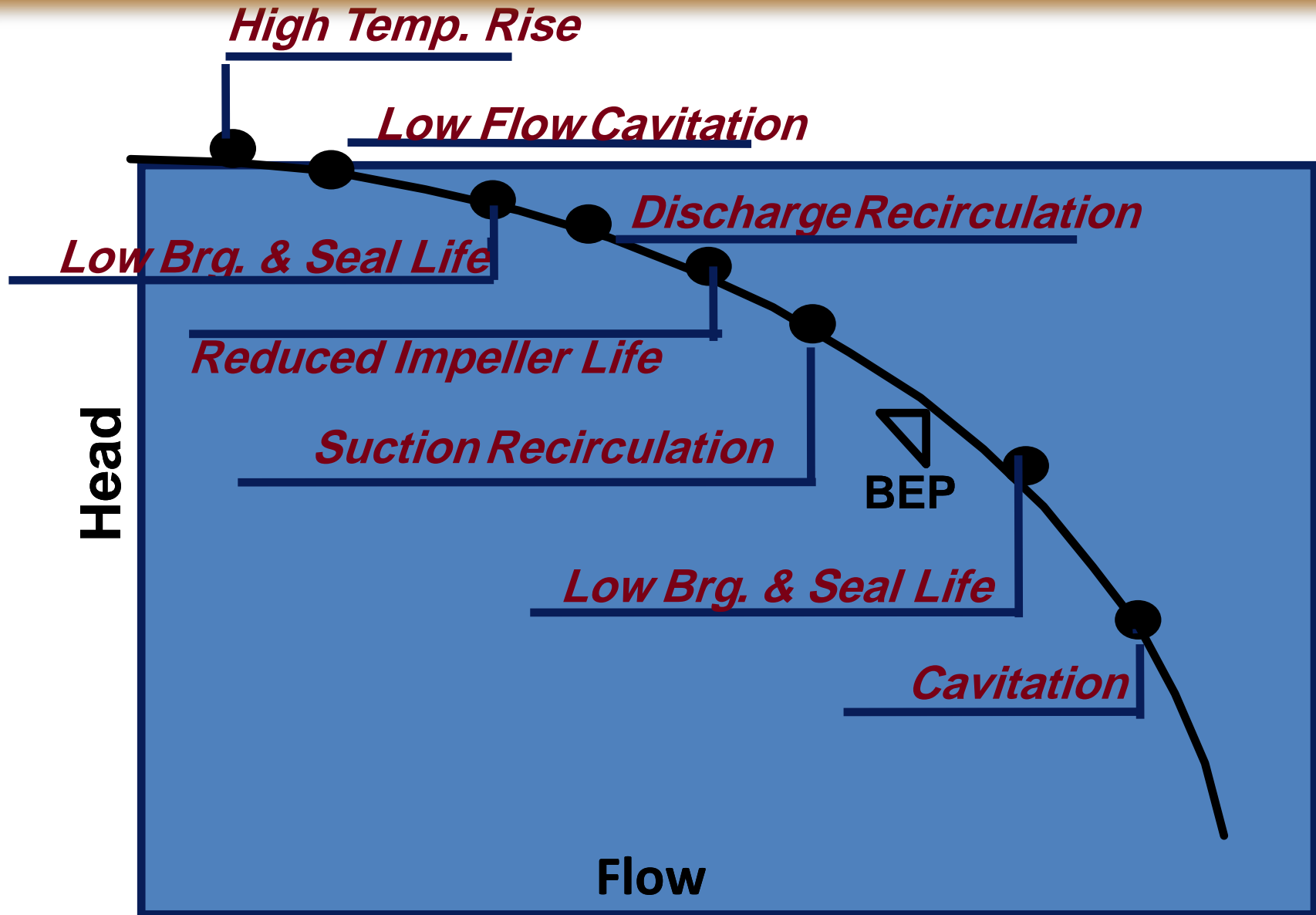


PUMP FAILURE ANALYSIS

6 month period in a typical process plant

CAUSE	NUMBER	% of TOTAL
Bearing	25	10.50
Bearing housing	1	0.42
Case wearing ring	2	0.84
Impeller	8	3.36
Rotating face	1	0.42
Screws /set screws	1	0.42
Seals - mechanical	179	75.21
Shaft	12	5.04
Sleeve	9	3.78
TOTAL	238	100.00%

Results of Operating Off BEP



Shaft Deflection

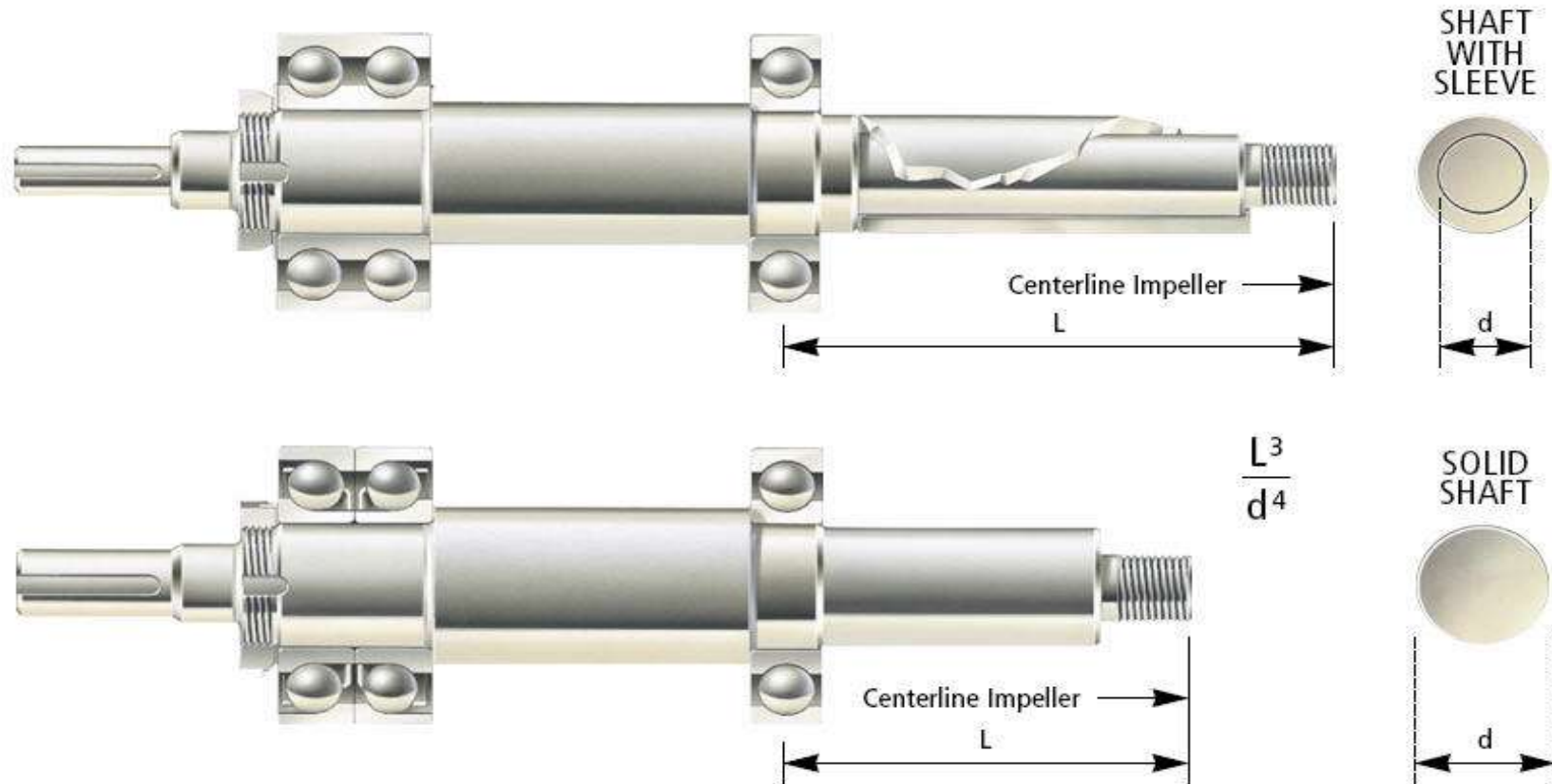
Shaft deflection is the result of unbalanced radial loads. The amount of shaft deflection or bending depends on the amount of unbalance radial forces and a pump's slenderness ratio. The higher the forces or the larger the slenderness ratio, the more shaft deflection will occur. Shaft deflection results in sealing device, bearing, and other pump mechanical failures.

Shaft Slenderness Ratio

The Shaft Slenderness Ratio is a ratio of shaft length to shaft diameter.

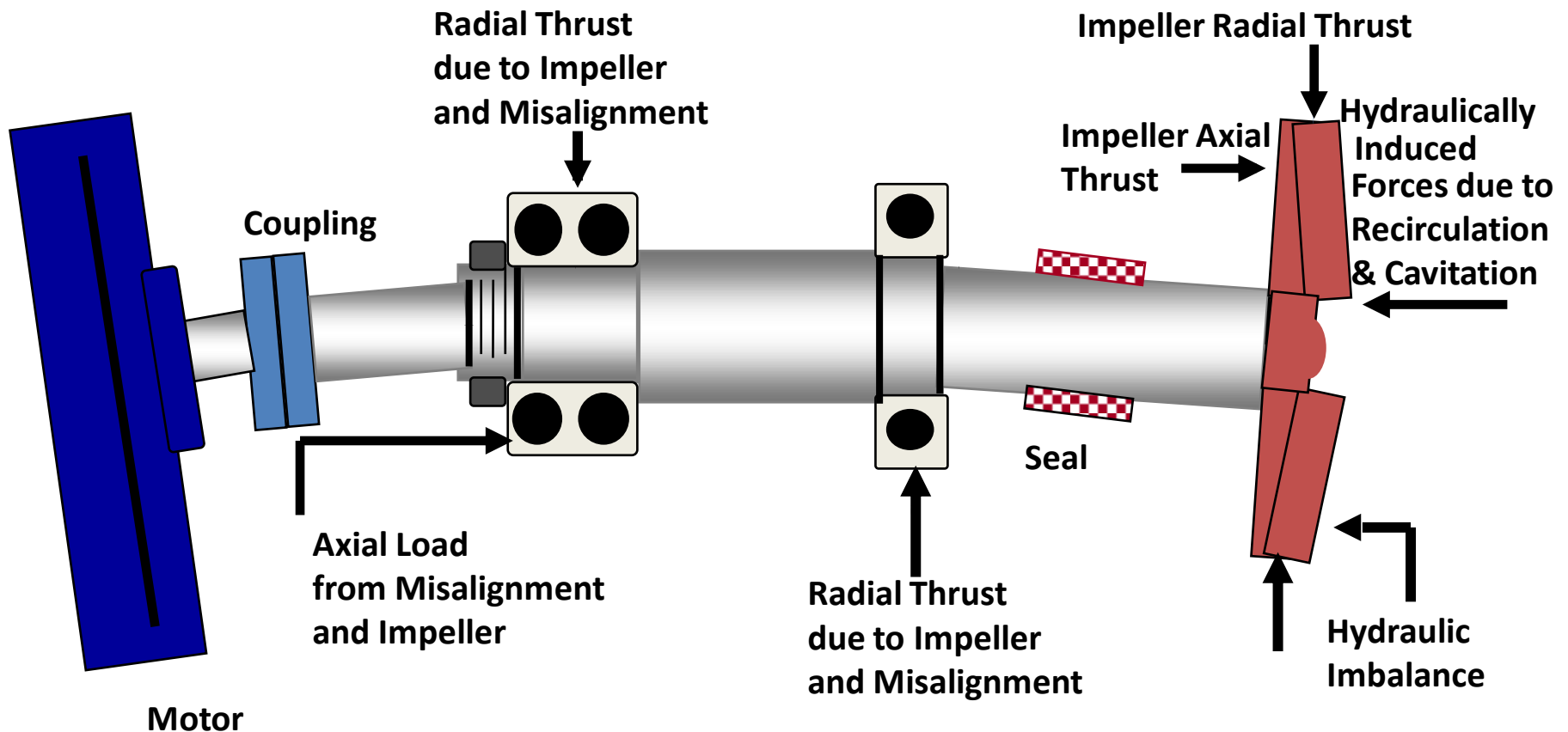


Shaft Deflection



Shaft Deflection

SIMULTANEOUS DYNAMIC LOADS ON PUMP SHAFT



TEMPERATURE RISE

Overheating of the liquid in the casing can cause:

- *Rubbing or seizure from thermal expansion*
- *Vaporization of the liquid and excessive vibration*
- *Accelerated corrosive attack by certain chemicals*

Temperature rise per minute at shutoff is:

$$\Delta T \text{ } ^\circ\text{F (} ^\circ\text{C) / min.} = \frac{\text{HP (KW)}_{\text{so}} \times K}{\text{Gal (m}^3\text{)} \times \text{S.G.} \times \text{S.H.}}$$

HP_{so} = HP (KW) @ shutoff from curve

Gal. (m³) = Liquid in casing

S.G. = Specific gravity of fluid

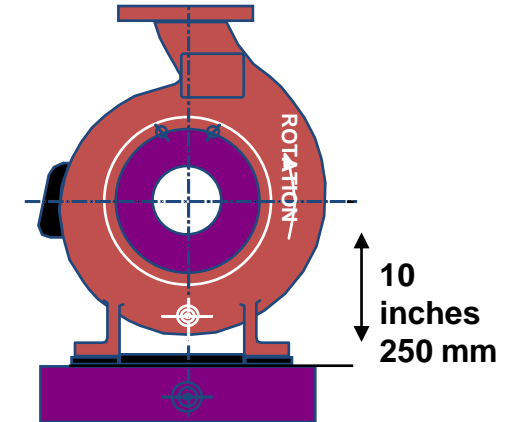
S.H. = Specific heat of fluid

Ex.: Pump w/ 100HP (75KW) @s.o. , 6.8 gal casing (.03m³)
w/ 60°F (16°C) water would reach boiling in 2 min.

A recirculation line is a possible solution to the low flow or shut off operation problems....

CASING GROWTH DUE TO HIGH TEMPERATURE

High temperature requires more clearance



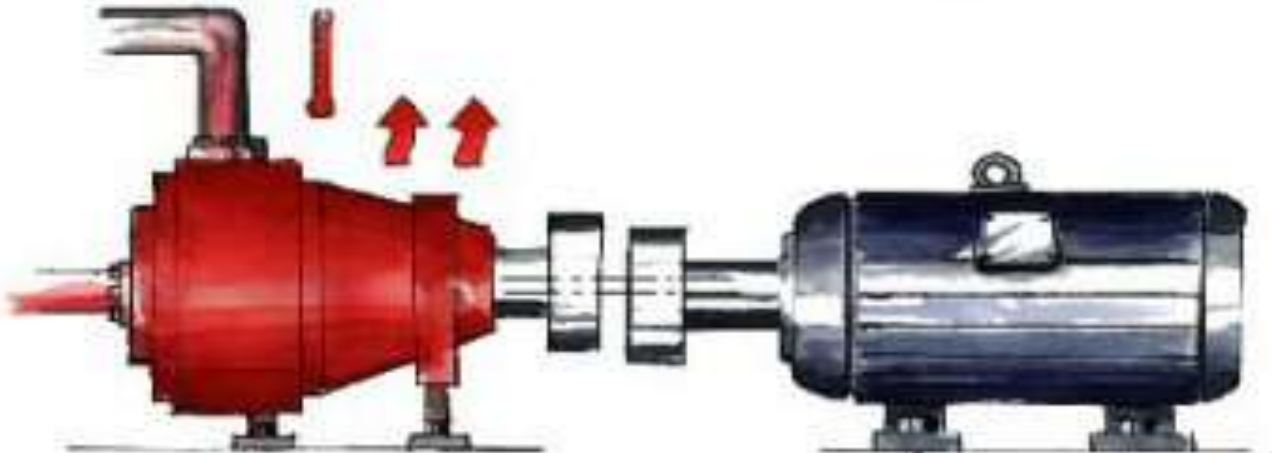
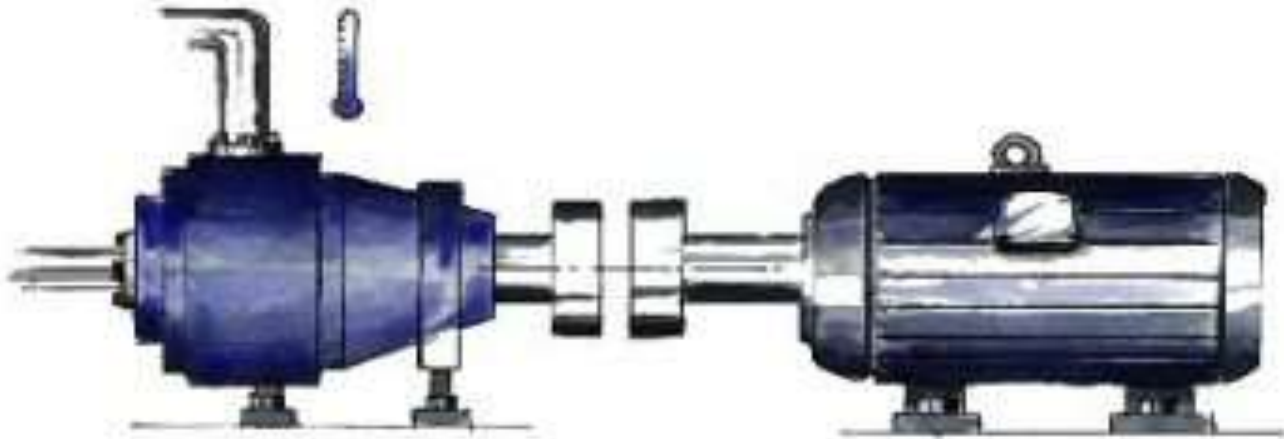
COEFFICIENT OF THERMAL EXPANSION FOR 316 S/S
IS 9.7×10^{-6} IN/IN/°F OR 17.5×10^{-6} MM/MM/°C

CALCULATION IS $\Delta T \times 9.7 \times 10^{-6} \times \text{LENGTH IN INCHES}$
 $\Delta T \times 17.5 \times 10^{-6} \times \text{LENGTH IN}$

MILLIMETERS

$\Delta T^{\circ} \text{ F}$	$\Delta T^{\circ} \text{ C}$	EXPANSION	
		INCHES	MILLIMETERS
100 F	55 C	0.0097 IN	0.245 MM
200 F	110 C	0.0190 IN	0.490 MM
300 F	165 C	0.0291 IN	0.735 MM
400 F	220 C	0.0388 IN	0.900 MM
500 F	275 C	0.0485 IN	1.230 MM
600 F	330 C	0.0582 IN	1.470 MM

PUMP GROWTH DUE TO HIGH TEMPERATURE



IMPELLER BALANCE

← MECHANICAL

- Weight offset from center of impeller
- Balance by metal removal from vane

← HYDRAULIC

- Vane in eye offset from impeller C/L
- Variation in vane thickness
- Results in uneven flow paths thru impeller
- Investment cast impeller eliminates problem
- Careful machining setup can help



Centrifugal Pump Troubleshooting Guide

Table 4-6
Troubleshooting Guide -- Centrifugal Process Pumps

Troubleshooting Guide -- Centrifugal Process Pumps												
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SUCTION PROBLEMS

HYDRAULIC SYSTEM

Table 4-6 (cont.)

Symptoms													Symptoms																									
D Insufficient Disch. Pressure													Short Bearing Life													E												
C Intermittent Operation													Short Mech. Seal Life													F												
B Insufficient Capacity													Vibration & Noise													G												
A No Liquid Delivery													Power Demand Excessive													H												
Possible Causes													#	A	B	C	D	E	F	G	H	#	Possible Remedies															
HYDRAULIC SYSTEM	Strainer Partially Clogged													7		3							7	* Inspect And Clean														
	Pump Impeller Clogged													8	8	8							5	8	* Check For Damage And Clean													
	Suction And/Or Discharge Valve(s) Closed													9	9								9	* Shut Down And Open Valves														
	Viscosity Too High													10		7		5					4	10	* Heat Up Liquid To Reduce Viscosity * Increase Size Of Discharge Piping To Reduce Pressure Loss * Use Larger Driver Or Change Type Of Pump * Slow Pump Down													
	Specific Gravity Too High													11									2	11	* Check Design Specific Gravity													
MECHANICAL SYSTEM	Total System Head Lower Than Design Head Of Pump													12				4		11		3	12	* Increase System Resistance To Obtain Design Flow * Check Design Parameters Such As Impeller Size, Etc.														
	Total System Head Higher Than Design Head Of Pump													13	6	5	4			10	2		13	* Decrease System Resistance To Obtain Design Flow * Check Design Parameters Such As Impeller Size, Etc.														
	Unsuitable Pumps In Parallel Operation													14	7	6		6					14	* Check Design Parameters														
MECHANICAL SYSTEM	Improper Mechanical Seal													15						1			15	* Check Mechanical Seal Selection Strategy														
	Possible Causes													#	A	B	C	D	E	F	G	H	#	Possible Remedies														

HYDRAULIC SYSTEM

MECHANICAL SYSTEM

Centrifugal Pump Troubleshooting Guide

Table 4-6 (cont.)

Table 4-6 (cont.)

Symptoms												Symptoms											
D Insufficient Disch. Pressure						Short Bearing Life						E											
C Intermittent Operation						Short Mech. Seal Life						F											
B Insufficient Capacity						Vibration & Noise						G											
A No Liquid Delivery						Power Demand Excessive						H											
Possible Causes	#	A	B	C	D	E	F	G	H	#	Possible Remedies												
Speed Too High	16								1	16	* Check Motor Voltage - Slow Down Driver												
Speed Too Low	17	4	4		2					17	* Consult Driver Troubleshooting Guide												
Wrong Direction Of Rotation	18	5			3				6	18	* Check Rotation With Arrow On Casing - Reverse Polarity On Motor												
Impeller Installed Backward (Double Suction Imp.)	19		10						12	19	* Inspect												
Misalignment	20					1	2	4	7	20	* Check Angular And Parallel Alignment Between Pump And Driver												
Casing Distorted From Excessive Pipe Strain	21					2	3	5		21	* Check For Misalignment * Check Pump For Wear Between Casing And Rotating Elements * Analyze Piping Loads												
Inadequate Grouting Of Base	22							6		22	* Check Grouting And Regrout If Required												
Bent Shaft	23					3	4	7	8	23	* Check Deflection (Should Not Exceed 0.002"). Replace Shaft And Bearings If Necessary												
Internal Wear	24				8				9	24	* Check Impeller Clearances												
Possible Causes	#	A	B	C	D	E	F	G	H	#	Possible Remedies												

MECHANICAL SYSTEM

MECHANICAL SYSTEM

Table 4-6 (cont.)

Symptoms												Symptoms																						
D						Insufficient Disch. Pressure						Short Bearing Life						E																
C						Intermittent Operation						Short Mech. Seal Life						F																
B						Insufficient Capacity						Vibration & Noise						G																
A						No Liquid Delivery						Power Demand Excessive						H																
Possible Causes												#	A	B	C	D	E	F	G	H	#	Possible Remedies												
MECHANICAL SYSTEM	Mechanical Defects Worn, Rusted, Defective Bearings											25							5	8	10	25	* Inspect Parts For Defects - Repair Or Replace. Use Bearing Failure Analysis Guide * Check Lubrication Procedures											
	Unbalance - Driver											26						5	7	9		26	* Run Driver Disconnected From Pump Unit - Perform Vibration Analysis											
	Unbalance - Pump											27						4	6	3		27	* Investigate Natural Frequency											
	Motor Troubles											28						6	8	10	11	28	* Consult Motor Troubleshooting Guide											
Possible Causes												#	A	B	C	D	E	F	G	H	#	Possible Remedies												

MECHANICAL SYSTEM

**Beckwith
& Kuffel**

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**Any
Questions ?**

